

## **ABSTRACT**

Title of Dissertation:                    **INTERFACE DESIGN FOR ALL-SOLID-  
STATE LITHIUM METAL BATTERIES**

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Lithium-ion batteries (LIBs) have expanded their application from electronics to electric vehicles (EVs). To ease the safety concerns and the “range anxiety”, solid-state lithium batteries (SSLBs) become a more attractive choice. The replacement of flammable and toxic liquid electrolytes with solid-state electrolytes (SSEs) makes it a safer option. The utilization and compatibility of high specific capacity materials such as sulfur cathode and lithium-metal anode increase the cell energy density. However, SSLBs still face challenges towards practical application, which mainly from the solid-solid contact nature on the interfaces. On the anode side, lithium dendrite growth and high interface resistance both hindered the longevity of the cells. On the cathode

side, low initial Coulombic efficiency (CE) and low capacity utilization of sulfur obstructed the realization of high loading cathodes.

In this dissertation, I addressed both challenges of dendrite and contact on the anode side by adding strontium into lithium anodes. Different from all previous metal/metal oxide coating on garnet or Li alloy anodes that form lithiophilic interlayer, a lithiophilic/lithiophobic bifunctional layer is formed to reduce the interfacial resistance and to suppress the growth of lithium dendrite, which is confirmed by comprehensive material characterizations, electrochemical evaluations, and simulations. The optimum Li-Sr | garnet | Li-Sr symmetric cells achieve a high critical current density (CCD) of 1.3 mA/cm<sup>2</sup> and can be cycled for 1,000 cycles under 0.5 mA/cm<sup>2</sup> at room temperature, providing a new strategy for high-performance garnet SSLB. Furthermore, I (1) verified the importance of lithiophobic on dendrite suppression by discovering and successfully constructing the highest interface energy ( $\gamma$ , against lithium) material ever reported among all lithium compounds that can be formed on the electrolyte | anode interface; (2) revealed the impact of anode properties on the interface by enhancing the Li self-diffusivity by a co-doping method, achieved an outperformed critical loading of 4.1 mAh/cm<sup>2</sup> at 1.0 mA·cm<sup>-2</sup> at room temperature. On the cathode side, I tackled both low CE and low capacity utilization issues by promoting both Li<sup>+</sup> and e<sup>-</sup> transportation across the cathode | SSE interface, resulting in high capacity utilization of 96.5% and high capacity retention of 88.8% after 145 cycles at a high loading of 4.0 mAh cm<sup>-2</sup> under room temperature in Li<sub>6</sub>PS<sub>5</sub>Cl based SSLB.

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by

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**Dedicated to**

**Those who have been struggling and suffering but keep  
marching on with a brave heart**

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# Chapter 1 Introduction

## 1.1 Sustainable Energy and Energy Storage Devices

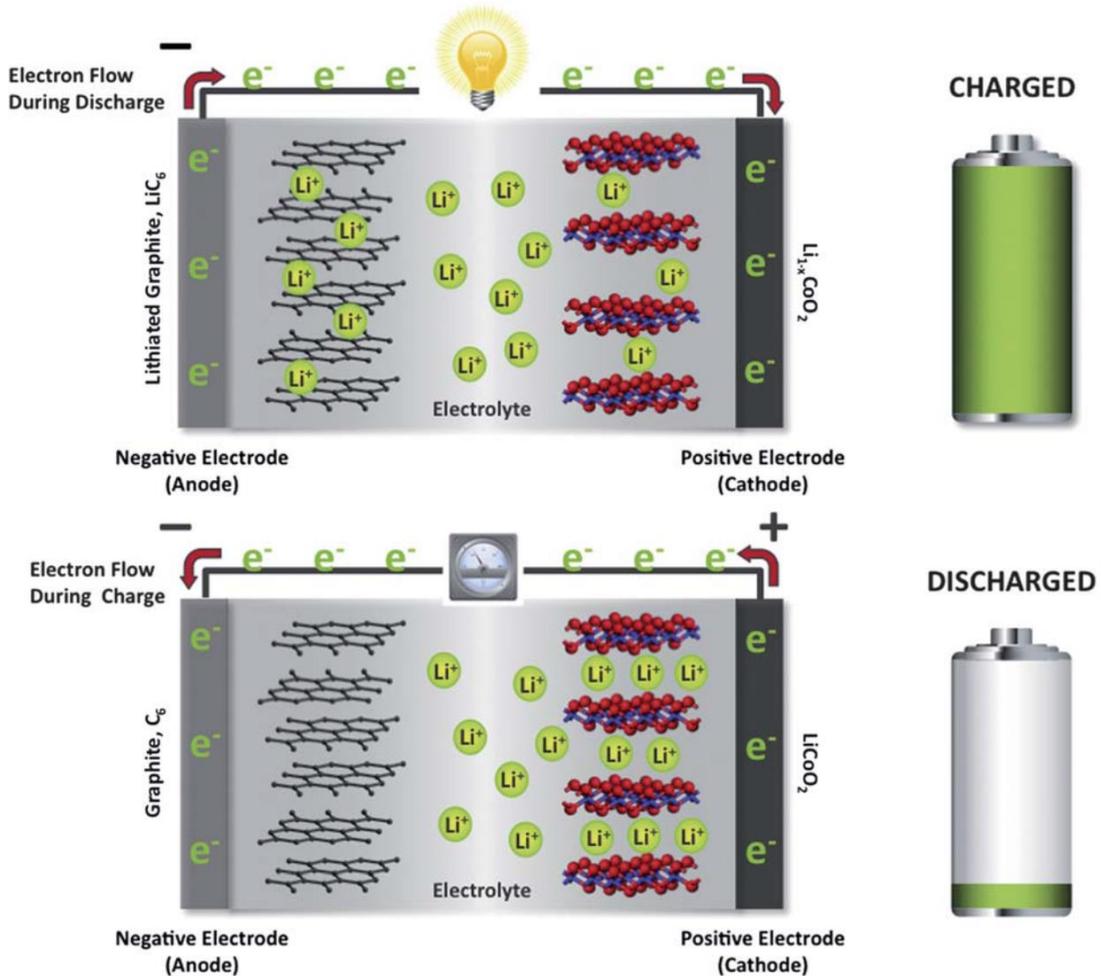
With the advent of electric vehicles and the extensive usage of various new mobile electronic devices, sustainable clean energy has become more and more important for the whole planet and future generation. Energy storage devices are the connections between clean energy sources (such as wind energy, solar energy, etc.) and people's practical daily life <sup>1</sup>, which can gather the energy from the former sources and release it for the latter.

Energy storage technologies can be categorized into physical energy storage (such as pumped water storage, compressed air energy storage, flywheel energy storage, etc.), chemical energy storage (such as various energy storage batteries, flow batteries hydrogen fuel cells, and supercapacitors, etc.) and magnetic energy storage (such as superconducting magnetic energy storage technology, SMES) <sup>2</sup>. Among which, lithium-ion battery is the most successfully commercialized energy storage device.

## 1.2 Lithium-ion Batteries and Next Generation Batteries

Lithium-ion battery is a secondary battery in which lithium ions are intercalated and deintercalated back and forth between the positive (cathode) and negative (anode) electrodes, accompanied by redox reactions. The cathode is generally a lithium-

containing transition metal oxide; there are many types of canoed material, and commercialized lithium-ion batteries mostly use graphite. The electrolyte is generally a lithium salt dissolved in an organic solvent. A porous polymer film is often used as a separator to separate the anode from the cathode to avoid short-circuits. **Figure 1-1** is a schematic diagram of the working principle of a lithium-ion battery. During discharge, the lithium-ion stored between the graphite layers migrates and intercalates into the cathode. And vice versa when charging.



**Figure 1-1** A schematic illustration of the working principles of a  $\text{Li}_x\text{C}_6/\text{Li}_{1-x}\text{CoO}_2$  lithium-ion cell. During discharge, lithium ions diffuse from a lithiated graphite

( $\text{Li}_x\text{C}_6$ ) structure (the anode) into a delithiated  $\text{Li}_{1-x}\text{CoO}_2$  structure (the cathode) with concomitant oxidation and reduction of the two electrodes, respectively. The reverse process occurs during charge.<sup>3</sup>

Lithium-ion battery was first mass-produced by Sony in Japan in the 1990s, utilizing  $\text{LiCoO}_2$  as the positive electrode and graphite as negative electrode. With significant advantages such as small size, long cycle life, no memory effect, and high working voltage, lithium-ion batteries have a wide range of applications. In addition to portable electronic devices, people's pursuit of electric/hybrid vehicles and large-scale power grids in recent years has also brought lithium batteries into more exposure.

In the past two decades, lithium-ion batteries and their industries have continued to flourish. However, in recent years, the existing lithium-ion battery technology has gradually been unable to meet people's increasingly stringent requirements on batteries for mobile consumer electronic devices, electric vehicles, and large-scale energy storage system. Next generation battery technologies have gradually become a hotspot.

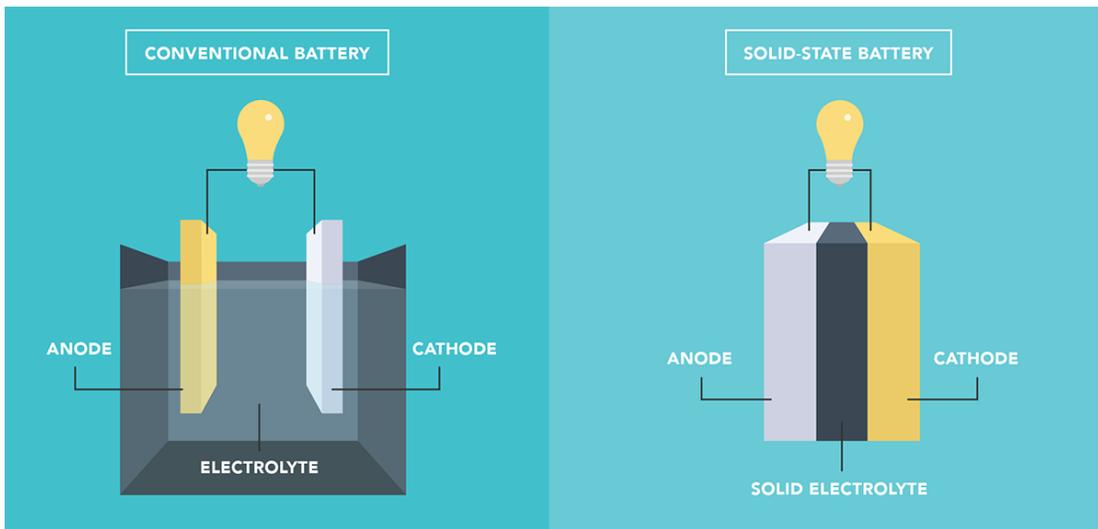
Although lithium-ion batteries are powering almost everything in our daily life from your cell phone, laptop to even electric vehicles, scientists are still pursuing next-generation batteries to make the electric vehicle range longer, the cell phone charge faster and the laptop battery lighter. And most importantly, making a high safety battery to protect people from any accident caused by the batteries thermal runaway.

The all-solid-state lithium metal battery is believed to be the ultimate answer, in which the substitution of flammable organic liquid electrolyte to solid state

electrolyte (SSE) provides the safety while the substitution of graphite to lithium metal anode provides the high energy.

### 1.3 All-Solid-State Lithium Metal Batteries

The basic structure and working principle of all-solid-state lithium batteries are similar to those of traditional lithium-ion batteries. <sup>4</sup> As shown in **Figure 1-2**, the lithium-ion battery is composed of cathode, separator, electrolyte, anode and current collector. While the SSLB keeps the solid electrodes and replaces the separator and liquid electrolyte with a solid-state electrolyte (SSE).



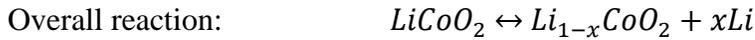
**Figure 1-2** A schematic illustration of the structure of a solid-state batteries. <sup>4</sup>

Take  $\text{LiCoO}_2$  – Graphite lithium-ion battery as an example:





When the anode material is substituted to lithium metal, the cathode reaction keeps the same, while the anode an overall reaction become:



Given the fact that most of the current all-solid-state batteries use metallic lithium or lithium alloy as the anode and it is also the main subject this dissertation focuses on, this article collectively refers to such batteries as solid-state lithium metal batteries (SSLBs).

### 1.3.1 Advantages of Solid-State Batteries

Compared with traditional lithium-ion batteries, SSLBs have the following technical advantages:

1. High energy density. Thanks to the excellent stability and mechanical strength of the SSE, lithium metal is expected to be used in SSLB. Lithium metal is the lightest metal element in the periodical table. It has a very low reduction potential ( $-3.04$  V vs. standard hydrogen electrode potential) and an ultrahigh theoretical specific capacity ( $3,860$  m Ah  $g^{-1}$ ). In addition, when high-voltage positive electrodes are

used in conjunction with lithium metal, the energy density of the battery can be further improved.

2. The shape of the battery is highly expandable and has a wide range of applications. Thanks to the material diversity and good processability, SSLB can be produced in various forms, such as sputtering, pressing, casting, etc. which are applicable to a variety of occasions.

3. Higher safety. SSLB utilizes SSE instead of toxic, flammable organic electrolyte that consists of organic solvent and lithium salts. It can solve the leakage, corrosion and other issues in traditional lithium-ion battery. In addition, inorganic solid electrolytes have significantly improved heat dissipation compared with liquid electrolytes.

4. Simplified battery pack design. Single SSLB can be connected in series in order to reduce the waste of energy/volumetric density from the auxiliary materials (such as current collectors and packaging). Its excellent wide temperature work range greatly reduces the dependence on thermal management modules, which is further improving energy density on the pack level.

### 1.3.3 SSE and its Categories

There are many kinds of SSE with totally different characteristics. Generally, SSE can be divided into oxides, sulfides and polymers. Among them, the oxide solid electrolyte can also be subdivided into LISICON (Lithium superionic conductors)

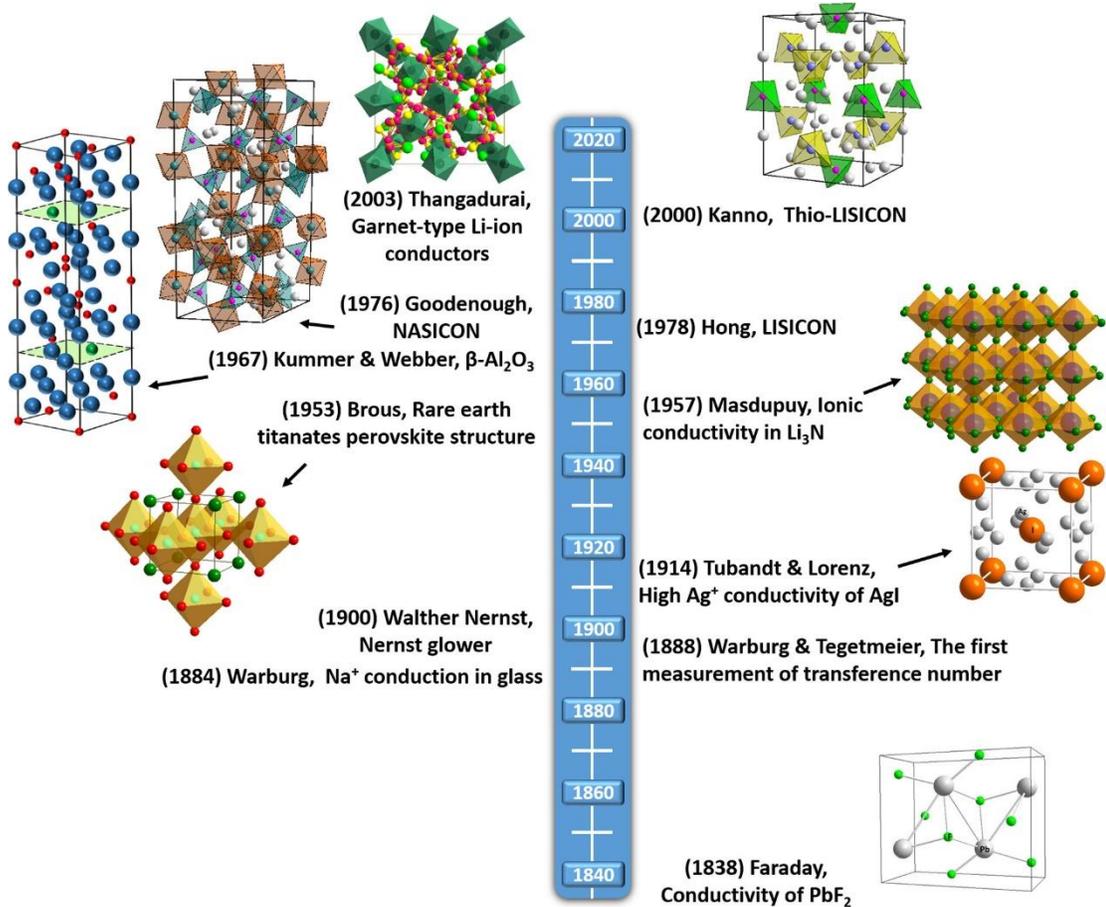
type, NASICON (Sodium superionic conductors) type, garnet type, etc.<sup>5</sup> Sulfides can also be divided into binary  $\text{Li}_2\text{S-P}_2\text{S}_5$ , LGPS series, lithium argyrodite  $\text{Li}_6\text{PS}_5\text{X}$  ( $\text{X} = \text{Cl, Br, I}$ ), etc.<sup>6</sup> While polymer SSE can be divided into polyethylene oxide (PEO) base, polypropylene oxide (PPO) base, base, polymethyl methacrylate (PMMA) base, polyacrylonitrile (PAN) base, etc. In addition, LiPON-based thin-film solid electrolytes, hydride, nitride and halide SSE have also been developed rapidly in recent years. In view of the large number of types, the following highlights a few of the most commonly used types.

#### 1.3.4 Garnet-type SSE

As demonstrated in **Figure 1-3**, Garnet SSE was first reported by Thangadurai in 2003.<sup>7</sup> Among which, garnet SSE with a nominal formula  $\text{Li}_7\text{La}_3\text{Zr}_2\text{O}_{12}$  (LLZO)<sup>8</sup> demonstrates a high ionic conductivity (1 mS/cm for Ta-doped LLZO<sup>9</sup>) and wide electrochemical window<sup>8,10</sup>. In addition, the high mechanical properties are expected to block the lithium dendrite penetration.

In its crystal structure,  $\text{Li}^+$  will first occupy and fill tetrahedrons and be fixed, thus contributing less to the overall conductivity. While the octahedrals are not filled, the accordingly generated vacancies will provide the main channel for  $\text{Li}^+$  conduction. Since lithium ions need such directional diffusion to adjacent vacancies to generate ionic conduction and there is no  $\text{Li}^+$  vacancies in the tetragonal phase. Thus, the

tetragonal LLZO (t-LLZO) is thermodynamically more stable than the cubic LLZO (c-LLZO), but the ionic conductivity is orders of magnitude lower.



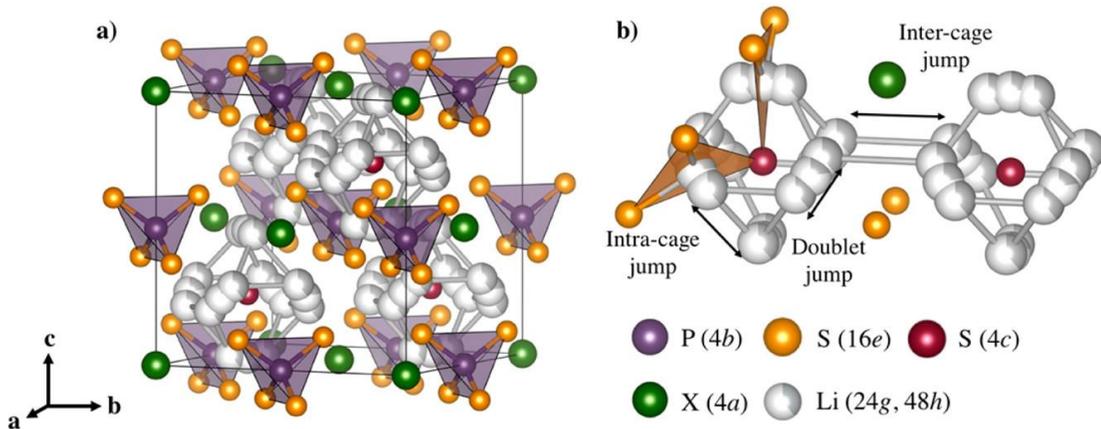
**Figure 1-3** Historical development of solid electrolytes and schematic of their structures.<sup>5</sup>

Massive efforts had been made on how to increase lithium vacancies to obtain cubic LLZO. Major methods includes: substitution of Li<sup>+</sup> site with high-valence cations ion Al<sup>3+</sup>, Ga<sup>3+</sup>; replacement of Zr<sup>4+</sup> sites with Sb<sup>5+</sup>, Nb<sup>5+</sup>, Ta<sup>5+</sup>, Te<sup>5+</sup>, W<sup>5+</sup>; substituting La<sup>3+</sup> site with Rb<sup>3+</sup> etc.<sup>11</sup> Among witch, ionic conductivity as high as  $1.62 \times 10^{-3}$  S cm<sup>-1</sup> at room temperature through Ga<sup>5+</sup>, Rb<sup>+</sup> co-doping can be achieved.<sup>12,13</sup>

Although garnet-type SSE have good performance, its hard and brittle characteristics also lead to poor interface contact with the electrode and thus obstacles in the processing towards practical application.<sup>12</sup> The Ta-doped LLZTO ( $\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.5}\text{Ta}_{0.5}\text{O}_{12}$ ) is selected as one of the model SSE in this dissertation for its high ionic conductivity and stability against the lithium anode, and detail of the synthesis process will be elaborate in [Chapter 2.1.1](#).

### 1.3.3 Argyrodite-type SSE

Argyrodite  $\text{Li}_6\text{PS}_5\text{X}$  ( $\text{X}=\text{Cl}, \text{Br}, \text{I}$ ) has a parent phase of  $\text{Li}_7\text{PS}_6$ , and a cubic phase (originally an orthorhombic phase at low temperatures) can be obtained by substituting part of S to X, resulting in  $10^{-3} \text{ S cm}^{-1}$  level of  $\text{Li}^+$  conductivity.<sup>14</sup> **Figure 1-4** shows the structure and the lithium-ion transportation modes of the  $\text{Li}_6\text{PS}_5\text{X}$ .



**Figure 1-4** Crystal structures of  $\text{Li}_6\text{PS}_5\text{X}$  with  $\text{X} = \text{Cl}, \text{Br}, \text{I}$ . (b) Doublet jump, intra-cage jumps and inter-cage jump of Li in the  $\text{Li}_6\text{PS}_5\text{X}$ .

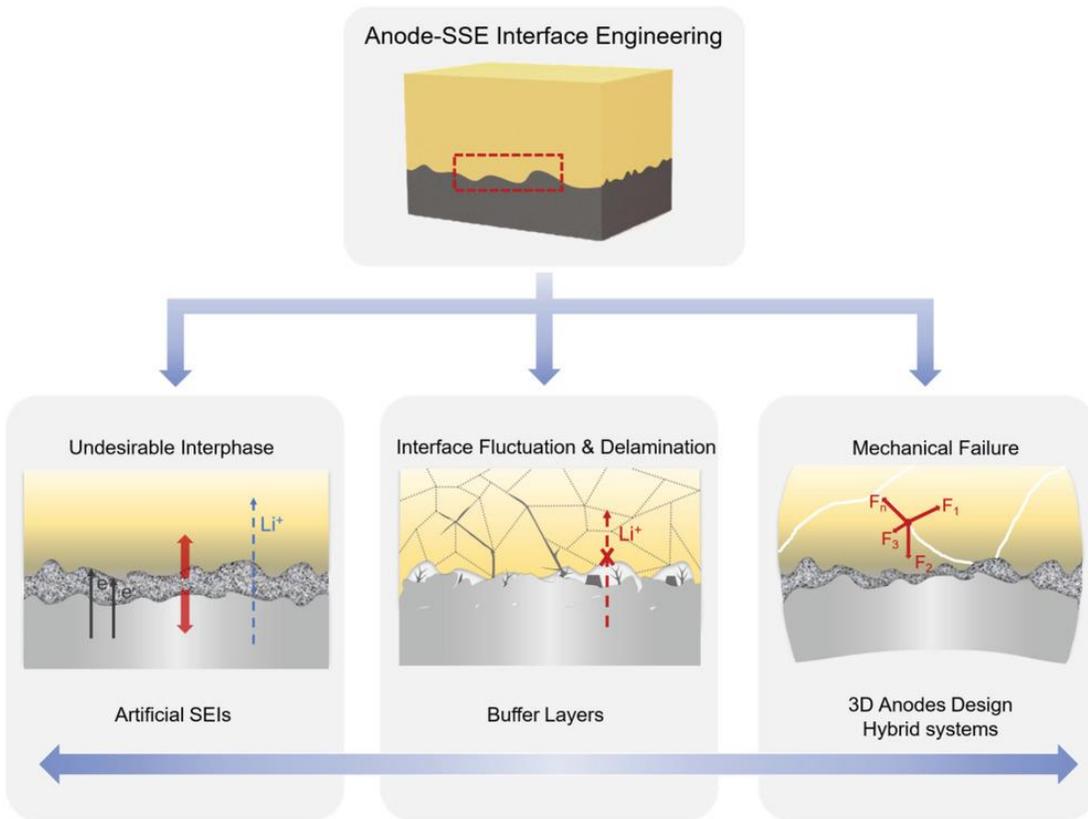
There are two major preparation methods for argyrodite  $\text{Li}_6\text{PS}_5\text{X}$ , liquid phase method and solid phase synthesis method. The liquid phase method is a good way to synthesize particles with controllable particle size and morphology, which makes it possible to tune the relevant properties of the SSE. In 2015, Yubuchi et al.<sup>15</sup> first reported the synthesis of  $\text{Li}_6\text{PS}_5\text{Cl}$  by dissolution-reprecipitation method with ethanol as the solvent. However, the ionic conductivity at room temperature of  $1.4 \times 10^{-5} \text{ S cm}^{-1}$  is not very ideal. Afterwards, Yubuchi et al.<sup>16</sup> utilized tetrahydrofuran (THF) and absolute ethanol (EtOH) as dual solvents, resulting in  $10^{-3} \text{ S cm}^{-1}$  level of  $\text{Li}^+$  conductivity. However, significantly more impurities are always found in argyrodite  $\text{Li}_6\text{PS}_5\text{X}$  made by liquid phase method, mainly due to the inevitable reactions between the  $\text{P}_4\text{S}_3$  unit and the solvent.<sup>17</sup>

In the solid phase method, precursors  $\text{Li}_2\text{S}$ ,  $\text{P}_2\text{S}_5$  and  $\text{LiX}$  are annealed under protected inert atmosphere after mechanical milling. Rao et al. reported the synthesis of  $\text{Li}_6\text{PS}_5\text{Cl}$  using this solid route for the first time and got an ionic conductivity of  $1.1 \times 10^{-3} \text{ S cm}^{-1}$  at room temperature.<sup>18</sup> The  $\text{Li}_6\text{PS}_5\text{Cl}$  using solid route is selected as one of the model SSE in this dissertation for its high ionic conductivity, feasibility and repeatability of synthesis, and detail of the synthesis process will be elaborate in [Chapter 2.1.3](#).

## 1.4 The Challenges of All-Solid-State Lithium Metal Batteries and Progress

### 1.4.1 Lithium Metal Anode and its Interface with SSE

As discussed in [Chapter 1.3](#), lithium metal is considered to be the ideal anode material for next-generation batteries for its high theoretical specific capacity. However, the interfacial contact of the inorganic solid electrolyte/metal lithium anode interface is poor and the dendrite penetration has become the biggest obstacles to the application of metal lithium anode.



**Figure 1-5** The overview of main existing problems and strategies for the anode–SSE interface.<sup>19</sup>

On the one hand, the poor wettability between inorganic SSE and lithium metal results in a large interfacial resistance. On the other hand, the interfacial reaction at the electrolyte/lithium metal interface leads to the formation of an interfacial layer, which may hinder the migration of  $\text{Li}^+$  and leads to performance degradation. Most importantly, lithium dendrites form in solid-state batteries and penetrate the solid electrolyte, causing internal short-circuit, leading to serious safety hazards. Therefore, exploring the interface design of inorganic solid electrolyte/lithium metal towards 1) good contact, 2) high stability, 3) dendrite-free, become the most critical challenges.

#### 1.4.2 Sulfur-Based Cathode and its Interfaces in Solid-State Batteries

The energy density of the current state-of-art lithium-ion/metal batteries are restricted by the traditional metal oxide cathodes (such as  $\text{LiCoO}_2$ ,  $\text{LiFePO}_4$  and  $\text{LiMnO}_4$ , etc.) which usually have a theoretical specific capacity of around  $100\text{-}200 \text{ mAh g}^{-1}$ . Due to the high theoretical specific capacity of sulfur element ( $1675 \text{ mAh g}^{-1}$ ), lithium-sulfur batteries are considered to be the best choice for next-generation high-energy-density energy storage systems.

During the conversion between  $\text{S}_8$  and  $\text{Li}_2\text{S}$ , polysulfide would form as intermediate product. These polysulfides can dissolve in common liquid Li-S electrolytes, which will migrate from the cathode to the anode under the concentration gradient, and further being reduced by lithium metal, forming the “shuttle effect”<sup>20</sup>, leading to the loss of active material and efficiency.

Fortunately, replacing organic liquid electrolyte to SSE can prevent the formation of polysulfide and eliminate the polysulfide “shuttle effect”. However, there are also other problems, such as the insulating properties of S and  $\text{Li}_2\text{S}$  and the volume change between the S and  $\text{Li}_2\text{S}$ . The former will lead to poor electrochemical reaction kinetics, resulting in the low utilization rate of active materials, causing the increase of the polarization inside the battery and reduction of the energy density. The latter with a volume expansion of about 80% after lithiation<sup>21</sup> will cause the cathode material to pulverize and permanent loss of capacity. Both these two problems will be much tougher challenges in a solid-state battery originating from the poor solid-solid contact of the three main component inside a cathode for solid-state battery: the active material, the electronic conductor and the SSE. Therefore, the interface design of the electronic additive/SSE/sulfur triple-phase boundaries become the most critical challenge.

Improving the  $\text{Li}^+$  transfer through coating SSE on sulfur, or enhancing the e-conduction using electronic conductive carbon as sulfur host can enhance S/ $\text{Li}_2\text{S}$  redox reaction due to the improved triple-phase contacts in these modified sulfur composite cathode. However, the preparation procedures for these modified sulfur cathodes are time-consuming. Besides, the low active sulfur content in the S@C composite will decrease the cell-level energy density because the large amount of electronic conductive carbon host cannot provide capacity to the battery. Therefore, sulfur host that can provide extra capacity was introduced into the sulfur Among these active sulfur hosts,  $\text{FeS}_2$  with high electronic/ionic conductivity has been

demonstrated to mediate the sulfur redox reaction in SSLB.<sup>22,23</sup> Besides, the pyrite cathode has a high-cost advantage. FeS<sub>2</sub> could reduce cathode material costs by 90%, from \$35 per kWh to \$3 per kWh. Therefore, FeS<sub>2</sub> will be used as the model sulfur host for this dissertation to studies the interface design of cathode-electrolyte, which will be elaborate in [Chapter 6](#).

### 1.5 Motivation, Objectives and Dissertation Layout

#### 1.5.1 Motivation and Objectives

In order to achieve the goal of high energy density and high safety next-generation SSLB battery, both deeper fundamental understanding and practical advance of the electrode-electrolyte interface design are urgently needed.

On the anode side, I choose garnet SSE as the model electrolyte for its stability against lithium, which provides a low-noise background as by-product free as possible. In this way, the interface components will be simplified, and related interface properties can be clearer. And I will focus on the interface design toward both better solid-solid contact and dendrite suppression.

On the cathode side, the establishment of garnet cathode requires a co-sintering of the cathode materials and the ceramic electrolytes, which can be time consuming for each iteration. In consideration of the efficiency and reproducibility, I choose sulfide as the model electrolyte for the cathode study.

### 1.5.2 Dissertation Layout

**Chapter 2:** Common experimental methods used in following chapters, such as the synthesis of the SSE will be summaries in here to avoid repetition.

**Chapter 3:** On the anode side interface, I will address both the challenges of Li dendrite and high interface resistance by doping strontium(Sr) into lithium anodes, thus form a lithiophilic/lithiophobic bifunctional layer. The interlayer reduces the interfacial resistance and also suppresses lithium dendrite. This work is published in ACS Energy Letter. (**He, X.**; Ji, X.; Zhang, B.; Rodrigo, N. D.; Hou, S.; Gaskell, K.; Deng, T.; Wan, H.; Liu, S.; Xu, J.; Nan, B.; Lucht, B. L.; Wang, C. Tuning Interface Lithiophobicity for Lithium Metal Solid-State Batteries. *ACS Energy Letter* **2021**. <https://doi.org/10.1021/acseenergylett.1c02122>.)

**Chapter 4:** In this Chapter, I screened the Gibbs energy for the reaction between Li and the metal oxides ( $nLi + MO_m \leftrightarrow M + nLiO_{m/n}$ ) and identified the LiYO<sub>2</sub> as a highly thermodynamical stable candidate for the interface between the electrolyte and lithium. In addition, LiYO<sub>2</sub> has a record high interface energy against lithium of 81.65 meV/Å, which would provide high dynamic stability against dendrite penetration. This work is ready to submit. (**He, X.**; Ji, X.; Wang, Z.; Wan, H.; Wang, C. High Interface Energy Enabled Highly Stable Garnet-based Lithium Metal Solid-State Batteries)

**Chapter 5:** I will discuss my attempt to understand the void formation on the SSLB anode interface. The product of the lithium full stripping capacity and the applied

current, which will be defined as the void suppression capability (VSC). The relationship between the CCD/interface-stability and VSC will be discussed. Enhancement of the VSC will be demonstrated by refining the grain using a Mg-1wt%La inoculant. This work is under review with Nature Material. (Ji, X.†; **He, X.†**; Chen, C.†; Hou, S.; Xu, J.; Zhang, B.; Ruan, Y.; Zhang, J.; Deng, T.; Chen, J.; Wang, C. Void Suppressive Lithium Anodes for All-Solid-State Batteries. (Co-First Author))

**Chapter 6:** On the cathode side, I will elaborate on the idea to construct a  $\text{FeS}_2@\text{S}@\text{CuI}$  composite to form a decent  $\text{Li}^+/\text{e}^-$  pass way across the cathode |  $\text{Li}_6\text{PS}_5\text{Cl}$  SSE interface upon first several cycle. The S/ $\text{Li}_2\text{S}$  redox kinetics will be enhanced for better capacity utilization at high cathode loading ( $4.0 \text{ mAh cm}^{-2}$  under room temperature). This work is ready to submit. (Wan, H. †; He, X.†; Ren, Y.; Wang, C. Highly reversible sulfur cathode for all-solid-state lithium-sulfur battery (Co-First Author))

## Chapter 2 Material Synthesis, Battery Fabrication and Characterization Methods

### 2.1 Material Synthesis Methods

#### 2.1.1 Synthesis of the LLZTO Solid Electrolyte

The LLZTO garnet electrolyte was synthesized via a conventional solid-state reaction technique. LiOH·H<sub>2</sub>O (99.995%, Sigma-Aldrich, 10 wt.% excess to compensate for the loss of Li during high-temperature sintering), La<sub>2</sub>O<sub>3</sub> (99.99%, Sigma-Aldrich, pre-heated at 900°C for 12 h to remove the water), ZrO<sub>2</sub> (99.5%, Alfa Aesar), and Ta<sub>2</sub>O<sub>5</sub> (99.99%, Sigma-Aldrich) with stoichiometry ratio were used as precursors. The mixture was mechanical ball-milled (PM 100, Retsch) at 400 rpm for 24 h within a zirconia ceramic vial together with anhydrous 2-propanol. ZrO<sub>2</sub> balls with a diameter of 5 mm were used as the grinding medium. After ball-milling, the slurry was dried and calcined at 900 °C for 10 h in the Al<sub>2</sub>O<sub>3</sub> crucible. After the first calcining, the powder was ball-milled again with the same parameters as above. This step is done to decrease the particle size further and increase the reactivity of the powder. Then, the obtained powder was sieved through 100 grits after drying. The obtained powder was pressed into Φ13 mm pellets, followed by isotactic pressing under 0.2 metric tons. The pellets were then sintered in air at 1150°C for 5 hours in MgO crucible covered with the same powder. The area of the obtained LLZTO pellet is around 0.75 cm<sup>2</sup> and the thickness is around 1 mm.

### 2.1.2 Assembly of the LLZTO Cells

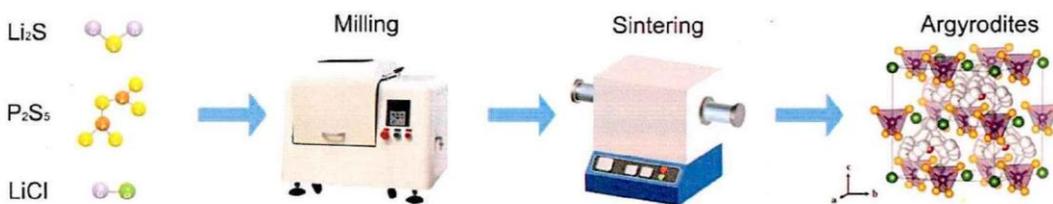
For Li-Au | LLZTO | Li-Au symmetric cells, the gold was sputtered on the LLZTO pellets under 15 mA for 600 seconds (Cressington sputter coater 108). The residual Au on the side surfaces is polished off with sandpaper. Lithium foil was brushed to expose a fresh shining surface and punched into a round shape with a diameter of 3/8 inch. The Au sputtered LLZTO pellets were sandwiched by lithium foils followed by heat-treatment at 175°C for 12 hours to ensure the alloy reaction between Au and Li. Then, the as-prepared Li-Au | LLZTO | Li-Au symmetric cell was cooled down to room temperature for testing.

The symmetric cells were assembled in 2032-coin cells by sandwiching the spring, stainless steel (SS) disc, and the anode-attached pellet. The thickness was controlled around 100-200  $\mu\text{m}$  for any Li or Li alloy anode attached to SSE.

In the “Proof of Concept” full-cells, the commercially available NMC811 cathode was provided by SAFT. The NMC811 with the loading of  $\sim 0.8$  or  $1.6 \text{ mAh/cm}^2$  was selected as the cathode for the SSLBS. The  $\text{LiFePO}_4$  cathode was prepared by mixing  $\text{LiFePO}_4$ , conductive carbon and PVDF with a weight ratio of 80:10:10. A small amount of liquid electrolyte (10  $\mu\text{L}$ ) was used to wet the cathode | LLZTO interface.

### 2.1.3 Synthesis of the Li<sub>6</sub>PS<sub>5</sub>Cl Solid Electrolyte

As shown in **Figure 2-1**, Li<sub>6</sub>PS<sub>5</sub>Cl solid electrolyte was synthesized using high-energy mechanical milling. Li<sub>2</sub>S (Sigma-Aldrich, 99.98%), P<sub>2</sub>S<sub>5</sub> (Sigma-Aldrich, 99%) and LiCl (Sigma-Aldrich, 99%) were used as starting materials. These materials were weighed in the molar ratio of Li<sub>2</sub>S/P<sub>2</sub>S<sub>5</sub>/LiCl = 5/1/2 in an argon-filled glovebox, milled, and sintered at 550 °C for 5 hours under Ar.



**Figure 2-1** Schematic diagram of the synthesis process of Li argyrodite electrolytes in this work.<sup>23</sup>

### 2.2 Electrochemical Characterization Methods

The Li<sup>+</sup> ionic conductivity measurements of the electrolytes were carried out on an electrochemical station (Gamery G1000) with sputtered Au as the electrode. The measurements were performed over the frequency range from 1Hz to 1 MHz with an AC voltage amplitude of 10 mV.

### 2.3 Material Characterization Methods

SEM was taken at the University of Maryland using Hitachi SU-70 analytical GEG SEM (Japan) equipped with an EDS detector. The electron accelerating voltage is 200 KeV.

X-ray powder diffraction (XRD) was performed on D8 Advance with LynxEye and SolX (Bruker, USA) using Cu K $\alpha$  radiation.

### 2.4 Density Functional Theory (DFT) Calculation

The DFT calculations<sup>24,25</sup> are performed by using Vienna Ab-initio Simulation Package (VASP)<sup>26</sup> with Projector Augmented Wave (PAW) method.<sup>27</sup> And the exchange-correlation energy is described by the functional of Perdew, Burke, and Ernzerhof (PBE) form<sup>28,29</sup> including van der Waals corrections (DFT-D3 method).<sup>30</sup> The kinetic energy cutoff of electron wave functions is 520 eV. The Brillouin zone is sampled by using the Monkhorst–Pack scheme.<sup>31</sup> The interface energy was evaluated using the same method in previous work.<sup>32</sup> Visualization of the atomic structures is made by using VESTA.<sup>33</sup>

# Chapter 3 Tuning Interface Lithiophobicity for Lithium Metal Solid-State Batteries

## 3.1 Introduction

Lithium-ion batteries (LIBs) have expanded their application from electronics to electric vehicles (EVs).<sup>34</sup> To ease the safety concerns<sup>35</sup> and the “range anxiety”, the solid-state lithium battery (SSLB) becomes a more attractive choice. The replacement of flammable and toxic liquid electrolyte<sup>36</sup> with solid-state electrolyte (SSE) makes it a safer option. Moreover, the wide electrochemical window of SSE enables the utilization of high-voltage cathodes and Li-metal anodes, which leads to a higher output voltage and thus a higher energy density.

Among all the inorganic SSE, garnet SSE with a nominal formula  $\text{Li}_7\text{La}_3\text{Zr}_2\text{O}_{12}$  (LLZO)<sup>8</sup> demonstrates a high ionic conductivity (1 mS/cm for Ta-doped LLZO<sup>9</sup>) and wide electrochemical window<sup>8,10</sup>. In addition, the high mechanical properties are expected to block the lithium dendrite penetration. Unfortunately, short-circuiting is still observed even at a low current density and a low capacity. Meanwhile, solid-solid contact at Li | LLZO also induces a high interface resistance, which accelerates the reduction of the SSE and the dendrite growth. Thus, interfacial engineering that is aiming to minimize interfacial impedances is critical for SSLB. Introducing a lithiophilic interlayer to wet Li metal is proved as an effective strategy to reduce the interface resistance. Various materials such as Au<sup>37</sup>, Mg<sup>38,39</sup>, Ag<sup>40</sup>, Ge<sup>41</sup>, Al<sup>42</sup>, Si<sup>43</sup>,  $\text{Al}_2\text{O}_3$ <sup>44</sup>, and ZnO<sup>45</sup>, have been utilized to form alloys or prelithated layers. In

addition, various surface coating technologies, such as sputtering<sup>18</sup>, vapor deposition<sup>42</sup>, metal salt aqueous solution<sup>46</sup>, and atomic layer deposition<sup>47</sup>, are applied to form an interlayer between Li and garnet. Interfacial engineering has successfully reduced interfacial resistance from thousands to single-digit  $\Omega \text{ cm}^2$ .<sup>44</sup> This extremely small interfacial resistance at Li | SSE already rivals the ones in conventional LIBs employing liquid electrolytes.<sup>48</sup> However, these interlayers are electronic conductive, which promotes the reduction of solid-state electrolytes and Li dendrite growth. The interfacial engineering seems to be stuck in a new bottleneck since no breakthrough was obtained using new interfacial materials or coating methods. A strategy forming a stable interlayer that keeps an ionic-conducting nature and separates the lithium plating position away from the SSE is needed.

For Li anode, one significant interface resistance comes from the void formation during Li stripping at a high current and capacity due to low  $\text{Li}^0$  diffusivity and large volume shrink. Since the voids cannot be completely healed in the following Li plating process, the void will accumulate into a large hole, increasing the interface resistance<sup>49,50</sup>. If pressure is applied, the plastic deformation capability of the anode also plays an essential role in void evolution.<sup>51</sup> The  $\text{Li}^0$  self-diffusivity can be accelerated by the high lithiophilicity at the Li/SSE interface.<sup>39</sup> However, the wisdom of Li dendrite suppression in liquid electrolytes suggests that a lithiophobic SEI is needed to achieve a high critical current density, which in turn will increase the interface resistance. To simultaneously reduce the interface resistance and also suppress lithium dendrite, a bifunctional surface layer that forms lithiophilic inner-

face bonding to Li and lithiophobic out-layer bonding to SSE is desired. To maintain a low interface resistance during long-term lithium plating/stripping cycles, the lithiophilic/lithiophobic bifunctional layer should be stable at SSE | anode interface without diffusion into or reaction with neither Li nor SSE, and should not reduce the diffusivity of  $\text{Li}^0$  and/or  $\text{Li}^+$ . Although the alloy interface can provide an initial good wettability, the electron-conducting nature of the alloy interfacial layer will facilitate the charge transfer reaction to take place right between the interlayer and the SSE.<sup>52</sup> The deposition of lithium will push the alloy layer away instead of remaining located at the SSE | anode interface<sup>5,38,53,54</sup>, which may not be able to keep benefit for the long-term operation condition.

The ideal bifunctional interlayer for lithium anode should (1) be stably enriched at Li | SSE interface where lithiophilic part toward to the inside Li and lithiophobic part toward to SSE; (2) not reduce the anode  $\text{Li}^0$  diffusivity on lithiophilic side and do not reduce the SSE on lithiophobic side; (3) have a plastic deformation capability to accommodate Li volume change. However, such a Li bifunctional layer has not been explored yet.

$\text{Li}_2\text{O}$  has a high interfacial energy  $\gamma$  and high Li dendrite suppression ability  $\gamma E$ ,<sup>32</sup> which can function as a lithiophobic interlayer to suppress the lithium dendrite growth and lithiophobicity should reflect each other from energy and macroscopic angles, respectively.<sup>55</sup> However, the low ionic conductivity and high interface resistance at Li |  $\text{Li}_2\text{O}$  also introduced considerable resistance<sup>56</sup>. In this work, we demonstrated that 1% of strontium and *in situ* formed SrO could serve as a

bifunctional interlayer where SrO doped Li<sub>2</sub>O keeps the high lithiophobic nature of the Li<sub>2</sub>O but reduces resistance due to the formation of lithiophilic Li-Sr alloy. The unique bifunctional property of Sr-in-Li anodes can reduce the interface resistance and also suppress the Li dendrite, which is distinct from other alloy electron-conductor layers. SrO also shows a robust garnet-philic property as evidenced by the high ionic conductivity of Sr-doped garnet<sup>57,58</sup>, and the high wetting capability of Sr-in-Li on garnet. Using Ta-doped LLZTO (Li<sub>6.5</sub>La<sub>3</sub>Zr<sub>1.5</sub>Ta<sub>0.5</sub>O<sub>12</sub>) as a model solid-state electrolyte<sup>9</sup>, the interface resistance, critical current density (CCD) and cycle stability of LLZTO were systematically investigated using bifunctional Sr-in-Li anodes. The mechanism of bifunctional Sr-Li at Li | LLZTO was revealed using comprehensive characterization, electrochemical performance evaluation, and simulation.

## 3.2 Experimental

### 3.1.1 Synthesis of the Li-Sr Alloy and the Assembly of the Anode

The anode was prepared by a molten lithium method in a glove-box. Initially, 1%, 5%, 10%, and 20% of mole ratio Sr metal flask was added into molten lithium metal at 300°C in a stainless-steel crucible. The crucible was kept at 300°C in an oven for 30 minutes, followed by stirring to ensure a homogeneous reaction. The as-synthesized alloy was melted in a shallow stainless-steel crucible at 300°C with a hot plate inside the glove-box. The as-synthesized LLZTO electrolyte pellet was cleaned

by mechanical dry-polishing using 400 grit sandpaper and then polishing with 1500 grit sandpaper in an Ar-filled glove-box. The cleaned pellet was directly immersed in the shallow crucible with the molten alloy in and the anode will be attached within around 2 minutes. After cooling down to room temperature, the residual metal on the side surface will be polished off with sandpaper. For Li | LLZTO | Li symmetric cells, lithium foil was brushed to expose a fresh shining surface and punched into a round shape with a diameter of 3/8 inch. After being immersed in the molten lithium for 2 minutes, the LLZTO pellets were cooled down to room temperature and sandwiched with two fresh lithium foils. The sandwiched cells were put under 175°C for 12 hours then cool down to room temperature for testing. The thickness was controlled around 100-200µm for any lithium or Li-Sr alloy attached to SSE.

### 3.1.2 Material Characterization

XPS data were collected using the K-Alpha X-ray Photoelectron Spectrometer System (Thermo Scientific™, Al K $\alpha$  radiation,  $h\nu = 1486.68$  eV) at the University of Rhode Island. The sample preparation is the same as the ToF-SIMS test. The sample was directly moved from Ar atmosphere to the XPS chamber with a vacuum transfer container to avoid exposure to the air. The instrument was working under ultra-high vacuum ( $<1 \times 10^{-12}$  atm). The spot size, as well as the analysis area, was 400 µm by 400 µm. The depth profiling was conducted using an Ar<sup>+</sup> ion gun with an ion energy of 200 eV. The angle between the ion gun beam and the surface normal was 0°. A 2 mm ion beam spot was quickly rastered over the targeted area. The etching procedure

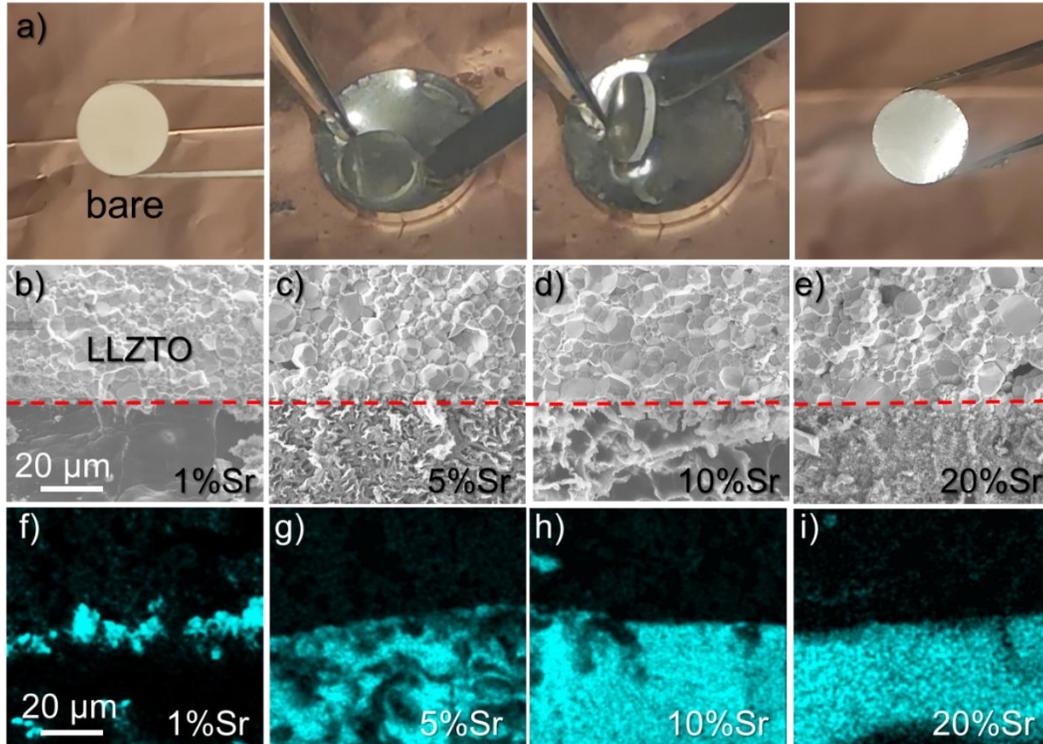
was carried out in a cycle of an accumulated 0, 300, 900, 3000 and 7200 seconds. Spectra were recorded of the sample surface before sputtering and between sputtering cycles. All data was calibrated based on the C1s peak to 284.8 eV for binding energy values. Peak fitting and relative atomic percentage estimation were done using CasaXPS software (version 2.3.24), after removal of a Shirley background and accounting for the relative sensitivity factors (R.S.F) of Thermo K-Alpha.

ToF-SIMS were analyzed on Ga<sup>+</sup> focused ion beam (FIB)/scanning electron microscope (Tescan GAIA3) equipped with ToF-SIMS at the NanoCenter of the University of Maryland. The accelerated voltage for FIB/SEM was 20 kV. To prepare the sample, the garnet pellet with anode reattached was cleaned with a scraper for removing the anode as much as possible in the Ar-filled glove-box before characterizations. The Sr (88), Zr (90), La (139), Li (7) were tested simultaneously in the negative mode. The O (16) was tested in the positive mode. The results from negative mode and positive mode were plotted together according to the depth of the craters measured in the SEM results. The frames were converted to depth according to the depth of the craters measured in the SEM results. The surface of the sample (anode side) is defined as the 0 depth.

### 3.3 Li-Sr / LLZTO Interface and the Li-Sr Anode

Li-Sr alloys with 1%, 5%, 10%, and 20% of mole ratio Sr were synthesized by melting Li and Sr at 300°C. The corresponding Li-Sr alloys were noted as Li-Sr-1%,

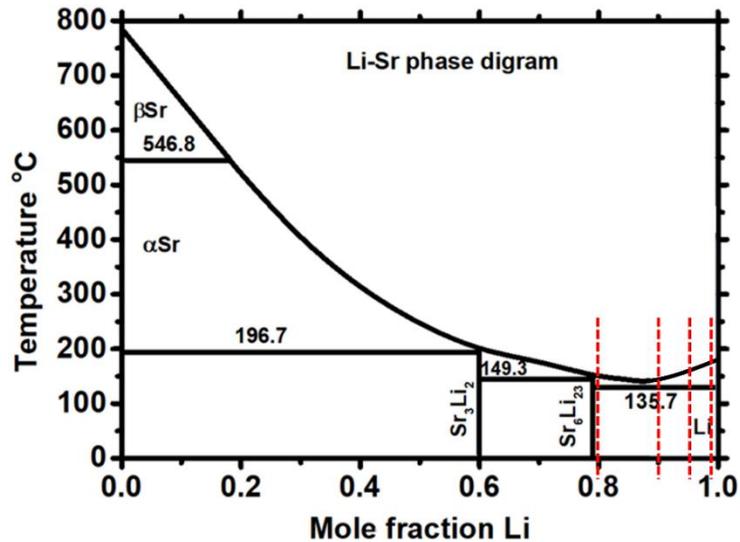
Li-Sr-5%, Li-Sr-10%, and Li-Sr-20%, respectively. As shown in **Figure 3-1 a**, when the polished LLZTO pellet was immersed into the molten Li-Sr alloy, liquid Li-Sr alloy quickly spread onto the LLZTO surface, indicating a high wettability of Li-Sr alloy with LLZTO.



**Figure 3-1** Assembling and characterization of Li-Sr | LLZTO interface. (a) Digital photographs showing the process of attaching the Li-Sr onto garnet LLZTO pellet. Cross-section morphology (b-e) and Sr elemental mapping (f-i) of the Li-Sr-1%, Li-Sr-5% Li-Sr-10% and Li-Sr-20% electrode interface with the LLZTO pellet. The red dash lines mark the interfaces.

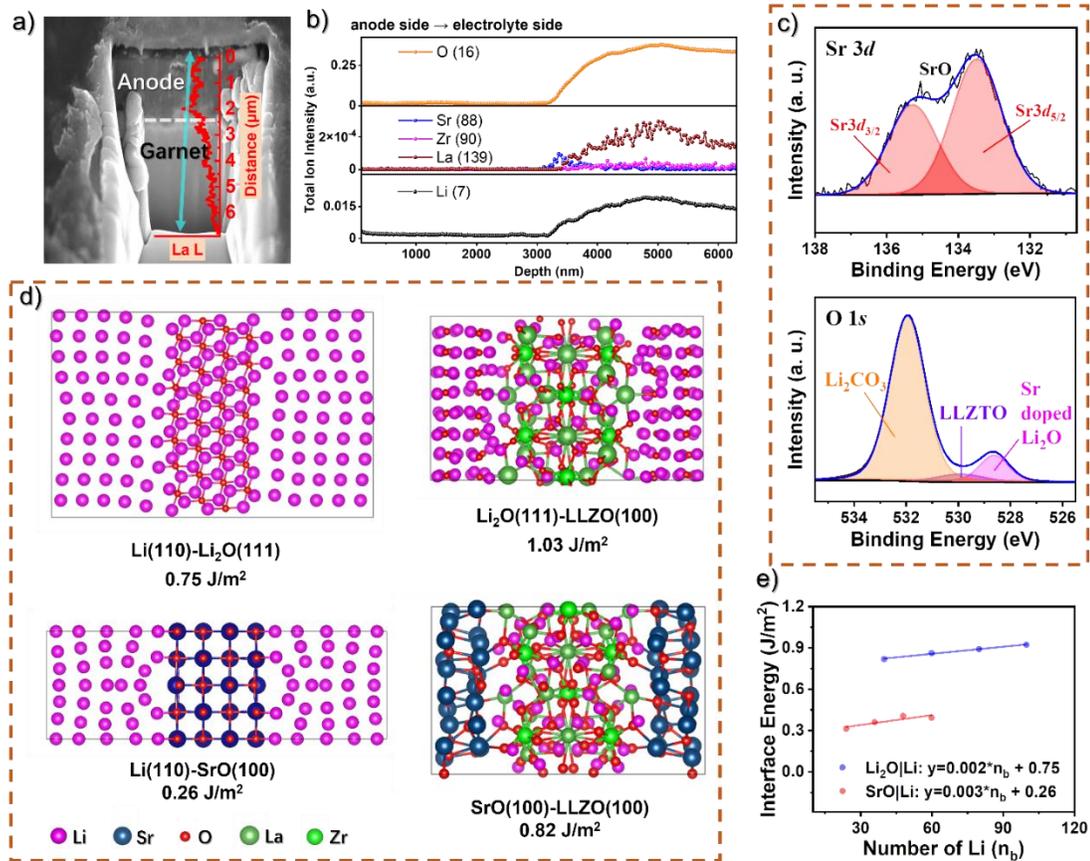
The morphology and element distribution of the cross-section of Li-Sr | LLZTO interfaces were characterized by scanning electron microscopy (SEM). As shown in **Figure 3-1 b-i**, all the Li-Sr | LLZTO interfaces, regardless of the anode composition,

demonstrated seamless contact, confirming the high wettability of Li-Sr alloy against LLZTO. However, the microstructure of the Li-Sr anodes varies for different ratios Li-Sr. The Li-Sr-1% anode showed a monolith metal-like smooth surface while inhomogeneous blocks and granules were found for Li-Sr-5%, Li-Sr-10% and Li-Sr-20% anodes. The morphological variation should be attributed to the different phase-composition of Li-Sr alloy. According to the energy-dispersive X-ray spectroscopy (EDS) mapping, for the low Sr contained alloy (1%), Sr mainly segregates at the interface between LLZTO and the Li anode. The segregation of Sr at the interface is attributed to the high wettability of the Li-Sr alloy to LLZTO due to the strong interaction of Sr with O-atom at the interface.<sup>59,60</sup> As the Sr ratio in the Li-Sr alloy (Figure 3-1 f-h) increases, more Sr-atoms can be found inside the bulk Li anode rather than segregating at the interface. Apparently, the higher ratio of Sr (>5% of Sr) will simultaneously affect the interface contact and the bulk Li anode.



**Figure 3-2** Phase Diagram of the Li-Sr system. The red dash lines mark the Li-Sr-1%, Li-Sr-5%, Li-Sr-10% and Li-Sr-20% composition from right to left.

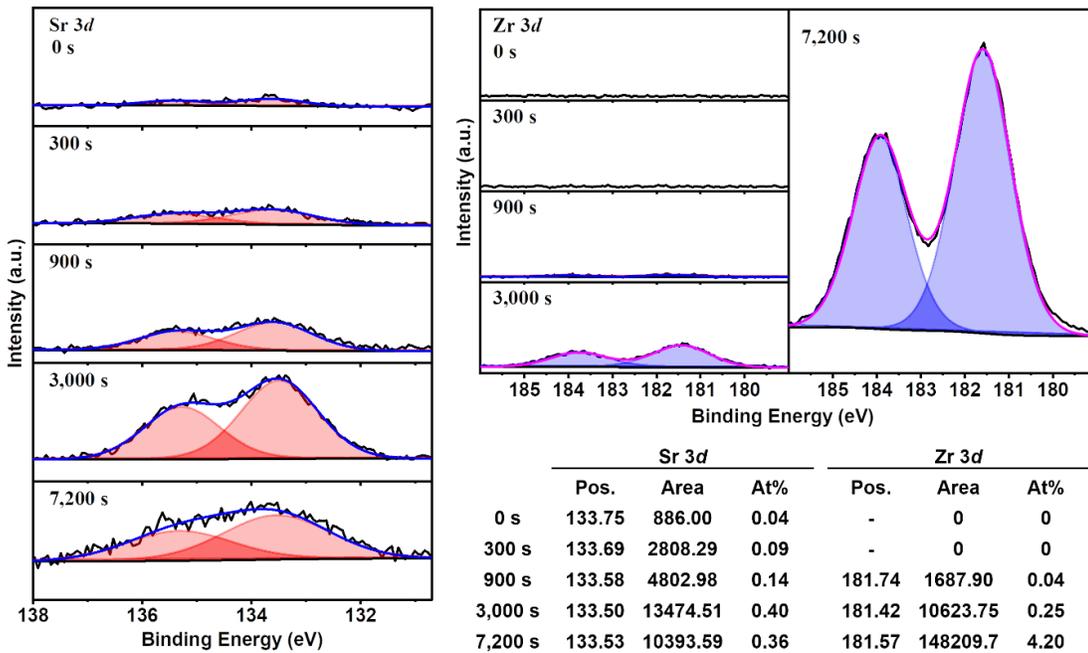
According to the phase diagram in **Figure 3-2**, the equilibrium Li-Sr-1% alloy consists of Li metal and a small amount of  $\text{Li}_{23}\text{Sr}_6$  intermetallic compound.  $\text{Li}_{23}\text{Sr}_6$  can react with trace oxygen in the glove-box forming a lithiophobic Li-Sr-O layer on the Li surface and anchoring to the LLZTO (Figure 1f). With increasing of Sr, the content of  $\text{Li}_6\text{Sr}_{23}$  phase quickly increases and  $\text{Li}_6\text{Sr}_{23}$  will distribute into bulk Li, forming an inhomogeneous composite microstructure (**Figure 3-1 g-i**). For Li-Sr-20% anode, the main component is  $\text{Li}_{23}\text{Sr}_6$  phase (**Figure 3-2**), which has quite different physical and chemical properties compared with Li metal. The morphological and composition variation of the alloys affected the electrochemical performances when serving as anode for SSLBs.



**Figure 3-3 Characterization and calculation of the Li | Garnet interface.** (a) The SEM image of a crater sputtered by the Ga<sup>+</sup> ion beam on the Li-Sr-1% | LLZTO interface showing the cross-sectional surface with an EDS elemental line scanning of the La L along scanning blue line. (b) ToF-SIMS analysis of the Li-Sr-1% | LLZTO interface. (c) The XPS spectra of the Sr 3d and O 1s on the Li-Sr-1% | LLZTO interface with 3,000 seconds of Ar<sup>+</sup> ion gun etching to remove the residual anode metal. The Li<sub>2</sub>CO<sub>3</sub> signals are mainly from the environment. (d) The atomic structures of the Li (110)-Li<sub>2</sub>O (111) interface, the Li<sub>2</sub>O (111)- Garnet (100) interface, the Li (110) | SrO (100) interface and the SrO (100) | Garnet (100) interface, with the corresponding calculated interface energy  $\gamma$  by DFT. (e) Schematic diagram of the bifunctional lithiophilic/lithiophobic interlayer.

The Sr element segregation at Li | LLZTO interface for Li-Sr-1% anode was further characterized using depth-profiling time-of-flight secondary-ion mass spectroscopy (ToF-SIMS). As shown in **Figure 3-3** a, after removing Li-Sr-1% anode from LLZTO with a scraper, the LLZTO surface was sputtered using Ga<sup>+</sup> ion beam. The Li

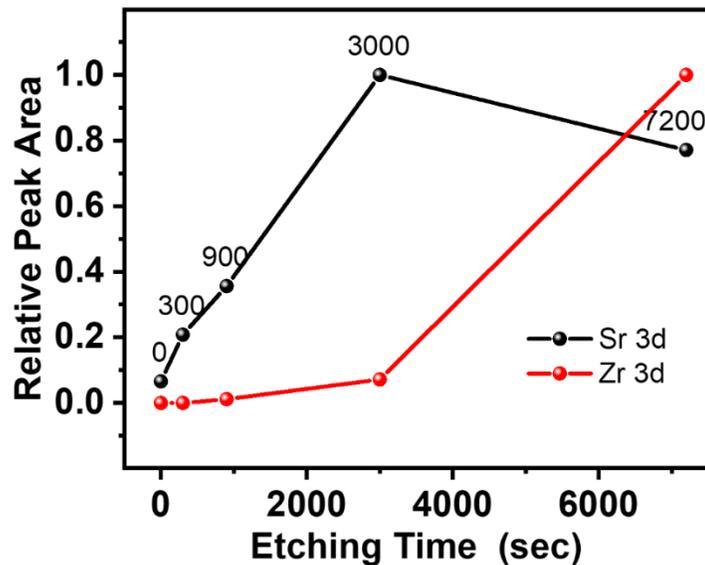
| LLZTO interface can be clearly noticed on the SEM of the crater (marked with a white dash line), which ensures the sputtering depth was deep enough to reach the interface as well as the SSE. The EDS elemental line scanning was conducted on the line marked in blue (**Figure 3-3 a**) and the distribution of the La element (red line in **Figure 3-3 a**) agrees well with the SEM result. Accordingly, the ToF-SIMS analysis in **Figure 3-3 b** shows a clear rise in the distribution of Zr (90), La (139), Li (7) and O (16) ions that are indicating the ion beam sputtering had reached the LLZTO solid electrolyte. Notably, the Sr (88) ion shows a peak right before the LLZTO phase, which validated the segregation of Sr element on the Li | LLZTO interface. The Sr ion enriched layer is around 250 nm thick, according to the ToF-SIMS analysis.



**Figure 3-4** The XPS spectra and the quantification of the Sr 3d and Zr 3d on the Li-Sr-1% | LLZTO interface with Ar<sup>+</sup> ion gun etching at 0, 300, 900, 3000 and 7200 seconds. The atom percentage was calculated based on Li 1s, C 1s, O 1s, La 3d, Ta 4f, Sr 3d and Zr 3d in the survey from 0 to 1200 eV. The y-axis is the relative

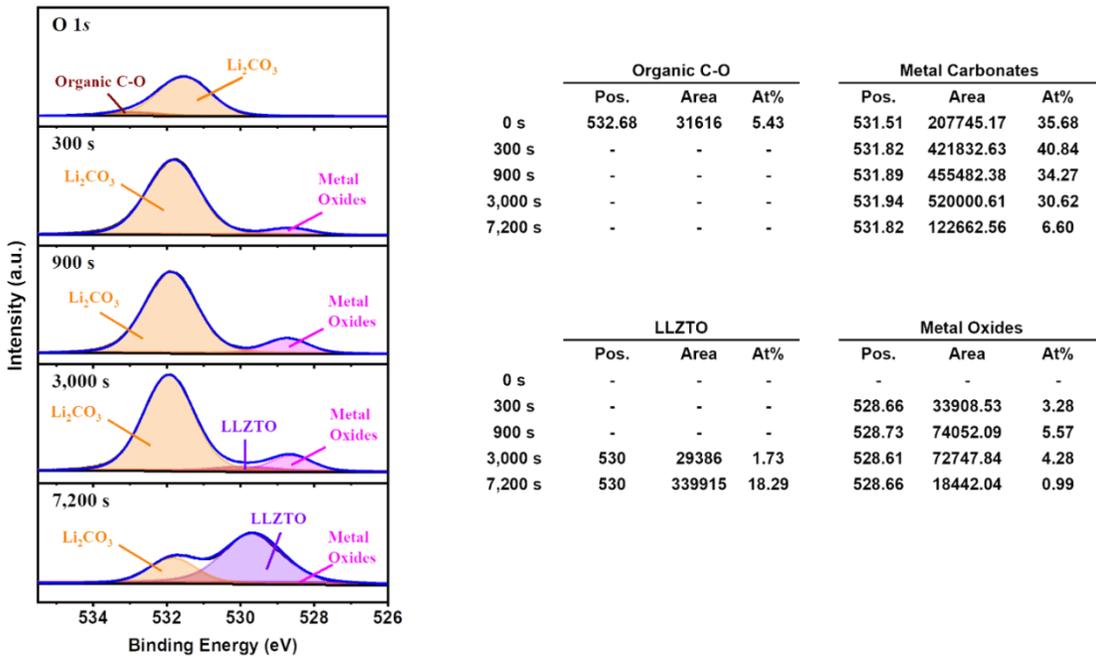
emission intensity (a.u.) that is kept in the same proportion for all Sr 3*d* spectra and all Zr 3*d* spectra respectively.

X-ray photoelectron spectroscopy (XPS) was also conducted with Ar<sup>+</sup> ion gun etching to identify the valence of the Sr element in this layer. As shown in **Figure 3-4** and **Figure 3-5**, Sr 3*d* enriched at the 3,000 seconds' cycle, while after that, a more than 16 times Zr 3*d* amount and a reduced Sr 3*d* amount indicated the etching already reached the LLZTO layer. Therefore, the Li | LLZTO interface is at the 3,000 seconds' cycle, Sr 3*d* and Zr 3*d* here were analyzed in detail. From the Sr 3*d* spectra (**Figure 3-3 c**), the peaks for 3*d*<sub>5/2</sub> and 3*d*<sub>3/2</sub> of SrO<sup>61</sup> located at 135.3 eV and 133.5 eV, respectively. The O 1*s* demonstrated that SrO doped Li<sub>2</sub>O exists on the Li | LLZTO interface (**Figure 3-3 c**). In addition to SrO, LiCO<sub>3</sub> also exists, which may come from atmospheric contamination.



**Figure 3-5** The relative peak area of Sr 3*d* and Zr 3*d* at 0, 300, 900, 3000 and 7200 seconds in the XPS. The Sr 3*d* (interface) and Zr 3*d*(SSE) are set as 1 respectively.

The quantification analysis (**Figure 3-6**) shows that  $\text{Li}_2\text{O} : \text{SrO}$  composition is roughly 9:1.  $\text{Li}_2\text{O}$  is lithiophobic with high interfacial energy of  $0.75 \text{ J/m}^2$  and a high Li dendrite suppression ability.<sup>32</sup> However, the low Li-ion conductivity of  $\text{Li}_2\text{O}$  also induces a large overpotential.<sup>56</sup> Metal oxide doping to  $\text{Li}_2\text{O}$  can be an effective method to reduce the resistance. SrO is one of the very few metal oxides that is relatively stable against Li with an equilibrium potential of  $5.0 \text{ mV vs. Li}$ <sup>62</sup>, similar to LLZO<sup>10</sup>.



**Figure 3-6** The XPS spectra and the quantification of the O 1s on the Li-Sr-1% | LLZTO interface with  $\text{Ar}^+$  ion gun etching at 0, 300, 900, 3000 and 7200 seconds. The atom percentage was calculated based on Li 1s, C 1s, O 1s, La 3d, Ta 4f, Sr 3d and Zr 3d in the survey from 0 to 1200 eV. The y-axis is the relative emission intensity (a.u.) that is kept in the same proportion for all spectra.

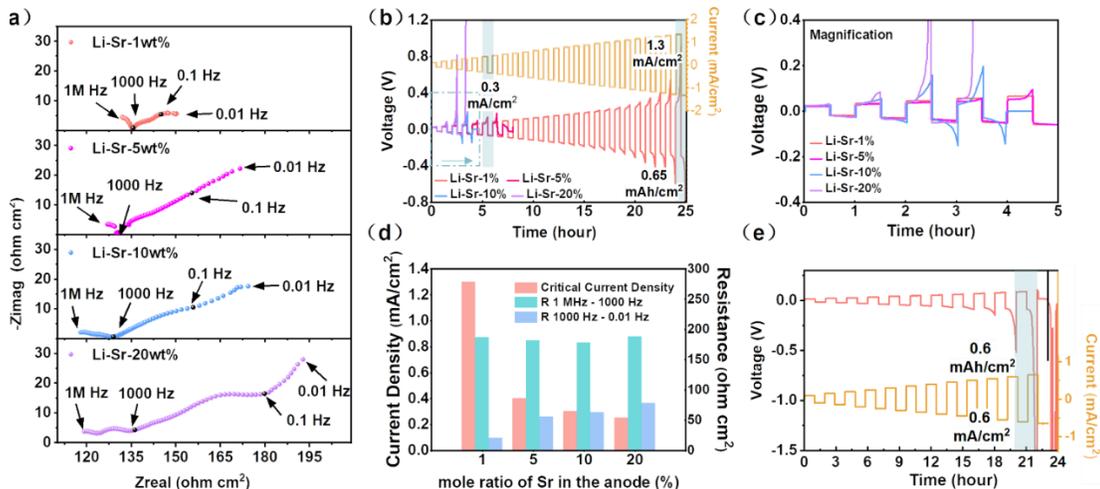
In addition, the thermodynamic calculations were done using HSC-software<sup>63</sup> (**Table 3-1**) and the positive Gibbs energy for the reaction between Li and SrO also verify the relative stability of SrO against Li. Therefore, SrO doped Li<sub>2</sub>O is stable with Li. In addition, SrO doped Li<sub>2</sub>O also enhances the wettability with significantly reduced interface resistance (discussed in the following section) by reducing the interface energy between Li<sub>2</sub>O and LLZTO, as demonstrated by the density functional theory (DFT) calculation. **Figure 3-3 d** demonstrated that Li<sub>2</sub>O is garnet-phobic due to the high interfacial energy of 1.03 J/m<sup>2</sup> with garnet. Since the Li<sub>2</sub>O layer on the molten Li surface is unavoidable even in the glove-box, the molten Li with Li<sub>2</sub>O surface cannot wet the LLZTO. Since SrO has low interface energy with garnet (0.82 J/m<sup>2</sup>) and low interfacial energy against Li (0.26 J/m<sup>2</sup>), SrO doped Li<sub>2</sub>O *functions* as an anchor to bond both the Li anode and the LLZTO, which significantly reduce the interface resistance. In addition, the lithiophobic SrO doped Li<sub>2</sub>O with low electronic conductivity can also suppress the reduction of LLZTO and Li dendrite growth (**Figure 3-3 e**).

**Table 3-1** The theoretical equilibrium potential and the Gibbs energy for the reaction between binary metal oxides and lithium metal. (\*The Gibbs energy for the reaction between Li and the metal oxides ( $nLi + MO_m \leftrightarrow M + nLiO_{m/n}$ ) are calculated using HSC-software<sup>63</sup>.)

$MO_m$	Theoretical equilibrium potential (mV)	$nLi + MO_m \leftrightarrow M + nLiO_{m/n}$ Gibbs energy* at 25 °C (kcal)
Al <sub>2</sub> O <sub>3</sub>	180	-24.179
ZnO	1252	-57.546
SiO <sub>2</sub>	694	-63.540
<b>SrO</b>	<b>5</b>	<b>0.106</b>

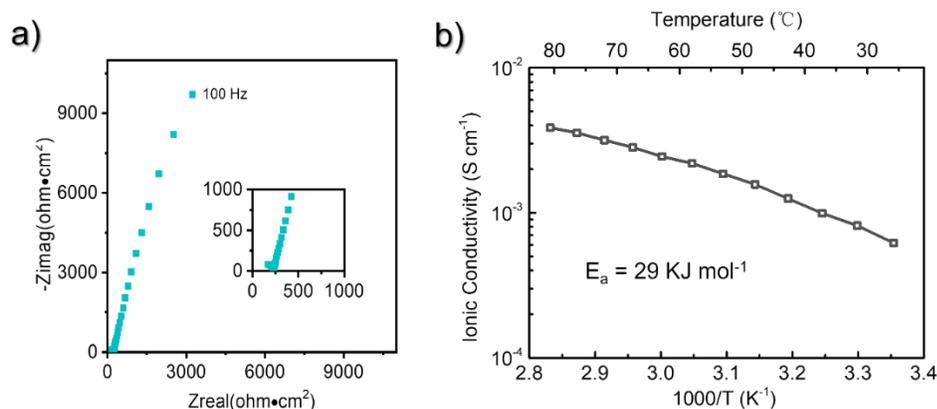
### 3.4 Electrochemical Behavior of Li-Sr / LLZTO / Li-Sr Symmetric Cells

The Li plating/stripping behavior of the Li-Sr alloy anodes with different Li-Sr ratios was evaluated at room temperature using symmetric cells. The interfacial resistance before cycling was firstly measured using electrochemical impedance spectra (EIS). EIS plots (**Figure 3-7 a**) of Li-Sr | LLZTO | Li-Sr cells demonstrated that Li-Sr-1% anode has the lowest impedance, and the total impedance of symmetric cells increase with Sr content in Li. The first semicircle (~1 kHz) of EIS plots is attributed to the total resistance of the LLZTO pellets (bulk and grain boundary), which is about 130-135  $\Omega \text{ cm}^2$  due to the difference of LLZTO pellets, which is consistent with conductivity measurement of LLZTO (**Figure 3-8**) and reported results <sup>64</sup>. The interfacial resistances (1kHz to 0.1Hz) increase with Sr content but they are still much smaller than that of Li | LLZTO | Li cells (**Figure 3-9**). The resistance from 1kHz to 0.01 Hz vastly increases with the increase of Sr content in the anode as 14, 40, 45, and 57  $\Omega \text{ cm}^2$  for Li-Sr-1%, Li-Sr-5%, Li-Sr-10%, and Li-Sr-20% anodes, respectively (**Figure 3-7 d**), indicating that excess  $\text{Li}_{23}\text{Sr}_6$  in bulk Li can reduce the Li atom diffusion.



**Figure 3-7 Electrochemical performance Li-Sr | LLZTO | Li-Sr symmetric cells.** (a) Impedance spectra of the symmetric cells tested at room temperature from 1 MHz to 0.01 Hz. (From top panel to bottom panel are: Li-Sr-1%, Li-Sr-5%, Li-Sr-10% and Li-Sr-1%, Li-Sr-5%, Li-Sr-10% and Li-Sr-20%.) (b) The Li plating/stripping behavior for these cells at a step-increase current for 0.5 h, with (c) a magnified figure for the first 5 cycles. (d) The critical current densities and resistances verse the Sr mole ratio in the anode. (e) The Li plating/stripping behavior for the cell at a step-increase current for 1.0 h.

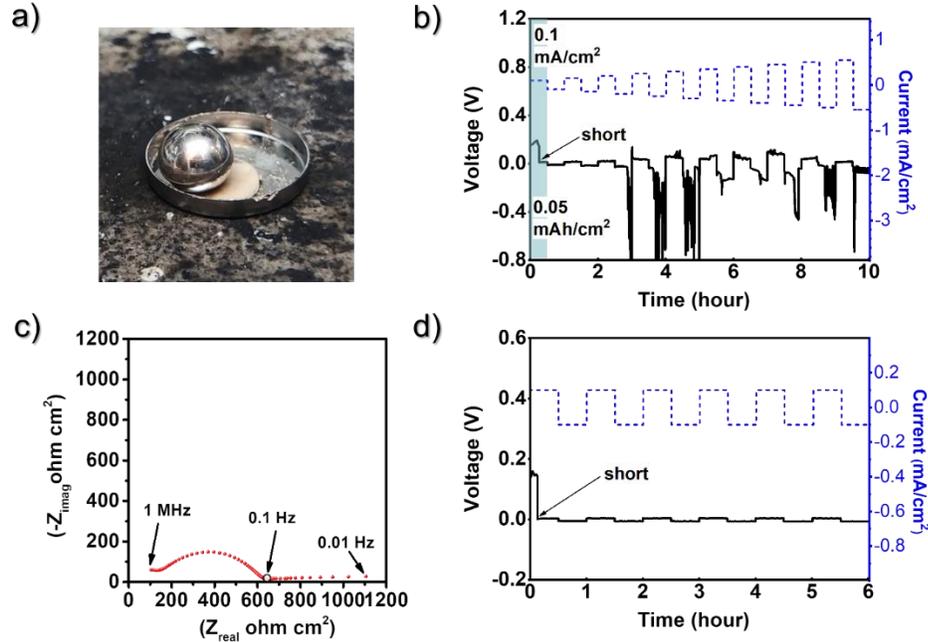
The CCD was evaluated using Li-Sr | LLZTO | Li-Sr cells by a step-increase current for a fixed 0.5 h of Li plating and 0.5 h of Li stripping. As shown in **Figure 3-7 b**, the CCD for Li-Sr-1% cell is 1.3 mA/cm<sup>2</sup> at 0.65 mAh cm<sup>-2</sup>, which is an order of magnitude higher than the CCD for Li | LLZTO|Li (**Figure 3-9**) and is highest among all reported alloy-based anode | LLZTO.<sup>52</sup> Therefore, SrO doped Li<sub>2</sub>O bifunctional layer has a high Li dendrite suppression capability. Nevertheless, the CCD for the cells with Li-Sr-5%, Li-Sr-10%, and Li-Sr-20% anodes are only 0.40, 0.30 and 0.25 mA/cm<sup>2</sup>, which are in line with resistance increase with Sr content in the EIS measurement (**Figure 3-7 d**).



**Figure 3-8** a) The EIS result of the Au | LLZTO | Au cell at 25°C. b) The Arrhenius plot for the Au | LLZTO | Au cell at temperatures from 25°C to 80°C. The data points are the average of the test result of elevated temperature and decreasing temperature.

Detail analysis of Li plating/stripping curves of all Li-Sr anodes shows that a rapid increase in the slope of the voltage profiles at the latest stripping state right before the short circuit. The rapid increase of voltage can be induced by void formation. The void formation reduced the contact area at Li | LLZTO, which increases the local current density, thus reducing the CCD. For example, for Li-Sr-1% anode, the transformation from the flat voltage plateau to drastic polarization did not happen until a current density of  $\sim 1 \text{ mA/cm}^2$ , while for the other three conditions the apparent potential boost occurred at a much lower current of  $0.1 \text{ mA/cm}^2$  since  $\text{Li}_{23}\text{Sr}_6$  in bulk Li may reduce the Li atom diffusion (**Figure 3-7 c**). When the Li plating/stripping time was extended from 1.0 h to 2.0 h, CCD of Li-Sr | LLZTO | Li-Sr cell was decreased from  $1.3 \text{ mA cm}^{-2}$  (**Figure 3-7 b**) to  $0.6 \text{ mA/cm}^2$  (**Figure 3-7 e**), while the capacity at 1.0 h of plating and stripping time before short-circuit is similar to the capacity of  $0.65 \text{ mAh/cm}^2$  measured at a short time of 0.5h (**Figure 3-7 b**), indicating

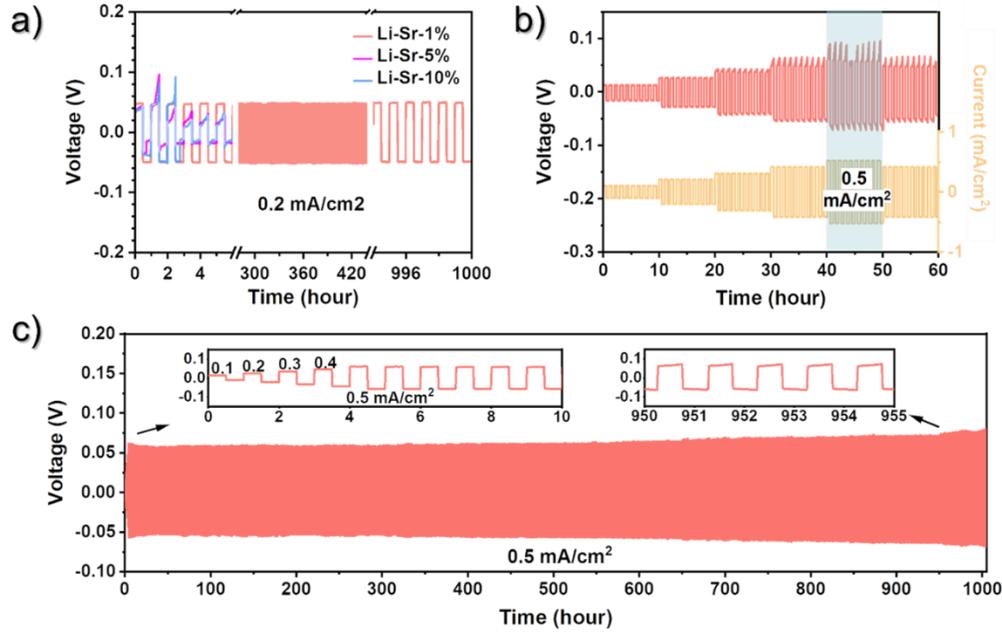
that the amount of the transported Li species controlled the void formation and also Li dendrite growth for the Li-Sr-1% anode.



**Figure 3-9** (a) Digital photographs showing attaching the Li onto garnet LLZTO pellet. (b) The Li plating/stripping behavior of the Li | LLZTO | Li symmetric cell at a step-increase current for 0.5 h each half-cycle at room temperature. (c) Impedance spectra of the Li | LLZTO | Li symmetric cell tested at room temperature from 1 MHz to 0.01 Hz. (d) Cycling performance of Li | LLZTO | Li symmetric cell at 0.1 mA/cm<sup>2</sup>.

The cycling stability of Li-Sr | LLZTO | Li-Sr symmetric cells under a constant current of 0.2 mA/cm<sup>2</sup> and capacity of 0.1 mAh/cm<sup>2</sup> were also investigated. As exhibited in **Figure 3-10** a, the Li-Sr-1% | LLZTO | Li-Sr-1% symmetric cell demonstrated an excellent stability for 1,000 cycles with a neat and flat potential profile. In contrast, an intense polarization occurs in the Li-Sr-5% and Li-Sr-10% cells and follows with a short-circuit within the first five cycles. Even when current density increases to 0.5 mA/cm<sup>2</sup>, the Li-Sr-1% | LLZTO | Li-Sr-1% symmetric cell

still shows super cycling stability without any intense polarization for 1,000 cycles (Figure 3-10 c), which is one of the best among reported planar garnet type solid-state electrolytes work at room temperature (Table 3-2).



**Figure 3-10** Cycling stability of Li-Sr | LLZTO | Li-Sr symmetric cells. (a) Long-term cycling performance at 0.2 mA/cm<sup>2</sup> with different Li-Sr anode. (b) Rate performance of Li-Sr-1% | LLZTO | Li-Sr-1% symmetric cell from 0.1 mA/cm<sup>2</sup> to 0.5 mA/cm<sup>2</sup>. (c) long-term cycling performance of Li-Sr-1% | LLZTO | Li-Sr-1% symmetric cell at 0.5 mA/cm<sup>2</sup>. Inset is the magnification of the voltage profiles of 1-10 cycles and 950-1000 cycles.

**Table 3-2** Reported (2018-2021) cycling current, capacity and time for planar garnet type solid-state electrolytes at room temperature/25°C/30°C. (Ranking in descending order of cycling capacity)

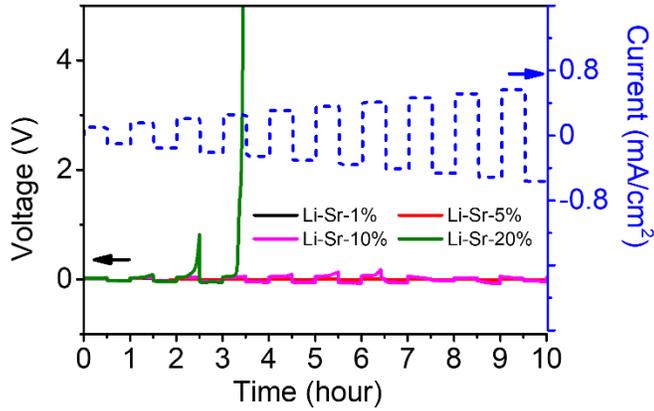
Composition	Methods	Cycling Current (mA·cm <sup>2</sup> )	Cycling Capacity (mAh·cm <sup>2</sup> )	Cycling Time (hour)	Ref.
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Sr bifunctional layer	0.5	0.25	1,000	This work
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.45</sub> Ta <sub>0.55</sub> O <sub>12</sub>	ultrafast sintering w/ Li <sub>3</sub> N Filler	0.5	0.25	160	Acs Energy Lett. 6, 3753–3760 (2021).
Li <sub>6.28</sub> Al <sub>0.24</sub> La <sub>3</sub> Zr <sub>2</sub> O <sub>12</sub>	Li–Zn alloy anode	0.35	0.175	2,200	Acs Appl Energy Mater. 3, 9010–9017 (2020).
Li <sub>5.9</sub> Al <sub>0.2</sub> La <sub>3</sub> Zr <sub>1.75</sub> W <sub>0.25</sub> O <sub>12</sub>	Graphite interface	0.3	0.15	1,000	Acs Energy Lett. 3, 1212–1218 (2018).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Li–C composite	0.3	0.15	250	Advanced Materials. 31, 1807243 (2019).
Li <sub>6.4</sub> La <sub>3</sub> Zr <sub>1.4</sub> Ta <sub>0.6</sub> O <sub>12</sub>	SnO <sub>2</sub> coating	0.2	0.1	650	J. of Power Sources. 420, 15-21 (2019).
Li <sub>6.28</sub> La <sub>3</sub> Zr <sub>2</sub> Al <sub>0.24</sub> O <sub>12</sub>	PVDF-PEO	0.1	0.1	600	J Mater Chem A. 9, 4018–4025 (2021).
Li <sub>6.6</sub> La <sub>3</sub> Zr <sub>1.6</sub> Ta <sub>0.4</sub> O <sub>12</sub>	Acid Etching	0.2	0.1	200	ACS Appl. Energy Mater. 2, 6720–6731(2019).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Nb coating	0.5	0.1	52	Rare Metals. 37, 473-479 (2018).
Li <sub>6.5</sub> La <sub>2.5</sub> Ba <sub>0.5</sub> ZrNbO <sub>12</sub>	Ionic liquid	0.2/0.3	0.05/0.075	92/30	Small. 16, 2000279 (2020).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Cu <sub>3</sub> N coating	0.1	0.05	1,000	Energy & Environmental Science. 13, 1, 127-134 (2020).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Li <sub>3</sub> N coating	0.1	0.05	210	Nano Lett. 18, 11, 7414–7418 (2018)
Li <sub>7</sub> La <sub>2.75</sub> Ca <sub>0.25</sub> Zr <sub>1.75</sub> Nb <sub>0.25</sub> 5O <sub>12</sub>	Ag coating	0.1	0.05	100	J Power Sources. 419, 91–98 (2019).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.45</sub> Ta <sub>0.55</sub> O <sub>12</sub>	rapid sintering w/ Al <sub>2</sub> O <sub>3</sub> coating	0.2	0.033	300	Mater Today. 42, 41–48 (2021).
Li <sub>6.28</sub> Al <sub>0.24</sub> La <sub>3</sub> Zr <sub>2</sub> O <sub>12</sub>	Au coating w/ thermally evaporated Li	0.03	0.0125	70	J Power Sources. 396, 764–773 (2018).

The rate performance of the Li-Sr-1% | LLZTO | Li-Sr-1% symmetric cell was tested at a step-increase current of 0.1, 0.2, 0.3, 0.4, 0.5 mA/cm<sup>2</sup> for 10 cycles at each current density and then move back to 0.4 mA/cm<sup>2</sup> (**Figure 3-10 b**). The Li plating/stripping curve at 0.4 mA/cm<sup>2</sup> before and after increasing the current is identical, demonstrating a stable Li-Sr | LLZTO interface during cycling at different currents.

### 3.5 The Mechanism for the Intense Polarization of Li-Sr | LLZTO | Li-Sr Cells

As shown in **Figure 3-7 c** and **Figure 3-10 a**, in the first few cycles, a flat and similar potential profile was found for all cells. However, the polarization quickly increases for Li-Sr anodes with Sr content  $\geq 5\%$ , as demonstrated by either an increase of current density or constant current cycling. The interpretation of this strong polarization (**Figure 3-11**) is crucial for the understanding of the failure mechanism. As the current density increases in a linear step in the CCD test, the ionic transportation inside SSEs should also render linear overpotential according to the Nernst-Planck equation, which is not the case for the intense polarization. The increase in Li plating/stripping overpotential at the latest Li plating/stripping stage can potentially be attributed to (1) phase transformation at Li | LLZTO interface between Li<sub>23</sub>Sr<sub>6</sub> and Li<sub>2</sub>Sr<sub>3</sub> with different lithiation/delithiation potential (**Figure 3-2**) because the Li<sub>23</sub>Sr<sub>6</sub> phase may change to Li<sub>2</sub>Sr<sub>3</sub> in Li stripping process, (2) void formation due to reduced Li atom diffusion by Li<sub>23</sub>Sr<sub>6</sub> phase in bulk Li, and (3)

formation of cracks in the bulk Li-Sr anodes due to the large volume changes during Li plating/stripping.

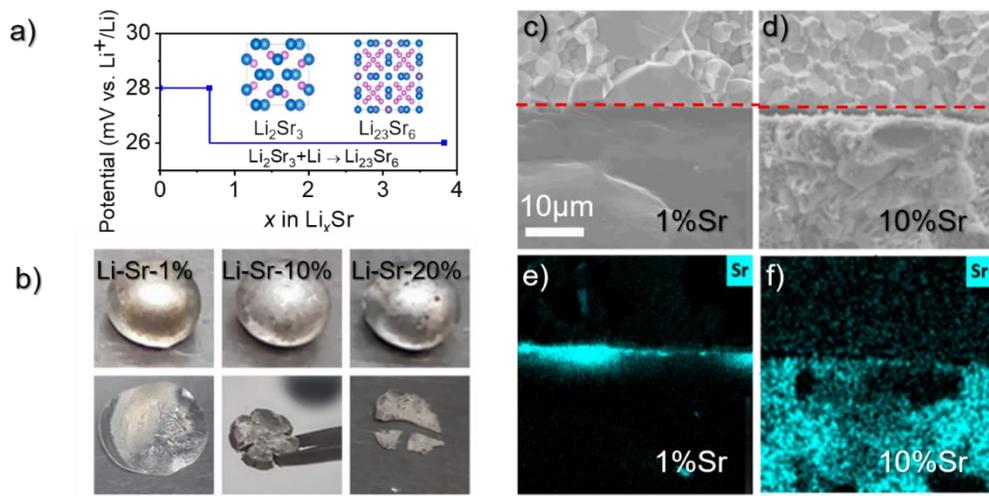


**Figure 3-11** The enlarged image for **Figure 3-7 b**. The Li plating/stripping behavior for these cells at a step-increase current for 0.5h.

The boosting overpotential can be a sign of overcoming a high energy barrier. We first calculated the equilibrium potentials of  $\text{Li}_{23}\text{Sr}_6$  and  $\text{Li}_2\text{Sr}_3$  using DFT since the  $\text{Li}_{23}\text{Sr}_6$  phase will convert into  $\text{Li}_2\text{Sr}_3$  during Li stripping. The equilibrium potentials of  $\text{Li}_2\text{Sr}_3$  and  $\text{Li}_{23}\text{Sr}_6$  are 27.8 mV and 25.7 mV, respectively (**Figure 3-12 a**). The 2.0 mV potential difference cannot cause a significant potential increase at the latest Li stripping state right before short-circuit.

The void formation at Li | LLZTO interface may be responsible for the polarization at the latest Li stripping stage, where the Li vacancy diffusion inside the alloy electrode cannot keep the pace of the current increasing.<sup>39,50</sup> The void evolution is closely related to the Li atom diffusivity in the bulk Li, lithiophilic/lithiophobic property at Li-Sr | SrO doped  $\text{Li}_2\text{O}$  | LLZTO interface. A high CCD of 1.3 mA/cm<sup>2</sup> for Li-Sr-1%

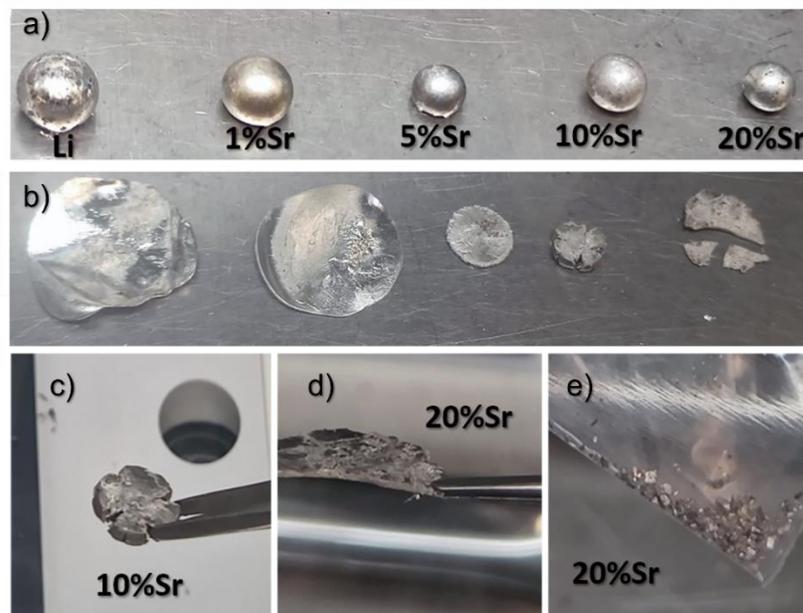
anode at a high capacity of 0.65 mAh/cm<sup>2</sup> is attributed to the bifunctional SrO doped Li<sub>2</sub>O interlayer that bonds Li to Li<sub>2</sub>O and also reduces the interface energy at Li<sub>2</sub>O/LLZTO, decreasing the interface resistance and also suppressing Li dendrite growth. With the increasing of Sr content in Li-Sr anodes, a large amount of Li<sub>23</sub>Sr<sub>6</sub> phase is distributed inside Li, reducing the Li diffusivity, thus forming voids at the early stage of Li stripping thus a low CCD.



**Figure 3-12** Electrochemical and mechanical stability of Li-Sr anodes and Li/LLZTO interface stability. (a) DFT calculation for the equilibrium potentials of Li-Sr alloys. (b) Digital pictures of Li-Sr alloys with significantly different ductility and malleability after press. (c-f) Morphologies and Sr elemental mapping of Li-Sr | SSE interface after 2 cycles with a current density of 0.2 mA/cm<sup>2</sup> and capacity of 0.1 mAh/cm<sup>2</sup>.

The cracks formed inside the Li-Sr bulk due to the poor mechanical property of Li<sub>23</sub>Sr<sub>6</sub> phase may also contribute to the low CCD. The brittle Li<sub>23</sub>Sr<sub>6</sub> phase in Li-Sr anodes will crack during the significant volume change in Li plating/stripping, which also blocks the Li atom diffusion to interface and reduce the contact area<sup>49,51</sup> The

deformation capability of Li-Sr anodes with different Sr content was evaluated using a facile pressing test. As shown in **Figure 3-12 b**, the flow and elastic behavior exhibit noteworthy differences by pressing the Li metal ball, as well as the Li-Sr-alloy balls under 2 MPa. The Li-metal and the Li-Sr-1% alloy demonstrate well ductility and form thin foils with a smooth surface and metallic luster. While the Li-Sr-5%, 10% and 20% alloys render wrinkles, cracks gaps, and even fracture.

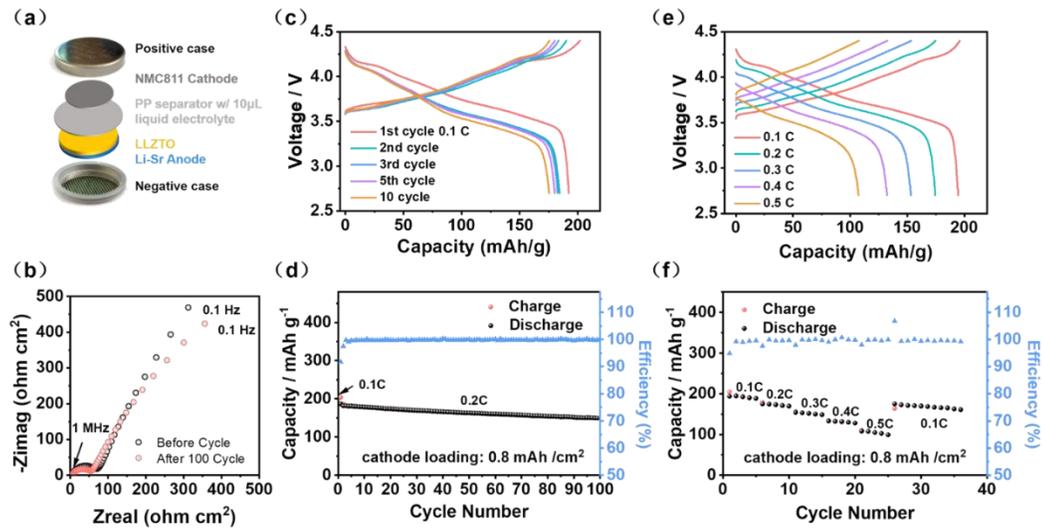


**Figure 3-13** Digital pictures of Lithium anode with significantly different ductility and malleability. (a) The electrodes before pressing. (b) The electrodes after pressing. (c) The magnification of the 10% Sr in Li, (d) the fracture of 20% Sr in Li, and (e) the shattered small pieces of the 20% Sr in Li.

As shown in Error! Reference source not found., the pressed Li-Sr-20% has a sharp fracture, and part of it even shattered into small pieces. Although a precise or quantitative study on the deformation property is in absence, the contract is distinct.

A significantly worse ductility and malleability can be anticipated with the increase of

the Sr ratio in the Li-Sr alloy, which would introduce more detrimental cracks during cycling. The postmortem SEM was taken after the cycling test to analyze the morphology and element distribution evolution of the cross-section of Li-Sr | LLZTO interfaces. As shown in **Figure 3-12** c-f, after Li plating/stripping cycles, Sr is still enriched at Li | LLZTO interface without being pushed away due to the high stability of the SrO anchor, which is totally different from those electron-conducting alloy coating. However, gaps can be clearly seen between the LLZTO and anode for the Li-Sr 10% and 20% cells, as evidence of void formation and contact loss. Cracks and holes also appeared in the Li-Sr anode bulk with Sr >5%.

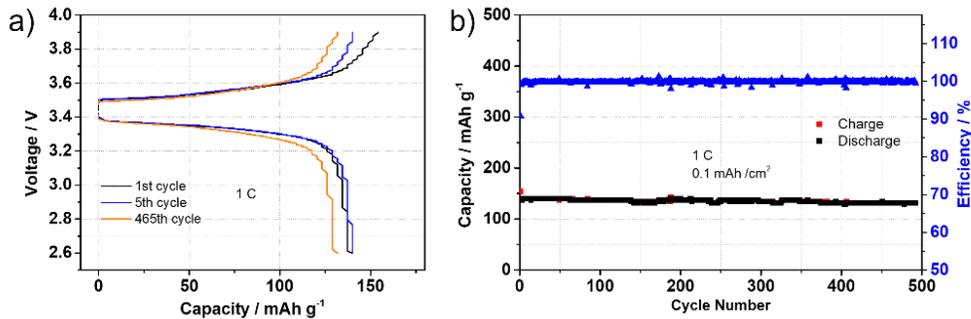


**Figure 3-14 Electrochemical performance of Li-Sr-1% | LLZTO | NMC811 cells.** a) Schematic diagram of a Li-Sr | LLZTO | NMC811 cells. b) Impedance spectra of the cell tested at room temperature before (black circle) and after 100 cycles (red circle). c, d) The cycle performance for the cell at 0.2 C with cathode loading of 0.8 mAh / cm<sup>2</sup> (0.1 C for the first cycle for activation). e, f) The rate performance for the cell at stepped C-rate.

### 3.6 Electrochemical Behavior of the Proof-of-Concept Li-Sr | LLZTO |

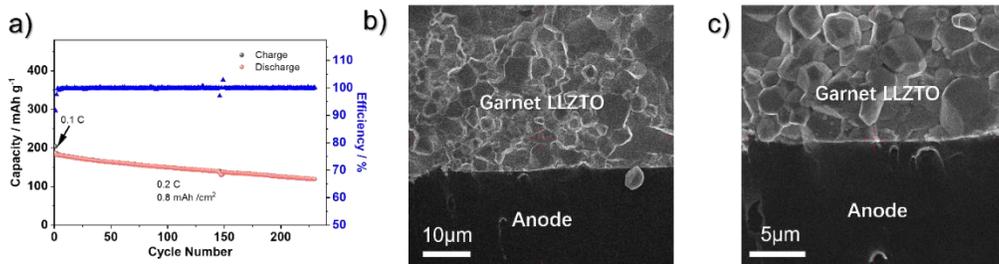
#### LiNi<sub>0.8</sub>Mn<sub>0.1</sub>Co<sub>0.1</sub>O<sub>2</sub> (NMC811) Cells

Since Li-Sr-1% anode shows the high CCD, high cycling stability with LLZTO electrolyte, it was selected for additional cell evaluation. Li-Sr-1% | LLZTO | LiNi<sub>0.8</sub>Mn<sub>0.1</sub>Co<sub>0.1</sub>O<sub>2</sub> (NMC811) cells were assembled as the schematic diagram demonstrated in **Figure 3-14 a**, with liquid electrolyte wetted cathode interface (**Table 3-3**) to eliminate the cathode side contact influence. The cell provides 192 mAh/g at 0.2 C from 2.7 V to 4.3 V (**Figure 3-14 c**) with a capacity retention of 82% after 100 cycles (**Figure 3-14 d**). The EIS plots (**Figure 3-14 b**) before and after 100 cycles indicate a small resistance reduction without short-circuiting. The initial Coulombic efficiency of 91.68% at 0.1C and average Coulombic efficiency of 99.82% for the rest cycles at 0.2C were displayed. The cell delivered discharge capacities of 192.1, 174.4, 153.0, 132.2 and 107.0 mAh/g at 0.1, 0.2, 0.3, 0.4 and 0.5C (**Figure 3-14 e**). The capacity quickly recovered to 175.2 mAh/g when the current was set back to 0.1C (**Figure 3-14 f**).



**Figure 3-15** Electrochemical performance of Li-Sr-1% | LLZTO | LiFePO<sub>4</sub> cells. The loading of the cathode is 0.1 mAh cm<sup>-2</sup>.

Long cycling of 500 cycles for Li-Sr | LLZTO | LiFePO<sub>4</sub> cell is also presented in **Figure 3-15**. These results indicate Li-Sr-1% as a stable anode (**Figure S10**) against LLZTO during cycling. However, further optimizations of liquid-free cathode interface engineering are still needed to realize practical applications of all-solid-state lithium metal batteries (ASSLB).



**Figure 3-16** a) The cycle performance for the same cell (Li-Sr-1% | LLZTO | NMC811) in **Figure 3-14** d showing the condition before cell test termination at the 230<sup>th</sup> cycle. b, c) Morphologies of Li-Sr | SSE interface after 230 cycles.

### 3.7 Conclusion

Solid-state Li metal batteries face two critical challenges of Li dendrite growth and high interface resistance. To suppress Li dendrite growth, interface should be lithiophobic (dendri-phobic), while low interface resistance requires a lithiophilic (wetting) interface. The dilemma between interface wetting and dendrite-phobic was solved with a unique combination of strontium and *in situ* formed SrO, which facilitate a bifunctional lithiophilic/lithiophobic interlayer combining low interface resistance and high dendrite suppression capability.

**Table 3-3** Reported cathode loading and wetting method, cycling rate and time for the prove-of-concept cells in planar garnet type solid-state electrolytes. (Operating at room temperature/25°C without further notice)

Composition	Anode Methods	Cathode and Loading (per cm <sup>2</sup> )	Wetting Method	Cycling rate and Cycles	Ref.
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Sr bifunctional layer	NMC811, 0.8 mAh	liquid electrolyte (10 μL)	0.2C, 100	This work
		LFP, 0.1 mAh		1C, 500	
Li <sub>5.9</sub> Al <sub>0.2</sub> La <sub>3</sub> Zr <sub>1.75</sub> W <sub>0.25</sub> O <sub>12</sub>	Graphite interface	NCM523, 0.9 mg	slurry w/ ionic liquid	0.5C, 500	Acs Energy Lett. 3, 1212–1218 (2018).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Li-C composite	LFP, --	PVDF-HFP film w/ 10 μL liquid electrolyte	0.5C, 100	Advanced Materials. 31, 1807243 (2019).
Li <sub>6.5</sub> La <sub>2.5</sub> Ba <sub>0.5</sub> ZrNbO <sub>12</sub>	Ionic liquid	LFP, 2.5mg	ionic liquid (2 μL)	0.05 mA cm <sup>-2</sup> , 45	Small. 16, 2000279 (2020).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Cu <sub>3</sub> N coating	LCO, 2mg	slurry w/ ionic liquid	0.2C, 300	Energy & Environmental Science. 13, 1, 127-134 (2020).
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Li <sub>3</sub> N coating	LFP (40 °C), 2mg	slurry w/ PEO and acetonitrile	0.1 mA cm <sup>-2</sup> , 200	Nano Lett. 18, 11, 7414–7418 (2018)
Li <sub>7</sub> La <sub>2.75</sub> Ca <sub>0.25</sub> Zr <sub>1.75</sub> Nb <sub>0.25</sub> 5O <sub>12</sub>	Ag coating	LCO, 0.45mg	slurry w/ ionic liquid	0.2C, 100	J Power Sources. 419, 91–98 (2019).
Li <sub>6.28</sub> Al <sub>0.24</sub> La <sub>3</sub> Zr <sub>2</sub> O <sub>12</sub>	Au coating w/ thermally evaporated Li	LCO, --	liquid electrolyte (10 μL)	0.05C, 70	J Power Sources. 396, 764–773 (2018).
Li <sub>7</sub> La <sub>2.75</sub> Ca <sub>0.25</sub> Zr <sub>1.75</sub> Nb <sub>0.25</sub> 5O <sub>12</sub>	Al <sub>2</sub> O <sub>3</sub> coating	LFMO, --	a tiny amount of liquid electrolyte	0.1 C	Nat Mater. 16, 572–579 (2016).

SrO is stable with Li and facilitates the contact between anode and LLZTO by reducing the interface energy between Li<sub>2</sub>O and LLZTO. It serves as an anchor which let the Li to be deposited between the interfacial layer and the anode that (1) suppress

the lithium nucleation and dendrite propagation on SSE; (2) keep the interfacial layer stable on the anode | SSE interface instead of being pushed away; (3) reduce the resistance of the Li<sub>2</sub>O lithiophobic layer but kept its lithiophobic nature; (4) having high affinity to garnet. An optimized Li-1% Sr alloy anode | LLZTO can synergistically achieve a low interface resistance and high Li dendrite suppression capability, as evidenced by a high CCD of 1.3 mA/cm<sup>2</sup> at 0.65 mAh/cm<sup>2</sup> and a stable cycle of 1,000 cycles (1,000 h) under 0.5 mA/cm<sup>2</sup> at room temperature. This work provides a new strategy and sheds light on enhancing the performance of SSLBs.

# Chapter 4 High Interface Energy Enabled Highly Stable Garnet-based Lithium Metal Solid-State Batteries

## 4.1 Introduction

Solid-state lithium metal battery (SSLB) is considered as one of the most promising next generation batteries to power the growing numbers of electric vehicles, owing to its high energy density and high safety origin from the lithium metal anode (LMA) and solid-state electrolyte (SSE) respectively. Among various SSEs, garnet-type Li-ion conductor  $\text{Li}_7\text{La}_3\text{Zr}_2\text{O}_{12}$  (LLZO) and its variants, are been extensively developed for their high ionic conductivity ( $8 \times 10^{-4} \text{ S cm}^{-1}$  with Nb doping at room temperature), low electronic conductivity ( $\sim 10^{-8} \text{ S cm}^{-1}$  at room temperature), wide electrochemical window, and high shear modulus over 100 GPa that was believed able to block the dendrite growth theoretically.

The most intuitive difference between SSE and its previous generation counterpart liquid electrolyte is the lack of flowing medium that adapts the shape changes and keeps a continuous conducting channel. Thus, the priority issue to be fixed for SSLB is to facilitated the solid-solid contact between the solid-electrolyte and the electrode. What makes the matter worse for the LMA is its nature of one monolithic piece instead of particles. This means a 3D contact by mixing SSE particles with active material particles in the electrodes like most cathodes and silicon anode can do will no longer be a solution for lithium metal. Instead, the contaare between the plane SSE

and plane LMA is in a 2D geometry that is more vulnerable once voids or cracks forms and lead directly to the loss of contact. Tremendous efforts had been made in the past decade to facilitate and maintain the solid-solid contact between the SSE and the LMA aiming at diminish or even eliminating the interfacial impedance. Added-on external pressure works but up to hundreds MPa pressure is not practical for the application of SSLMB in real life scenarios such as electric vehicles. Making the metal electrodes flowable such as Na-K alloy and liquid lithium solution also tackles the problem intrinsically, but the choices are extremely limited<sup>65</sup> for room temperature flowable electrodes. In particular, even for the garnet SSE with a nature of rigidity of ceramic and non-wettability with lithium, the interfacial impedance can be reduced from thousands to single-digit  $\Omega \text{ cm}^2$  with proper interface engineering.

Recent studies have demonstrated that the interface impedance can be almost eliminated in SSLB. However, the dendrite suppression capability and cycling stability are still far from the requirement of the practical applications. This reminds us the “interface impedance” may not be the golden target and the critical properties of the interface towards dendrite suppression instead of solely low impedance demands a more clear determination. Here, we screening the interface candidates aiming at properties directly contributes to the dendrite suppression: 1) the Gibbs energy for the reaction between Li and the candidate (for metal oxides:  $nLi + MO_m \leftrightarrow M + nLiO_{m/n}$ ) should be as positive as possible; 2) the interface energy against lithium should be as high as possible. The former guaranteed a thermodynamic stable interface that keeps the designed metal oxides interlayer

instead of being reduced by lithium upon cycling. The latter established a large energy barrier for lithium dendrite to pierce through against the dynamic energy input from overpotential and volume changing during the lithium stripping and plating.

In this study, we present a LiYO<sub>2</sub> as a highly thermodynamical stable candidate for the interface between SSE and LMA based on the critical properties of aforementioned Gibbs energy and interface energy. Li | Li<sub>6.5</sub>La<sub>3</sub>Zr<sub>1.5</sub>Ta<sub>0.5</sub>O<sub>12</sub> (LLZTO) interface with LiYO<sub>2</sub> as the interlayer was successfully established, which endows the symmetric cells a high critical current density of 1.15 mA cm<sup>-2</sup>, a critical capacity of 4.2 mAh cm<sup>-2</sup> at 0.1 mA cm<sup>-2</sup> and a long cycle life of 600 cycles under 0.5 mA cm<sup>-2</sup>/0.25 mAh cm<sup>-2</sup>. This work represents a significant advancement in designing the interface for SSE | LMA by providing critical parameters of the interface, which would advance the design of high performance SSLBs.

#### 4.2 Experimental

The Li-Y alloy anode was prepared by a molten lithium method in a glove-box. Initially, lithium foil (Alfa) and Y power (Sigma, 99.5%) was mixed in a shallow stainless-steel crucible under 350°C with weight ratio of 7:1, 3:1 and 1:1. The molten alloy will be stirred for more than 10 minutes to ensure a homogeneous reaction. The as-synthesized LLZTO electrolyte pellet was cleaned by mechanical dry-polishing using 400 grits, 1500 grits and 3000 grits sandpapers consequently. The polished LLZTO pellet was directly immersed in the crucible with the molten alloy and the

anode will be attached on the LLZTO pellet within around 10 seconds. After cooling down to room temperature, the residual metal attached on the side surface of LLZTO pellet will be polished off with sandpaper.

XPS was conducted on a high sensitivity Kratos Axis 165 X-ray photoelectron spectrometer with Al K $\alpha$  radiation. All binding energy values were referenced to the C1s peak to 284.8 eV. The surface of the sample (anode side) after scraper-cleaning is defined as the 0 depth. The sample was directly moved from Ar atmosphere to the XPS chamber with a vacuum transfer container to avoid exposure to the air. Peak fitting and relative atomic percentage estimation were done using CasaXPS software.

#### 4.3 Design of the Interlayer Towards Dendrite Suppression

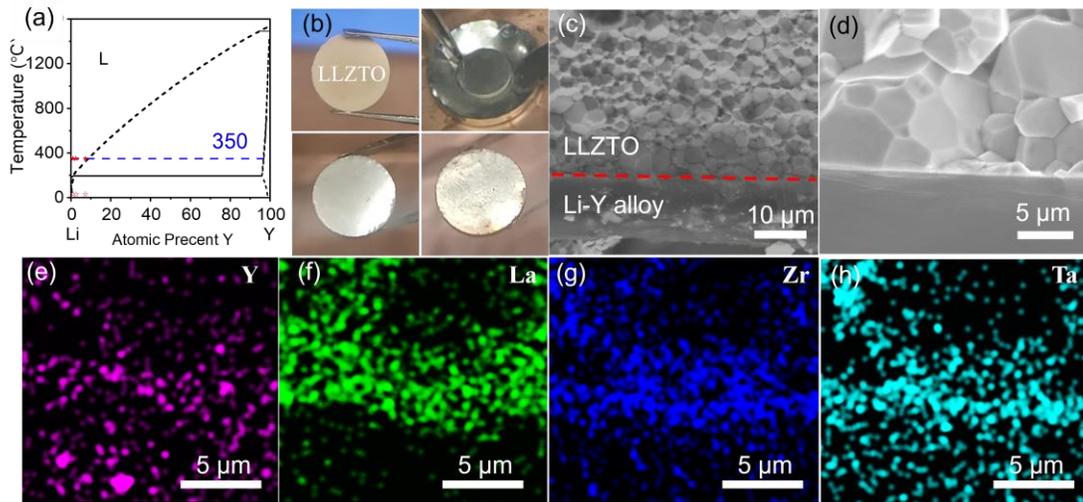
Li-M alloy (M = metal elements) can effectively increase the wettability with the garnet SSE. However, the formed electronically conducting interface causes directly contact between the e<sup>-</sup> and the SSE and let the lithium plating happen right on top of the SSE. This have two potential hazes: 1) the designed interface would be push away from the surface by the newly plated lithium and the interface will be invalid upon cycling; 2) the accumulated electron near the SSE can form a negative electric field and force the Li<sup>+</sup> expulse out of the bulk SSE to form lithium metal dendrite.<sup>66</sup> Thus, as mentioned earlier we aims on an interface of metal oxide ( $MO_m$ ) that contract a ion or ion/electron mix interface.

To stay spatially stable against being pushed backwards is not enough for a successful IL. Thermodynamically stability of  $MO_m$  against being reduced by lithium metal to  $M$  is another key to keep the interface layer stable upon cycling. According to the theoretical equilibrium potential for the reaction between binary metal oxides and lithium metal (calculated from the Gibbs energy for the reaction between Li and the metal oxides ( $nLi + MO_m \leftrightarrow M + nLiO_{m/n}$ )), and Gibbs free energy for the formation ( $\Delta_f G$ ) of the metal oxides (**Table 4-1**), the relatively stability against Li can be preliminarily estimated.  $Y_2O_3$  is one of the very few metal oxides that is stable against Li with a negative equilibrium potential, which inspires us to dope Y into the lithium metal to form a thermodynamically stable interlayer.

**Table 4-1** The theoretical equilibrium potential for the reaction between binary metal oxides and lithium metal, and Gibbs free energy of formation ( $\Delta_f G$ ).<sup>62</sup>

$MO_m$	$\Delta_f G$ (kJ/mol)	Theoretical equilibrium potential (V)	$MO_m$	$\Delta_f G$ (kJ/mol)	Theoretical equilibrium potential (V)
$V_2O_5$	-1419	1.441	$SiO_2$	-856	0.694
$MnO_2$	-465	1.708	$SnO_2$	-520	1.582
$Fe_2O_3$	-742	1.631	$SrO$	-561	0.005
$CoO$	-214	1.802	$Y_2O_3$	-1817	-0.226
$NiO$	-212	1.954	$Al_2O_3$	-1582	0.180
$CuO$	-128	2.248	$ZnO$	-320	1.252

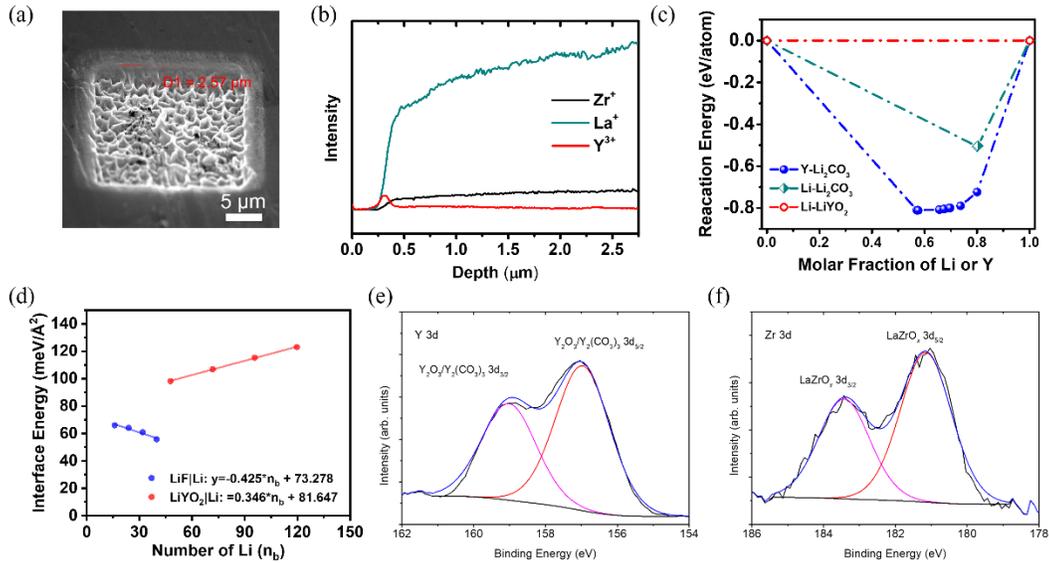
#### 4.4 Construction and Characterization of the Y doped Interlayer



**Figure 4-1 Characterization of the symmetric Li-Y|LLZTO|Li-Y cells.** (a) Li-Y Phase diagram. The red stars indicate the ratio of Li-Y alloy studied (7:1, 3:1, and 1:1); (b) Digital pictures for the Li-Y|LLZTO|Li-Y symmetric cells assembling process; (c, d) cross-sectional SEM image of the Li-Y|LLZTO interface. (e-h) EDS mapping of the Li-Y|LLZTO interface.

Li-Y alloy with three different compositions (7:1, 3:1, and 1:1, marked in Figure 1a) was synthesized and attached onto garnet LLZTO pellets using a molten Li method at 350°C. As demonstrated in **Figure 4-1** b, after immersing the LLZTO pellets into the molten Li alloy anode, the anode can be attached onto the surface of the solid electrolyte easily. After cooling to room temperature, the anode delivered a flat homogenous texture with metallic luster. The wettability of Li-Y to LLZTO solid electrolyte was demonstrated through this attachment process, and further confirmed through scanning electron microscopy (SEM). As shown in **Figure 4-1** c-d, intimate

contact without obvious void or gap was observed between LLZTO and Li-Y. The position of the interface was further confirmed using the energy-dispersive X-ray spectroscopy (EDS) mapping (**Figure 4-1 e-h**).



**Figure 4-2 Characterization of the interface chemistry for the Li-Y | LLZTO interface (the weight ratio of Y to Li was 3:1).** (a) SEM image (top view) for the Ga<sup>+</sup> ion beam sputtered crater of the interface. (b) Depth profiling of spatial distribution of Zr, La, and X element at the interface. (c) Thermodynamic equilibrium reaction energy for the X-Li<sub>2</sub>CO<sub>3</sub>, Li-Li<sub>2</sub>CO<sub>3</sub>, and Li-LiXO<sub>A</sub> interfaces. (d) The calculated interface energy ( $\gamma$ ) vs. the number of Li-metal formula units by DFT. High-resolution XPS of (e) X 3d, and (f) Zr 3d spectra of the interface.

Further characterizations were conducted to investigate the interface chemistry and evaluate the thermodynamic stability against dendrite penetration. The depth profiles of Zr<sup>+</sup>, Y<sup>3+</sup> and La<sup>+</sup> were acquired by *ex situ* time-of-flight secondary ion mass

spectrometry (ToF-SIMS). A  $20\ \mu\text{m} \times 20\ \mu\text{m}$  area (**Figure 4-2 a**) was sputtered with  $\text{Ga}^+$  ion focused ion beam (FIB) on top of the SSE, in which  $\text{Y}^{3+}$  show peak at a depth around  $0.3\ \mu\text{m}$  with the followed by a rise of  $\text{La}^+$ , indicating the aggregation of  $\text{Y}^{3+}$  at the Li-Y | LLZTO interface (**Figure 4-2 b**). X-ray photoelectron spectroscopy (XPS) was performed with  $\text{Ar}^+$  ion gun etching to identify the component at Li-Y | LLZTO interface. The etching depth of the interface was confirmed with the Zr  $3d$  spectra (**Figure 4-2 f**) to make sure the interface has been reached. From the Y  $3d$  spectra (**Figure 4-2 e**), the peaks for  $3d_{5/2}$  and  $3d_{3/2}$  of the oxide or carbonate of Y were located at 159.03 eV and 157.04 eV, respectively. As a cross-validation and further identification between the oxide and carbonate, calculation based on density functional theory (DFT) was conducted to find the potentially thermodynamically stable compound on the interface. The result was plotted in the “convex-hull” plot in **Figure 4-2 c**, in which a stable compound should have a lower formation energy than the linear combination of any other phases in the system, i.e., being on a convex hull. As shown by the blue and green curves, there are more stable compounds in both Y- $\text{Li}_2\text{CO}_3$  and Li- $\text{Li}_2\text{CO}_3$  systems. On the contrary, Li- $\text{LiYO}_2$  demonstrates a straight line in red without any more stable compound. These confirmed the most stable form of Y should be its oxide form:  $\text{LiYO}_2$ , and  $\text{LiYO}_2$  should be the main functioning species on Li-Y | LLZTO interface.

To further evaluate the dendrite suppression capability of  $\text{LiYO}_2$ , the interface energy ( $\gamma$ ) of the  $\text{LiYO}_2$  against Li was analyzed based on DFT simulation. On an energy perspective, interfaces with high  $\gamma$  will require high energy penalty for lithium to

penetrate in a dendritic form, and thus promoting lateral lithium motion along the interface.<sup>67</sup> In previous reports, LiF has been recognized as having the highest  $\gamma$  among all lithium compounds that can be formed in the electrolyte | anode interface.<sup>32</sup> LiF-rich interfaces have been used in multiple systems and demonstrated exceptional performance of dendrite suppression.<sup>68-70</sup>

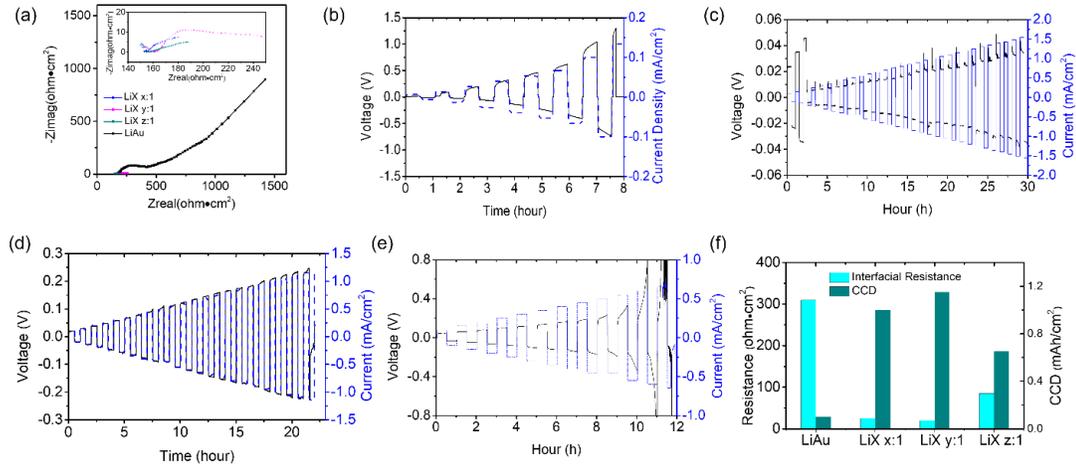
As shown in **Figure 4-2 d**, the interface energy obtained from the intercept of the fitted line was 81.65 meV/Å for LiYO<sub>2</sub>, which is even higher than that of LiF. The LiYO<sub>2</sub> with extremely high interface energy against lithium can effectively suppress Li dendrite growth.

Here, the high interface energy of LiYO<sub>2</sub> against lithium guaranteed a dynamic stable interlayer that suppressed the dendrite penetration. While the negative theoretical equilibrium potential of oxide form of Y against lithium affirmed a thermodynamic stable interlayer that would not be reduced back to an electron-conducting Y metal layer by lithium. With these two unique properties, the Y formed a solid “Great Wall” to protect the SSE from decomposition and Li dendrite penetration.

#### 4.5 Lithium Dendrite Suppression Capability of LiYO<sub>2</sub> Interphase

Electrochemical characterizations of the Li-Y|LLZTO|Li-Y cells were conducted to confirm the lithium dendrite suppression capability of the designed interlayer with high thermodynamic stability. In order to select the Li-Y alloy with optimized composition, electrochemical impedance spectra (EIS) were conducted to measure the

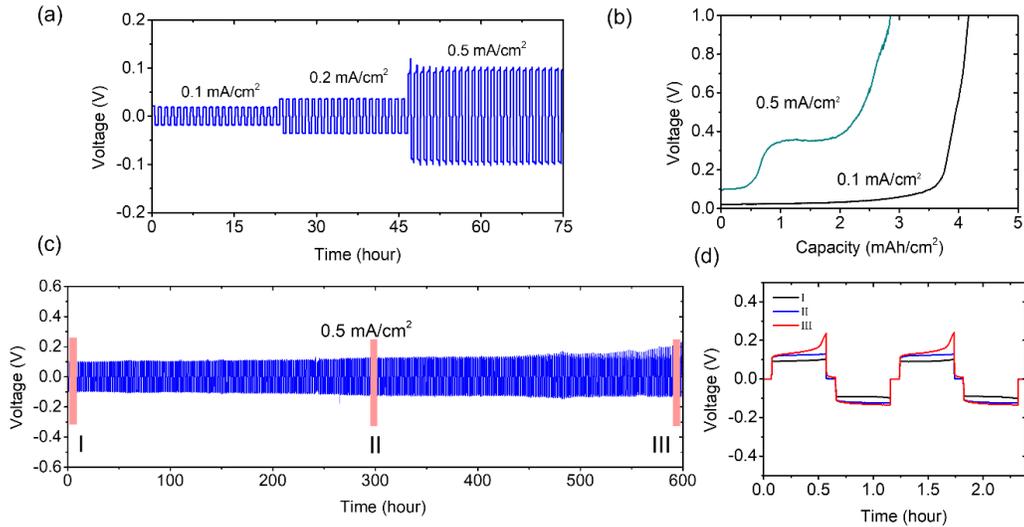
interfacial resistance before cycling, and critical current density (CCD) tests was conducted to evaluate the lithium dendrite suppression capability.



**Figure 4-3** Electrochemical characterizations of the symmetric Li-X|LLZTO|Li-X cells at room temperature without extra pressure. (a) EIS plot of Li-X|LLZTO|Li-X and Li-Au|LLZTO|Li-Au symmetric cells; The detailed EIS for different ratio of X were shown in the inset figure. CCD measurement for the (b) Li-Au|LLZTO|Li-Au cell, and (c-e) Li-X|LLZTO|Li-X (the weight ratio of X to Li was (c) x:1, (d) y:1 and (e) z:1, respectively) at step-increased current densities with a fix charging/discharging time of 0.5 h. (f) The summary of interfacial resistance and measured CCD for the symmetric cells with Li-Au and Li-X anodes.

As shown in **Figure 4-3** a and f, the resistance of the electrolyte pellets, including both bulk and grain boundary, are represented as the first semicircles, which are around 150~165  $\Omega \text{ cm}^2$  regardless the interface treatment. The interface resistances of Li-Y|LLZTO|Li-Y cells are around 20 - 85  $\Omega \text{ cm}^2$ , which are significantly smaller compared to the Au sputtered one (314  $\Omega \text{ cm}^2$ ). The CCD measurement shows that the Li-Y |LLZTO| Li-Y (the weight ratio of Y to Li was 3:1) can reach a high CCD of 1.15  $\text{mA cm}^{-2}$  (**Figure 4-3** d), which is 10 times higher than that of Li-Au |LLZTO| Li-Au (0.1  $\text{mA cm}^{-2}$ , **Figure 4-3** b). The comparison of the Li-Au anode and Li-Y

anode with different Li/Y weight ratios is shown in **Figure 4-3 f**, among which the Li-Y |LLZTO|Li-X (the weight ratio of Y to Li was 3:1) shows the smallest interface resistance and highest CCD (**Figure 4-3 c-e**).

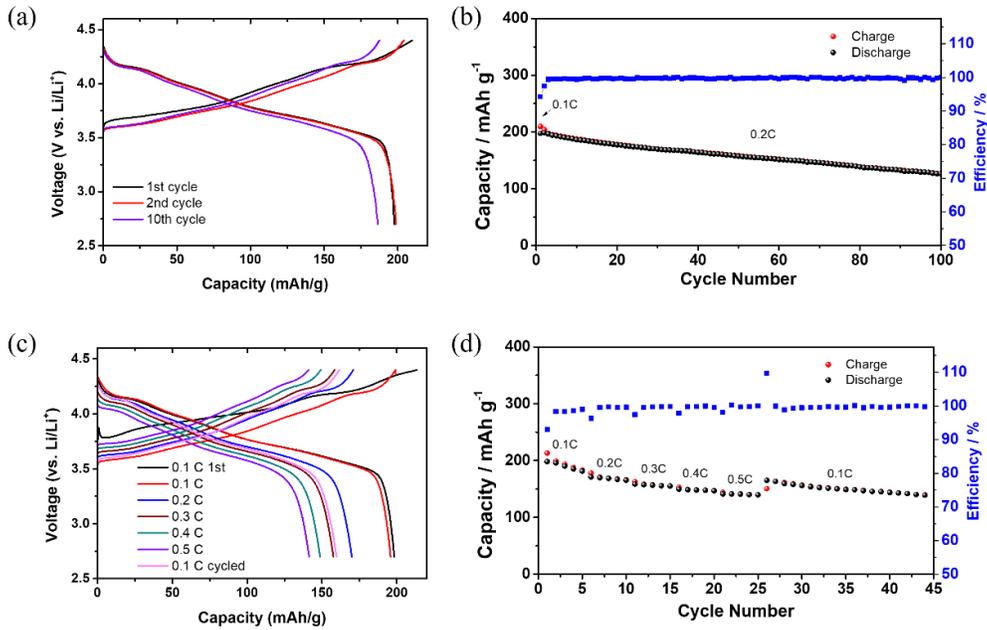


**Figure 4-4 Electrochemical characterizations of the composition optimized Li-Y anode.** (a) The voltage profile of Li-Y |LLZTO| Li-Y (the weight ratio of Y to Li was y:1) cell at step-increased current densities. (b) Voltage profile for Li-Y |LLZTO| Li-Y (the weight ratio of Y to Li was 3:1) cells when Li was stripped at a constant current density of 0.1 and 0.5 mA cm<sup>-2</sup> with a cut-off voltage of 1.0 V. (c) Galvanostatic cyclic performance of the symmetric Li-Y |LLZTO| Li-Y (the weight ratio of Y to Li was 3:1) cells at 0.5 mA cm<sup>-2</sup> and the corresponding details for the regions I, II, and III were shown in (d).

To further study the Li plating/stripping behavior of Li-Y anode (the weight ratio of X to Li was 3:1), the critical capacity of cell was tested. When Li-Y |LLZTO| Li-Y was stripped at constant current densities of 0.1 and 0.5 mA cm<sup>-2</sup> with a cut-off voltage of 1.0 V, the critical capacities of 4.2 and 2.8 mAh cm<sup>-2</sup> were achieved (**Figure 4-4 b**), which can fully meet the capacity requirement for practical application of Li-metal anode in all-solid-state battery. The optimized Li-Y |LLZTO|

Li-Y (the weight ratio of Y to Li was 3:1) shows stable cyclic performance at different current densities of 0.1, 0.2 and 0.5 mA cm<sup>-2</sup> without any abrupt overpotential increase (**Figure 4-4 a**). Besides, a long cycle life of 600 hours under 0.5 mA cm<sup>-2</sup>/0.25 mAh cm<sup>-2</sup> can also be achieved (**Figure 4-4 c-d**). The superior electrochemical performances of Li-Y |LLZTO| Li-Y cell demonstrate the effectiveness of our design principle for a thermodynamically stable interlayer.

#### 4.6 Electrochemical Performance of Full Cells



**Figure 4-5 Electrochemical performance of proof-of-concept Li-Y | LLZTO | NMC811 cells.** (a, b) The cycle performance for the cell at 0.2 C with cathode loading of 0.8 mAh cm<sup>-2</sup> (0.1 C for the first cycle for activation). (c, d) The rate performance for the cell at step-increased C-rate.

Since Li-Y anode shows high CCD and high cycling stability with LLZTO electrolyte, it was selected for additional full cell performance evaluation. Li-Y | LLZTO | LiNi<sub>0.8</sub>Mn<sub>0.1</sub>Co<sub>0.1</sub>O<sub>2</sub> (NMC811) cells were assembled with liquid electrolyte wetted cathode interface to eliminate the contact effect on cathode side. The cell was activated at 0.1C in the first cycle and then cycled at 0.2C in the following cycles. Li-X | LLZTO | NMC811 cell provides reversible capacity of 186.4 mAh g<sup>-1</sup> at the 10th cycle of 0.2 C under cut-off voltage of 2.7~4.3 V (**Figure 4-5 a**) with a capacity retention of 80% after 100 cycles with average Coulombic efficiency of 99.77% (**Figure 4-5 b**). Li-Y | LLZTO | NMC811 cells also shows excellent rate capability. As shown in **Figure 4-5 c-d**, The Li-X | LLZTO | NMC811 cells display capacity of 198.2 mAh g<sup>-1</sup> at 0.1 C, 170.0 mAh g<sup>-1</sup> at 0.2 C, 157.6 mAh g<sup>-1</sup> at 0.3 C, 148.7 mAh g<sup>-1</sup> at 0.4 C and 141.0 mAh g<sup>-1</sup> at 0.5 C. When the current recovered back to 0.1 C, reversible capacity of 159.7 mAh g<sup>-1</sup> can also be remained. The superior cyclic performance and rate capability of Li-Y | LLZTO | NMC811 cells can fully demonstrate the superior stability of Li-Y alloy anode to LLZTO electrolyte. However, further optimizations of liquid-free cathode interface engineering are still needed to realize practical applications of all-solid-state lithium metal batteries.

#### 4.7 Conclusion

Overall, a high stable LiYO<sub>2</sub> interface was established and studied in this chapter to validate our design principle of high interface energy for SSE | Li interface. A high critical current density of 1.15 mA cm<sup>-2</sup>, a critical capacity of 4.2 mAh cm<sup>-2</sup> at 0.1

mA cm<sup>-2</sup> and a long cycle life of 600 cycles under 0.5 mA cm<sup>-2</sup>/0.25 mAh cm<sup>-2</sup> was achieved in the lithium symmetric battery tests to demonstrate the dendrite suppression capability of the interface. This work sheds new insight on the rational design of the interface for SSLBs with high performance.

## Chapter 5 Void Suppressive Lithium Anodes for All-Solid-State Batteries

### 5.1 Introduction

All-solid-state lithium metal batteries have garnered great attention due to their high energy density and safety.<sup>71–73</sup> However, SSLBs suffer from high interface resistance and severe lithium dendrite growth, impeding their applications.<sup>74–78</sup> The initial interfacial resistance and overpotential can be reduced by enhancing the wettability between lithium and solid-state electrolyte (SSE) through removing the surface contaminants<sup>79</sup> and coating lithophilic layer<sup>80,81</sup>, enabling stable lithium cycling at a low rate and capacity. However, the interfacial overpotential dynamically increases due to the void evolution at the Li|SSE interface during cycling.<sup>50,82,83</sup> When the interfacial overpotential exceeds the critical overpotential (COP) of SSE<sup>65,84,85</sup>, chemomechanical degradation<sup>86</sup> will occur, accelerating lithium dendrite propagation inside SSE.

Lacking an understanding of the origin of void evolution, the reported preengineered methods cannot effectively eliminate dynamic void formation and dendrite propagation. The dynamic strategies of suppressing void evolution are mainly limited to applying stacking pressure<sup>87–89</sup> and raising the operating temperature<sup>39</sup>, which are unfavorable for battery integration due to the introduced weight and cost to the battery stacks. To develop an SSLB that can cycle at a high rate and a high capacity

under low pressure and room temperature, a fundamental mechanism of the void evolution<sup>90,91</sup> should be revealed, and corresponding effective strategies are urgently needed.

In this study, we systematically investigated the lithium dendrite formation mechanism and correlated it with the interfacial overpotential induced by void formation. To enhance the void suppression capability (VSC) of the lithium anode, lithium diffusion was accelerated over 10 times by refining the grain through solidification of molten Li with a Mg-La inoculant (LiMgLa) additive, simultaneously enhancing the wettability. The refined LiMgLa anode demonstrated a high VSC of  $4.1 \text{ mA}^2 \cdot \text{h} \cdot \text{cm}^{-4}$ , which is over 10 times higher than that of the LiMg alloy ( $0.4 \text{ mA}^2 \cdot \text{h} \cdot \text{cm}^{-4}$ ). The LiMgLa anodes enable a high critical current density (CCD) of  $2.2 \text{ mA} \cdot \text{cm}^{-2}$  at a high capacity of  $1.1 \text{ mAh} \cdot \text{cm}^{-2}$  with the  $\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.5}\text{Ta}_{0.5}\text{O}_{12}$  (LLZTO) electrolyte, improving the rate and capacity simultaneously. The LiMgLa|LLZTO interface evolution during lithium stripping is simulated using a phase-field model, providing dynamic insight into the void formation process at the dependency of current density and diffusivity.

## 5.2 Experimental

### 5.2.1 Synthesis of the Alloys as Anodes

The anodes were prepared by a molten lithium method in a glovebox with an argon-filled atmosphere with moisture and oxygen concentrations  $<0.1 \text{ ppm}$ . The lithium

foil was placed in a stainless-steel container and heated at 350 °C on a hot plate. The native surface film was carefully removed to present a shiny liquid lithium. To prepare the Li-Mg alloy, Mg powder was added slowly to the molten lithium according to the molar ratio and vigorously stirred for approximately 10 minutes. Then, the Li-Mg alloy was cooled to room temperature by moving from the hot plate. For the Li-Mg-La alloy, the La powder was added to the molten Li-Mg alloy at 350 °C by the weight ratio of Mg and La. The following procedures for the Li-Mg-La alloy are similar to those for Li-Mg.

#### 5.2.2 Electrochemical Characterizations

The critical current density (CCD) measurements were conducted with stepwise increased current densities (0.1, 0.2, 0.5, 0.7, 1.0, 1.2, 1.5, 1.7, 2.0, 2.2 mA·cm<sup>-2</sup>), and each step was fixed as 30 minutes of charging/discharging. The profiles for anodic dissolution were tested with a voltage cutoff of 5.0 V at various current densities.

A commercially available NMC811 cathode with a loading of 1.6 mAh·cm<sup>2</sup> was provided by SAFT as the cathode for the SSLBS. 1 C was defined as 200 mA·g<sup>-1</sup>.

### 5.2.3 Molecular Dynamics Simulations

All the classic molecular dynamics (MD) simulations conducted in this work were performed using the Large-scale Atomic/Molecular Massively Parallel Simulator (LAMMPS, <http://lammps.sandia.gov>) software.<sup>92</sup> The modified embedded atom method (MEAM) potentials were used for Li and LiMg. A lithium vacancy concentration of 2% is introduced to the Li and LiMg bulk and slabs. The MD simulations were performed in the NPT ensemble at  $p = 1$  atm and  $T = 298$  K with a Nose–Hoover barostat and thermostat for 5 ns with a time step of 1.0 fs to integrate the equations of motion. Periodic boundary conditions were used, and electrostatic interactions were considered using the particle–particle particle–mesh scheme in k-space. Subsequently, 10 ns equilibration MD runs were performed in the NVT ensemble, followed by 10 ns NVT production runs that were used to extract structural properties. The diffusion coefficients ( $D$ ) were defined as the mean squared displacement (MSD) over time as

$$D = \lim_{t \rightarrow \infty} \frac{\langle [r(t)]^2 \rangle}{6t} \quad (1.)$$

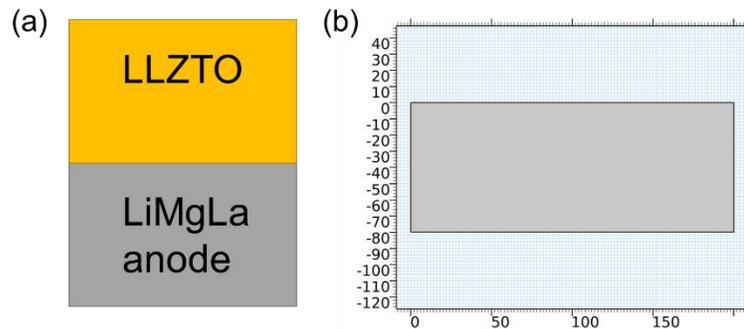
The average MSD,  $\langle [r(t)]^2 \rangle$ , was calculated by equation (3):

$$\langle [r(t)]^2 \rangle = \frac{1}{N} \sum_i \langle [r_i(t + t_0)]^2 - [r_i(t_0)]^2 \rangle \quad (2.)$$

where  $r_i(t)$  is the displacement of the  $i$ -th Li-ion at time  $t$  and  $N$  is the total number of ions in the system. The coefficients are finally attained from the slope of the average MSD vs. time plot for each temperature.

### 5.2.3 Phase-Field Model and Parameters

The phase-field method has been widely applied to dendrite growth in liquid and solid-state electrolytes, showing great capability in revealing the underlying mechanism for energy storage devices. However, the evolution of the anode during anodic dissolution has not been investigated. To probe the morphological evolution of the LiMg and LiMgLa anodes during the stripping process, the phase-field model<sup>93,94</sup> is simulated using a finite element method on the COMSOL Multiphysics 5.6 platform under an adaptive grid.



**Figure 5-1** (a) Scheme of the modeled LiMgLa and LLZTO interface and (b) the geometry of the anode in COMSOL Multiphysics. The physics in the LLZTO pellet has not been solved

The size of the lithium anode (**Figure 5-1**) is set to  $200 \times 80 \mu\text{m}$ , and the mesh size is set as  $50 \times 20$  with a minimum grid spacing of  $d_{min} = 4 \mu\text{m}$ . Since the amount of doped Mg and La is quite small, the Li bulk concentration is employed as  $c_0 = 7.64 \times 10^4 \text{ mol}\cdot\text{m}^{-3}$ . All the parameters are normalized to a characteristic energy density  $E_0 = c_0RT = 1.89 \times 10^8 \text{ J}\cdot\text{m}^{-3}$ , a characteristic length  $l_0 = 1 \mu\text{m}$ , and a characteristic time step  $\Delta t_0 = 10 \text{ s}$ . The detailed parameters and their normalized values are listed in **Table 5-1**.

**Table 5-1** Phase-field simulation parameters and their normalized values.

Parameter	Real value			Normalized value		
	Symbol	LiMg value	LiMgLa value	expression	LiMg value	LiMgLa value
<b>Diffusion coeff. in bulk lithium</b>	$D_{Li}$	$7.5 \times 10^{-11} \text{ cm}^2/\text{s}$	$1.2 \times 10^{-9} \text{ cm}^2/\text{s}$	$D_{Li}/(l_0^2/t_0)$	0.075	1.2
<b>Diffusion coeff. in void</b>	$D_v$	0	0	$D_v/(l_0^2/t_0)$	0	0
<b>Diffusion coeff. at surface</b>	$D_s$	$7.5 \times 10^{-8} \text{ cm}^2/\text{s}$	$7.5 \times 10^{-6} \text{ cm}^2/\text{s}$	$D_s/(l_0^2/t_0)$	75	1200
<b>Gradient energy coefficient</b>	$\kappa$	$1 \times 10^{-6} \text{ J/m}$	$5 \times 10^{-6} \text{ J/m}$	$\kappa/(E_0 l_0^2)$	0.0528	0.264
<b>Barrier height</b>	$W$	$4.95 \times 10^4 \text{ J/m}^3$	$4.95 \times 10^4 \text{ J/m}^3$	$W/E_0$	0.0264	0.0264
<b>Exchange current density</b>	$i_0$	$737.15 \text{ A/m}^2$	$737.15 \text{ A/m}^2$	$i_0 t_0 / (c_0 F l_0)$	1	1

To describe the diffuse interface in the phase-field model, a continuous phase-field variable  $\xi$  is introduced, which is a physical correspondence to the dimensionless concentration of Li atoms  $\tilde{c} = \xi = c/c_0$ . Here,  $c$  and  $c_0$  are the real-time and initial lithium concentrations, respectively.  $\xi = 1$  represents the electrode, while  $\xi = 0$

represents the void, and  $0 < \xi < 1$  represents the interface between these two phases. From the Ginzburg-Landau theory, a local chemical potential must be derived as a function of concentration. With  $F$  representing the free energy function, the chemical potential can be represented as a variational derivative as

$$\mu = \frac{\delta F}{\delta c} \quad (3.)$$

Since the concentration,  $c$ , is a conserved field, the mass conservation equation should be satisfied:

$$\frac{\partial c}{\partial t} = -\nabla \cdot \vec{J} \quad (4.)$$

The flux,  $\vec{J}$ , can be defined as

$$\vec{J} = -M \nabla \cdot \mu \quad (5.)$$

where  $M$  is the diffusion mobility. The equation of motion for the concentration field can be obtained by combining equations (3) and (4):

$$\frac{\partial c}{\partial t} = \nabla \cdot \left( M \nabla \frac{\delta F}{\delta c} \right) \quad (6.)$$

This is the Cahn-Hilliard equation, which represents the governing equation for concentration. The Ginzburg-Landau free energy functional,  $F$ , is defined as:

$$F = \int_V \left[ f(\xi) + \frac{1}{2} \kappa (\nabla \xi)^2 + \rho \phi \right] dV \quad (7.)$$

where  $f$  is the chemical free energy density,  $\kappa$  is the coefficient of gradient energy,  $\rho$  is the electrical charge density and  $\phi$  is the electric potential. Then, the time evolution of  $\xi$  in the phase-field model can be derived and given by:

$$\frac{\partial \xi}{\partial t} = M \nabla^2 \left( \frac{\partial f}{\partial \xi} - \kappa (\nabla \xi)^2 \right) \quad (8.)$$

An arbitrary double well function  $f(\xi) = W \xi^2 (1 - \xi^2)$  is used to describe the two equilibrium states for the electrode ( $\xi = 1$ ) and the void ( $\xi = 0$ ).  $W$  represents the barrier height.  $h(\xi) = \xi^3 (6\xi^2 - 15\xi + 10)$  is an interpolating function representing the fraction of material participating in the electrochemical reactions. The diffusion coefficient at the interface depends on the phase parameter  $D^{eff} = D_{Li} h(\xi) + 4D_s h(\xi)(1 - h(\xi)) + D_v(1 - h(\xi))$ , where  $D_{Li}$ ,  $D_s$ , and  $D_v$  are the lithium diffusion coefficients for the bulk, surface, and void, respectively.

To simulate the anodic dissolution process with a constant current density, the following rule is adapted to distribute the local current density ( $i$ ) at the anode and SSE interface.

$$i = I_{app} \frac{\int_{S_0} \xi ds}{\int_S \xi ds} \quad (9.)$$

where  $I_{app}$  is the applied current density and  $S_0$  and  $S$  are the initial and real-time contact areas at the electrode/electrolyte interface, respectively.

The reaction overpotential,  $\eta$ , is calculated by the Butler–Volmer equation:

$$i = -i_0 \left\{ \xi \exp \left[ \frac{(1 - \alpha)F}{RT} \eta \right] - \exp \left[ \frac{-\alpha F}{RT} \eta \right] \right\} \quad (10.)$$

where  $i_0$  is the exchange current density and  $\alpha$  is the charge-transfer coefficient.

### **5.3 Suppression of Voids and Lithium Dendrite**

#### **5.2.1 Definition of Void Suppression Capability (VSC)**

To analyze the void evolution mechanism, the VSC of an anode is defined as the product of the applied current ( $i$ ) and full depletion capacity ( $Q_{max}$ ). The VSC should be a constant for an ideal Li|SSE interface according to the mass-transfer transportation, which is determined by the effective diffusivity ( $D_{eff}$ ) and the initial interfacial concentration ( $c_0$ ) of the lithium anode.

Assuming a classical chemical diffusion process driven by the lithium concentration gradient in the anode and the initial interface resistance can be neglected, the depletion times ( $\tau$ ) can be determined by the applied current densities ( $i$ ) according to Sand's equation<sup>95</sup>:

$$\tau^{-\frac{1}{2}} = \frac{2}{\sqrt{\pi \cdot D_{eff}} \cdot c_0 \cdot F} \cdot i \quad (11.)$$

where  $D_{eff}$ ,  $c_0$ , and  $F$  are the effective diffusion coefficient, initial lithium concentration for the anode, and Faraday constant, respectively. We have the full depletion capacity  $Q_{max}$ ,

$$Q_{max} = i \cdot \tau \quad (12.)$$

Defining the void suppression capability:  $VSC = i \cdot Q_{max}$ , and combining equations (4) and (5),

$$VSC = i^2 \cdot \tau = \frac{\pi \cdot D_{eff} \cdot c_0^2 \cdot F^2}{4} \quad (13.)$$

Since the effective diffusion coefficient and initial lithium concentration for the anode are the intrinsic properties of the anode, the VSC should be a constant for certain lithium metal or alloy anodes. The relative void suppression capability (RVSC) is obtained by defining the VSC of Li metal as 1.

### 5.2.2 Relationship between the VSC and CCD

For ASSLMB, when the product of the stripped capacity and applied current approaches the VSC, the lithium at the interface will be depleted, inducing void formation.

The critical current density (CCD) is measured as the current density when the cell is short during lithium plating and stripping. According to our principles, a short circuit

occurs when the delivered capacity approaches the full depletion capacity using the CCD as the applied current density and a fixed time of  $t_{CCD}$ . Thus,

$$VSC = i \cdot Q_{max} > CCD^2 \cdot t_{CCD} \quad (14.)$$

Then, the relationship between the VSC and CCD can be derived as

$$CCD < \sqrt{VSC/t_{CCD}} \quad (15.)$$

The predicted maximum CCD at various  $t_{CCD}$  according to the VSC are listed in

**Table 5-2.**

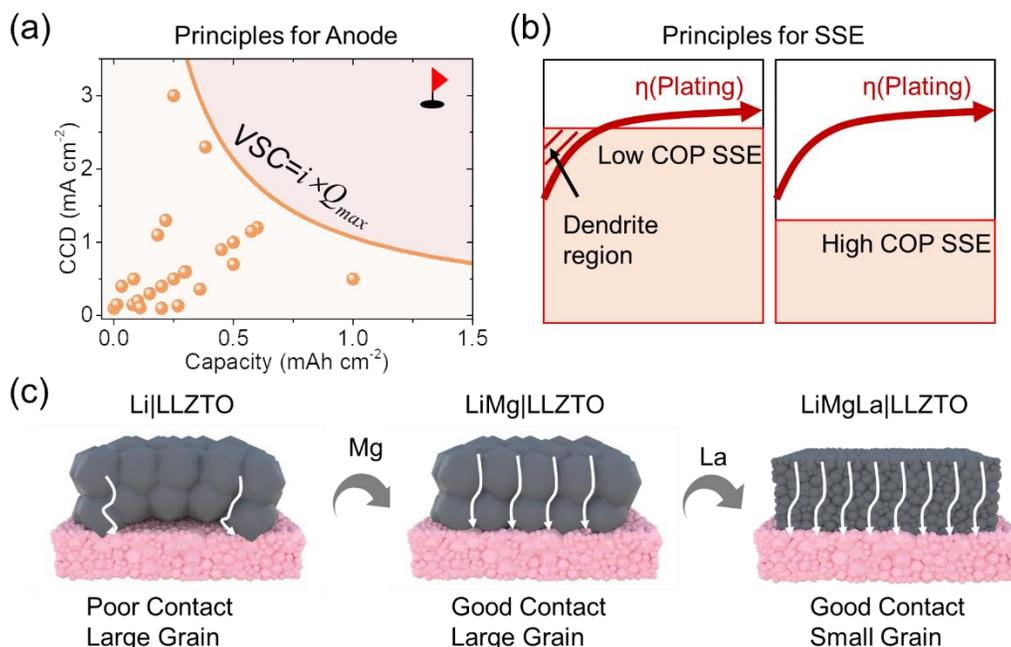
**Table 5-2** The predicted maximum CCD for Li metal, LiMg, and LiMgLa anodes at a fixed plating/stripping time of 0.5 h based on the published diffusion coefficients.

Anode	$D_{eff}(\text{cm}^2 \cdot \text{s}^{-1})$	VSC( $\text{s} \cdot \text{A}^2 \cdot \text{m}^{-4}$ )	Predicted CCD ( $\text{mA} \cdot \text{cm}^{-2}$ )
Li Metal	$(0.8 \sim 9) \times 10^{-11}$	$(0.34 \sim 3.84) \times 10^5$	0.44~1.46
LiMg	$(1.3 \sim 7) \times 10^{-11}$	$(0.55 \sim 1.42) \times 10^5$	0.56~1.29
LiMgLa	$3.6 \times 10^{-10}$	$1.50 \times 10^6$	2.89
Li Metal	$(0.8 \sim 9) \times 10^{-11}$	$(0.34 \sim 3.84) \times 10^5$	0.44~1.46

Current efforts to enhance the interface contact should be useful since it improves  $c_0$ .

For a critical  $c_0$  (ideal interface), the CCD can be predicted as a function of the capacity, which is presented as the orange line in **Figure 5-2** (data points listed in

**Table 5-3**).



**Figure 5-2 Design principles and strategies for high-performance ASSLMBs.** (a) The predicted upper limit of CCD (orange line) and reported CCDs (orange scatters) as a function of capacity. The red target on the top right represents a target of high rate and high energy density ASSLMB. (b) Schematic of dendrite formation mechanisms in the SSE with different COPs. The red arrow represents the voltage profile during plating. When the absolute value of voltage is higher than the absolute value of COP, dendrite growth starts. (c) Schematic of the design of high-performance ASSLMB by enhancing the contact and refining the grain size.

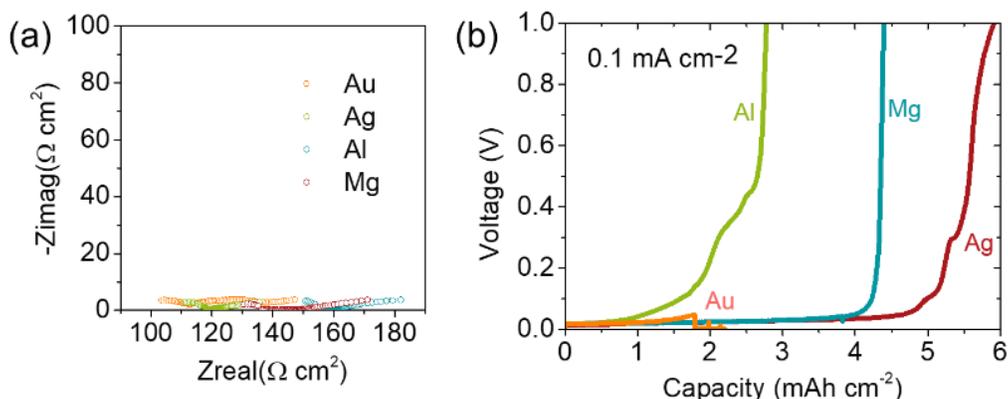
The reported CCDs (scatters in **Figure 5-2 a** and **Table 5-3**) by SSE modification and interface engineering are chasing the ideal CCD of lithium by  $c_0$  enhancement. The relationship indicates that a high CCD can be achieved by shortening the Li plating/stripping time, which is consistent with the reported results<sup>25</sup>. However, improving the CCD by sacrificing the capacity deviates from the original intention of utilizing the high energy density of ASSLMBs. To simultaneously reach the goal of fast charging and high energy density (star in **Figure 5-2 a**), the VSC should be raised by simultaneously improving  $c_0$  at the interface and  $D_{eff}$  of the anode.

**Table 5-3** Reported critical current densities (CCDs) and corresponding area specific capacity (ASC) for planar garnet-type solid-state electrolytes. The improvement strategies and experimental conditions are included. The 25 °C is defined as room temperature.

Composition	Methods	ASC (mAh·cm <sup>-2</sup> )	CCD (mA·cm <sup>-2</sup> )	T (°C)	P (MPa)	Ref.
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Microstructure	0.08	0.15	25	1.4	J. Power Sources 2017, 363, 145–152.
		0.20	0.40			
		0.30	0.60			
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Roughness	0.1	0.2	25	1.4	J. Electrochem. Soc. 2017, 164, A666-A671.
		0.2	0.4			
Li <sub>6.55</sub> La <sub>3</sub> Zr <sub>1.55</sub> Ta <sub>0.45</sub> O <sub>12</sub>	Relative density	0.36	0.36	25	/	Batteries Supercaps 2019, 2, 524–529.
		0.11	0.11			
Li <sub>6.6</sub> La <sub>3</sub> Zr <sub>1.6</sub> Ta <sub>0.4</sub> O <sub>12</sub>	Acid Etching	1.0	0.5	20	0.15	ACS Appl. Energy Mater. 2019, 2, 6720–6731.
		0.2	0.1			
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	SPS sintering	0.3	0.6	25	1.4	J. Power Sources, 2017, 363, 145-152
Li <sub>7</sub> La <sub>3</sub> Zr <sub>2</sub> O <sub>12</sub>	HIP	0.295	0.591	25	/	Solid State Ionics, 2018, 319, 285-290
Li <sub>6.25</sub> Ga <sub>0.25</sub> La <sub>3</sub> Zr <sub>2</sub> O <sub>12</sub>	Heat treatment	0.45	0.9	60	/	ACS applied materials & interfaces 2018, 11, 1, 898-905.
Li <sub>7</sub> La <sub>3</sub> Zr <sub>2</sub> O <sub>12</sub>	Grain refinement	0.134	0.268	25	/	ACS applied materials & interfaces 2015, 7.3, 2073-2081
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Au/Nb coating	0.083	0.5	25	0.1	Rare Metals 2018, 37, 473-479.
Li <sub>7</sub> La <sub>2.75</sub> Ca <sub>0.25</sub> Zr <sub>1.75</sub> Nb <sub>0.25</sub> O <sub>12</sub>	Mg coating	0.008	0.1	25	/	Angewandte Chemie International Edition 2017, 56, 47, 14942- 14947.
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Li <sub>3</sub> N coating	0.0125	0.15	25	/	Nano Lett. 2018, 18, 11, 7414–7418
Li <sub>6.5</sub> La <sub>3</sub> Zr <sub>1.5</sub> Ta <sub>0.5</sub> O <sub>12</sub>	Cu <sub>3</sub> N coating	0.6	1.2	25	/	Energy & Environmental Science 2020, 13, 1, 127-134.
Li <sub>6.4</sub> La <sub>3</sub> Zr <sub>1.4</sub> Ta <sub>0.6</sub> O <sub>12</sub>	SnO <sub>2</sub> coating	0.575	1.15	30	/	J. of Power Sources 2019, 420, 15-21.
Li <sub>5.9</sub> Al <sub>0.2</sub> La <sub>3</sub> Zr <sub>1.75</sub> W <sub>0.25</sub> O <sub>12</sub>	Graphite interface	0.15	0.3	25	/	ACS Energy Lett. 3, 2018, 1212-1218

		0.25	0.5	80	/	
$\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.5}\text{Ta}_{0.5}\text{O}_{12}$	Li-C composite	0.5	1	60	/	Adv. Mater. 2019, 31, 1807243
$\text{Li}_{6.28}\text{La}_3\text{Zr}_2\text{Al}_{0.24}\text{O}_{12}$	PVDF-PEO	0.033	0.4	25	/	J. of Mater. Chem. A 2018, 6, 42, 21018-21028.
$\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.45}\text{Ta}_{0.55}\text{O}_{12}$ with $\text{Li}_3\text{N}$ Filler	ultrafast sintering with Filler	0.383	2.3	25		Acs Energy Lett. 2021, 6, 3753–3760.
$\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.45}\text{Ta}_{0.55}\text{O}_{12}$	Control group	0.217	1.3		/	
$\text{Li}_{6.28}\text{Al}_{0.24}\text{La}_3\text{Zr}_2\text{O}_{12}$	Li-Zn alloy anode	0.183	1.1	25	/	Acs Appl Energy Mater. 2020, 3, 9010–9017
$\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.5}\text{Ta}_{0.5}\text{O}_{12}$	$\text{Li}_3\text{PO}_4$	0.4	0.8	25	/	J Mater Chem A. 2019, 7, 14565–14574
$\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.5}\text{Ta}_{0.5}\text{O}_{12}$	LiMgLa alloy	1.1	2.2	25	/	This Work
$\text{Li}_{6.5}\text{La}_3\text{Zr}_{1.5}\text{Ta}_{0.5}\text{O}_{12}$	LiMg alloy	0.5 0.25	0.7 3.0	25	/	This Work

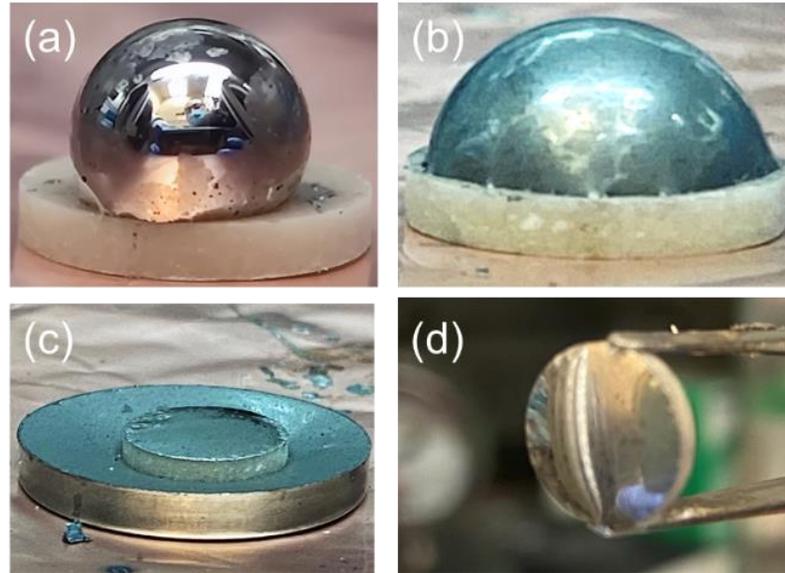
The voids at Li|SSE reduce the effective contact area at the interface and partially block lithium paths into the SSE, making the mass-transfer controlled overpotential ( $\eta$ ) increase rapidly with the galvanistic lithium stripping time. For the subsequent lithium plating process, the initial overpotential may be larger than the critical overpotential (COP) of an SSE with a low COP (less stable against lithium) due to the formed voids, driving lithium dendrite formation and propagation (shadow area in **Figure 5-2 b left**). Increasing the COP can effectively suppress dendrite propagation (**Figure 5-2 b right**). It should be noted that even for an ideal dendrite-free electrolyte with a high COP, the high interface overpotential due to the formed void will finally block the charge/discharge process. Hence, the “short-circuit” is only one of the external manifestations of the cell failure, while more attention should be given to the reduction of polarization through increasing the VSC.



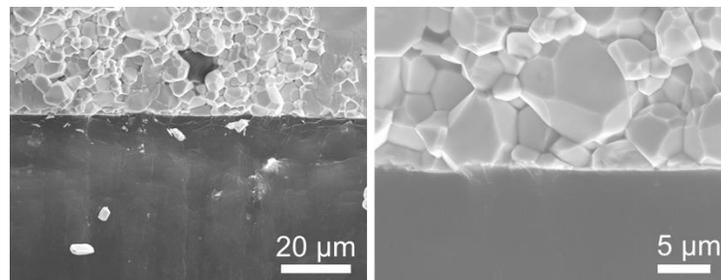
**Figure 5-3** (a) Nyquist plots before cycling and (b) voltage profiles at  $0.1 \text{ mA}\cdot\text{cm}^{-2}$  for symmetric cells with Ag-, Mg-, Al-, and Au-doped Li as anodes.

The high lithium concentration at the interface requires intimate contact between the SSE and Li anodes. Adding a small amount of lithiophilic metals, such as Al, Au, Ag and Mg, can effectively enhance the wettability and contact between lithium and SSE (**Figure 5-3**). Since Mg also has a long range of solid-solution phases, MgO can be easily formed at the LLZTO surface to protect the surface from further reduction. Therefore, Mg was selected as an additive in lithium anodes. However, as with other lithiophilic metals, Mg cannot effectively enhance the lithium diffusivity; thus, voids still form dynamically (**Figure 5-2 c middle** and **Figure 5-3**). Since the grain boundary has a higher diffusivity than that in the bulk, reducing the grain size should enhance the lithium diffusivity. One way to refine the grain is to add inoculant into molten lithium followed by a rapid solidification. It was reported that Mg-La can form intermetallic compounds, which can serve as the effective nucleus<sup>26</sup> for lithium crystallization (**Figure 5-2 c right**). Similar to the solidification process, Mg-La can also maintain the nuclear role during the electrochemical Li plating/stripping process,

inheriting the refined grain size. With a decent interface contact and fast lithium diffusion inside the lithium anode, the LiMgLa anodes should achieve a high VSC and enable both high rate and high energy density cells.



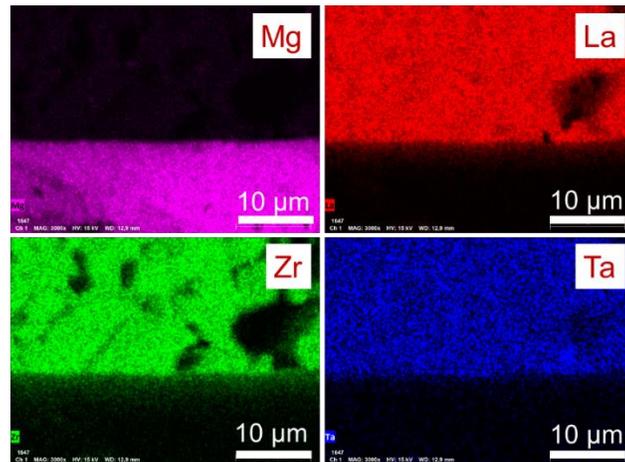
**Figure 5-4** Digital pictures of the wettability of (a) molten Li and (b) molten LiMgLa against LLZTO pellets and the assembled LiMgLa|LLZTO|LiMgLa symmetric cells at (c) 350 °C and (d) room temperature.



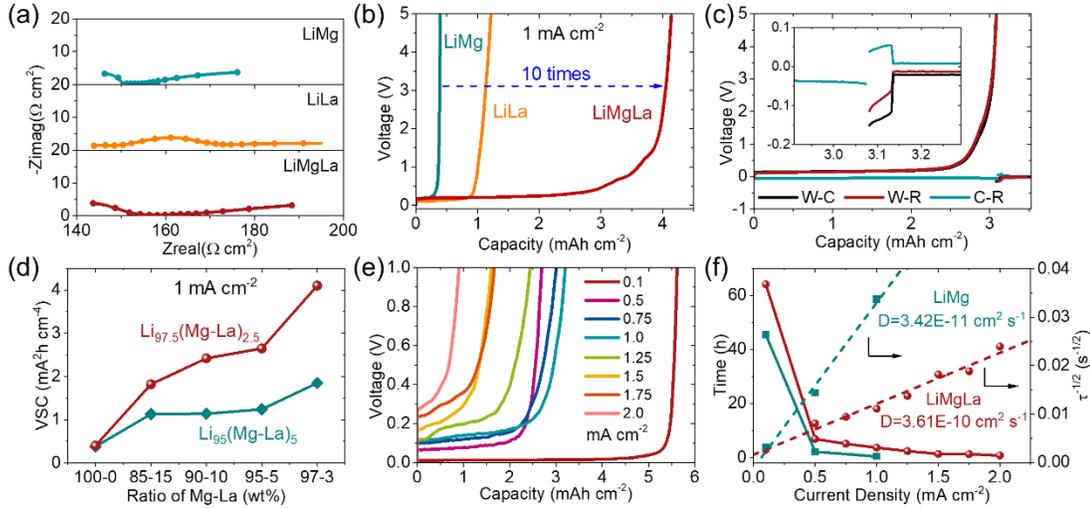
**Figure 5-5** Scanning electronic microscope (SEM) images for the cross-section of the LiMgLa|LLZTO interface before cycling at different scales, showing decent contact.

#### 5.4 Void Suppression Capability of the LiMgLa Anodes

Three doped Li anodes, including LiMg ( $\text{Li}_{97.5}\text{Mg}_{2.5}$ ), LiLa (Li-1%wt La) and LiMgLa ( $\text{Li}_{97.5}(\text{Mg-1\%wt La})_{2.5}$ ), were prepared by adding Mg and/or La into molten Li at 350°C followed by rapid solidification in a glovebox. The interface resistances of these alloy anodes with LLZTO were evaluated with electrochemical impedance spectroscopy (EIS). After subtracting the bulk transport resistance of  $\sim 155 \Omega\cdot\text{cm}^2$  in the LLZTO (**Figure 3-8**) from the symmetric cell resistance, the interface resistances of the LiMg, LiLa, and LiMgLa anodes were calculated as 20-35  $\Omega\cdot\text{cm}^2$  (**Figure 5-7**). The small initial interface resistances indicate excellent wetting (**Figure 5-4**), intimate contact, and high  $c_0$  for all of the interfaces (**Figure 5-5** and **Figure 5-6**).

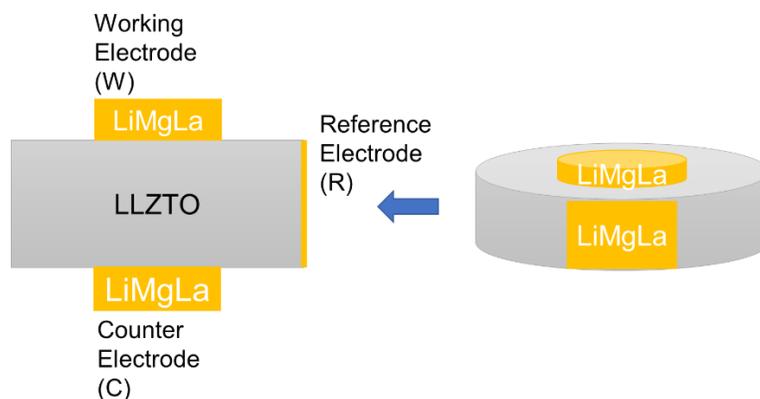


**Figure 5-6** Energy dispersive X-ray (EDX) mapping analysis for Mg, La, Zr, and Ta on the cross-section of the LiMgLa|LLZTO interface. The EDX mapping images show distinct domains for the LiMgLa and LLZTO pellets with Mg elements in the electrode and La, Zr, and Ta elements in the LLZTO pellet. The mapping for La confirms that only a small amount of La is doped.



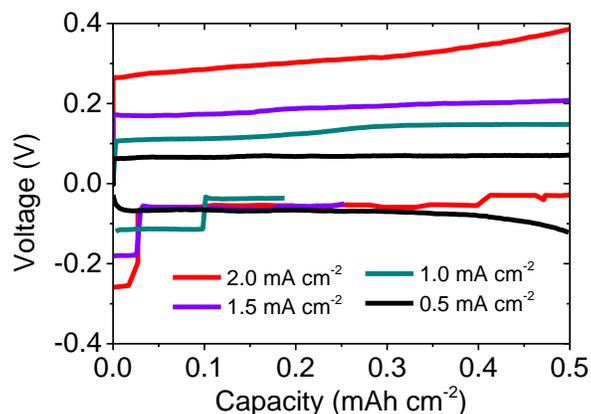
**Figure 5-7 VSC of LiMgLa anodes at room temperature.** (a) Electrochemical impedance spectra of symmetric cells with LiMgLa, LiLa, and LiMg anodes from 1 MHz to 0.1 Hz using symmetric cells without an external pressure at room temperature. (b) Delivered maximum capacity of LiMgLa LiLa and LiMg anodes during stripping at a current density of  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  with a voltage cut-off of 5.0 V. (c) Voltage profiles for the working-counter (W-C) electrodes, working-reference (W-R) electrodes, and counter-reference (C-R) electrodes measured using a three-electrode cell. The inset figure shows the potential profiles of the subsequent plating process after fully depleted Li stripping. (d) VSC of LiMgLa anodes with different compositions during stripping at a current density of  $1.0 \text{ mA}\cdot\text{cm}^{-2}$ . (e) Potential profiles of LiMgLa anodes during stripping at different current densities. (f) The current density dependency on the Li depletion times and fitted (dotted lines) diffusion coefficients for LiMg and LiMgLa anodes using Sand's equation.

The Li stripping voltage profiles of symmetric cells using LiMg, LiLa and LiMgLa electrodes show flat plateaus with a rapid increase to 5.0 V at the end of the Li stripping at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  (**Figure 5-7** b). The rapid increase in overpotential is attributed to the detachment of anodes to LLZTO due to void growth. The full stripping capacity of the LiMgLa anode is over 10 times larger than that of the Li anode at a high current of  $1.0 \text{ mA}\cdot\text{cm}^{-2}$ , suggesting a great enhancement of VSC.



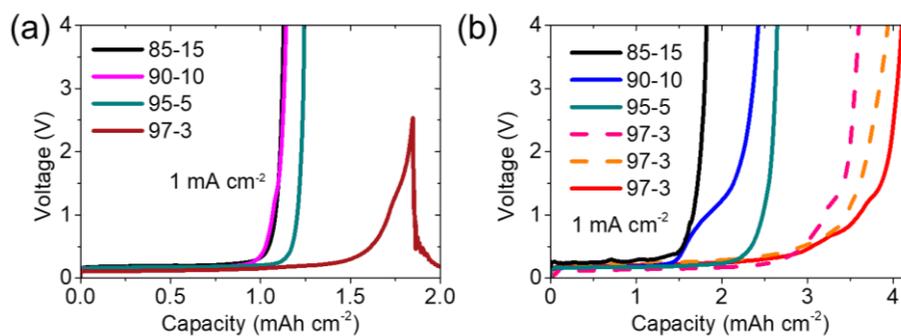
**Figure 5-8** Cell schematic for three-electrode cells with LiMgLa electrodes.

Three-electrodes measurement (**Figure 5-8**) demonstrates that under the circumstance of reaching full stripping capacity, even a small amount of plated lithium ( $0.05 \text{ mAh}\cdot\text{cm}^{-2}$ ) would shorten the circuit (**Figure 5-7 c**), indicating the strong correlation between void formation and Li dendrite growth. The potential of the plating side (W-R) gradually decreases while the potential of the stripping side (C-R) gradually increases, suggesting that the dendrite growth from the depleted interface is much faster. The fast short circuit on the depleted interface can also be found at a large current density in the LiMgLa|LLZTO|LiMgLa symmetric cells (**Figure 5-9**).



**Figure 5-9** The enlarged potential profiles of LiMgLa electrodes at the early stage of stripping and their subsequent plating process at different current densities with a voltage cutoff of 5.0 V. Short circuits are found for the cell for 1.0, 1.5, and 2.0  $\text{mA}\cdot\text{cm}^{-2}$  within a small capacity of  $0.1 \text{ mAh}\cdot\text{cm}^{-2}$ .

As shown in **Figure 5-7 d** and **Figure 5-10**, the VSC of Li anodes increases with Mg/La weight ratios at a fixed total amount of Li-Mg. At a fixed Mg/La weight ratio, all VSCs of the  $\text{Li}_{97.5}(\text{Mg-La})_{2.5}$  anodes are higher than those of  $\text{Li}_{95}(\text{Mg-La})_5$ . The voltage profiles of LiMgLa anodes at different current densities with a cut-off voltage of 5.0 V are displayed in **Figure 5-7 e**.

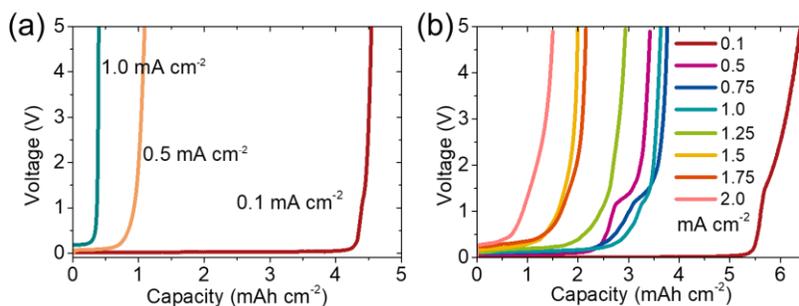


**Figure 5-10** Voltage profiles of different composite (a)  $\text{Li}_{95}(\text{MgLa})_5$  and (b)  $\text{Li}_{97.5}(\text{MgLa})_{2.5}$  electrodes with different Mg-La weight ratios. The dashed lines demonstrate the reproducible performance for LiMgLa anodes.

**Table 5-4** The effective diffusion coefficients ( $D_{eff}$ ), the initial lithium concentration ( $c_0$ ), and the calculated void suppression capability (VSC) and relative void suppression capability (RVSC, void suppression capability of Li metal set as 1) for Li metal, LiMg, and LiMgLa anodes. The initial surface concentration of LiMg and LiMgLa was set as 0.975 times that of Li metal.

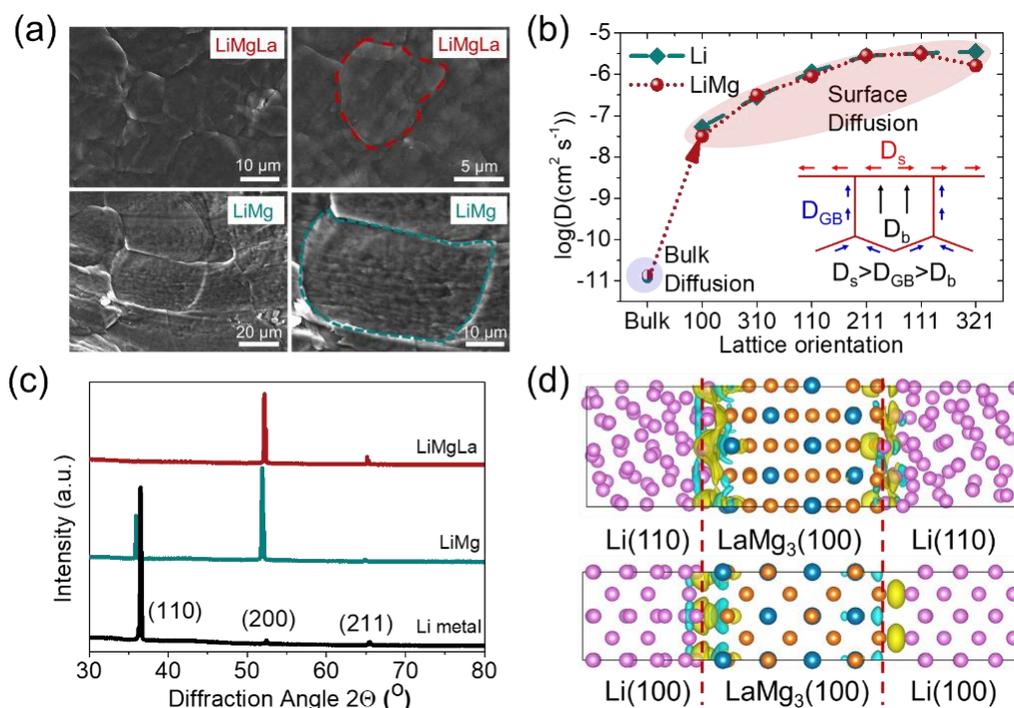
Anode	$D_{eff}$ (cm <sup>2</sup> ·s <sup>-1</sup> )	$c_0$ (mol·m <sup>-3</sup> )	VSC (s·A <sup>2</sup> ·m <sup>-4</sup> )	RVSC
Li Metal	$5.6 \times 10^{-11}$	$7.64 \times 10^4$	$2.39 \times 10^5$	1
LiMg	$3.4 \times 10^{-11}$	$7.45 \times 10^4$	$1.42 \times 10^5$	0.59
LiMgLa	$3.6 \times 10^{-10}$	$7.45 \times 10^4$	$1.50 \times 10^6$	6.28

Obviously, the full depletion capacity for the LiMgLa anode is much larger than that of the LiMg (**Figure 5-11**) anodes at a fixed current density. The full depletion times ( $\tau$ ) at different current densities of the LiMg and LiMgLa anodes are shown in **Error! Reference source not found.** f. By fitting plots of  $\tau^{-1/2}$  versus current densities ( $i$ ) using Sand's equation, the fitted  $D_{eff}$  of Li for the LiMgLa anode is  $3.43 \times 10^{-10}$  cm<sup>2</sup>·s<sup>-1</sup>, which is one order of magnitude higher than that of the LiMg anode ( $3.25 \times 10^{-11}$  cm<sup>2</sup>·s<sup>-1</sup>), confirming the enhancement of Li self-diffusivity and VSC in the LiMgLa anodes. Assuming ideal contact between the anode and SSE, the theoretical VSC of LiMgLa ( $1.50 \times 10^6$  A<sup>2</sup>·h·m<sup>-4</sup>) is 6.28 times higher than that of the Li anode ( $2.39 \times 10^5$  A<sup>2</sup>·h·m<sup>-4</sup>), while the VSC of LiMg ( $1.42 \times 10^5$  A<sup>2</sup>·h·m<sup>-4</sup>) is lower than that of Li (**Table 5-4**).



**Figure 5-11** Voltage profiles of LiMg|LLZTO|LiMg and LiMgLa|LLZTO|LiMgLa symmetry cells at various current densities with a voltage cutoff of 5 V.

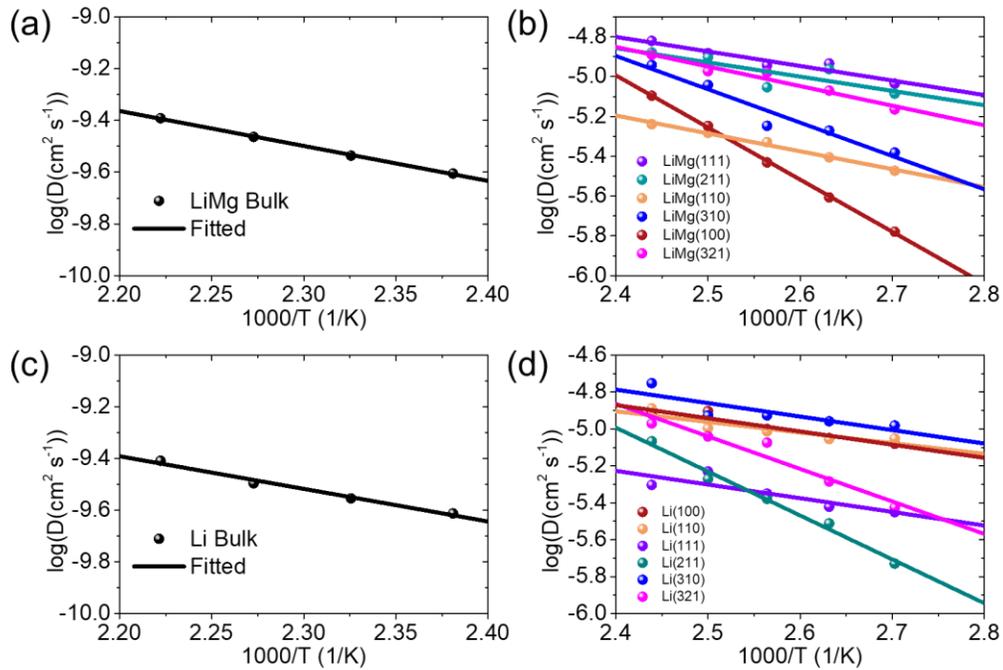
### 5.5 Mechanism for the high VSC of LiMgLa anodes



**Figure 5-12** Characterization of the LiMgLa anode. (a) SEM showing the grain distributions and sizes of the LiMgLa and LiMg alloys. (b) Molecular dynamics-calculated diffusion coefficients of bulk and differently oriented surfaces for Li metal and LiMg alloy at room temperature. The inset scheme illustrates different diffusion mechanisms. (c) Representative X-ray diffraction data for the Li metal, LiMg, and LiMgLa anodes. (d) Atomic structures and charge distributions of Li(110)|LaMg<sub>3</sub>(100) and Li(100)|LaMg<sub>3</sub>(100) interfaces. (Li in pink, Mg in orange,

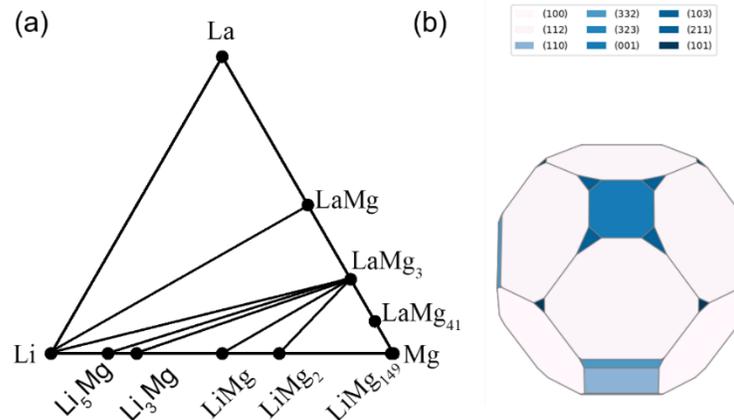
La in blue and the electron clouds in yellow for charge accumulation and cyan for charge depletion).

The high VSC of LiMgLa anodes is attributed to the refined microstructure with a fast lithium diffusion pathway since Mg-La is an excellent inoculant for metals. Scanning electron microscopy (SEM) was used to characterize the microstructure of the LiMg and LiMgLa anodes. **Figure 5-12** a shows the grain sizes of LiMg and LiMgLa. The grain sizes for the LiMgLa are in the range of 5-10  $\mu\text{m}$ , while those for the LiMg alloy are approximately 40  $\mu\text{m}$ . The smaller grain sizes indicate a larger specific surface and grain boundary area.



**Figure 5-13** Molecular dynamics (MD) calculated diffusion coefficients for (a) LiMg bulk, (b) LiMg surfaces with different orientations, (c) Li bulk, and (d) Li surfaces with different orientations.

The lithium diffusion coefficients of the bulk and surfaces with different orientations for Li and LiMg are calculated via molecular dynamics (**Figure 5-12 b** and **Figure 5-13**). LiMg and Li show close diffusion coefficients for both bulk and surface cases because of the low ratio of Mg and the same lattice type. The bulk LiMg shows a similar diffusion coefficient of  $1.4 \times 10^{-11} \text{ cm}^2\cdot\text{s}^{-1}$  to that of bulk Li ( $1.1 \times 10^{-11} \text{ cm}^2\cdot\text{s}^{-1}$ ). The calculated diffusion coefficients of LiMg are consistent with the measured  $D_{eff}$  ( $3.42 \times 10^{-11} \text{ cm}^2\cdot\text{s}^{-1}$ ) obtained by fitting the experimental data in **Figure 5-12 f**. However, the surface diffusion coefficients of Li and LiMg are over 3 magnitudes higher than those in the bulk (**Figure 5-12 b**). LiMgLa anodes have a higher specific surface and grain boundary area than Li and LiMg, enabling faster Li diffusion because of the higher defect concentration at surfaces and grain boundaries.



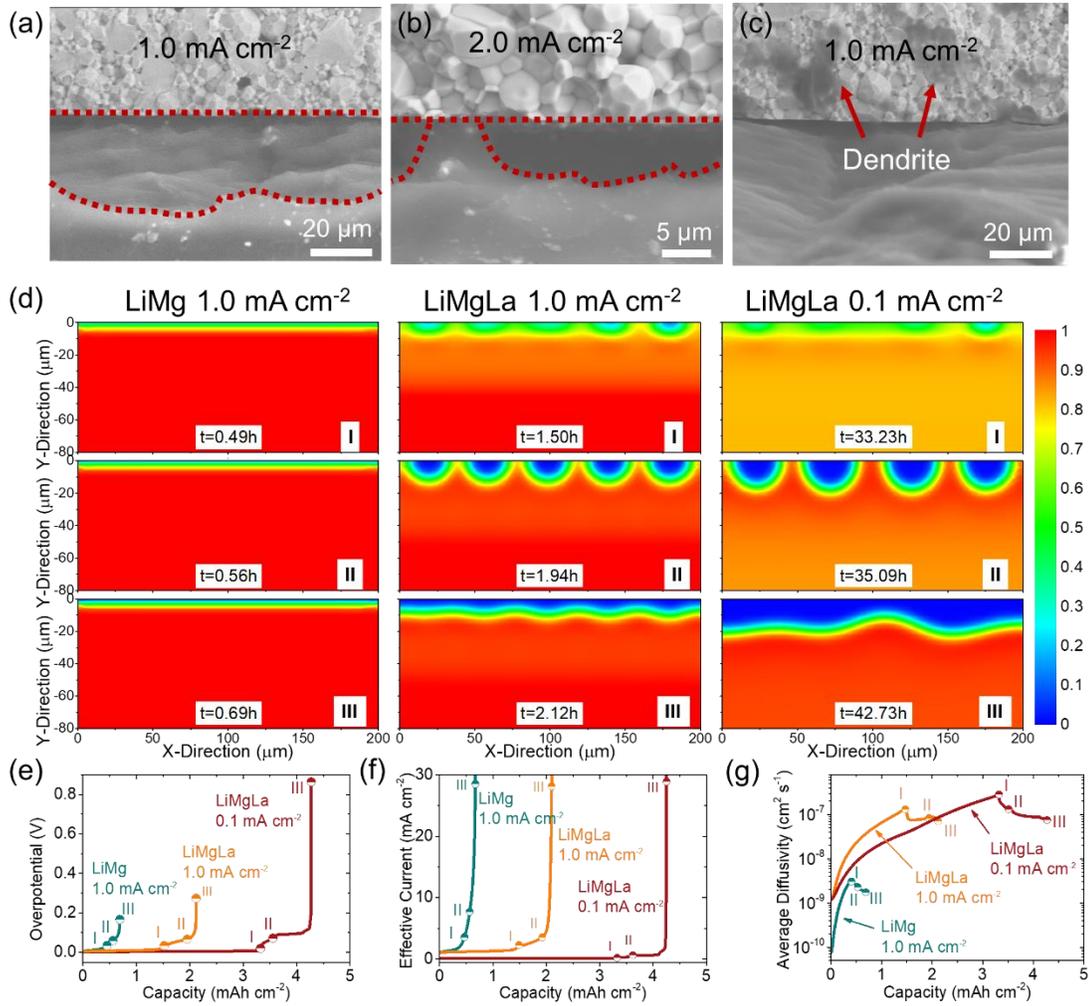
**Figure 5-14** (a) Phase diagram from the Materials Project and (b) Wulff shape constructed by calculating the surface energies of different slabs. The picture is generated by using Pymatgen. The Wulff shape indicates that the  $\text{La}_3\text{Mg}$  particle is domain by the (100) surface.

The mechanism by which the Mg-La inoculant refines the Li microstructure was analysed. According to the ternary phase diagram (**Figure 5-14 a**), the added La in

Mg can form  $\text{LaMg}_3$  compounds, while no intermetallic compound is formed for Li and La. The formed  $\text{LaMg}_3$  with a higher melting point would act as a crystal nucleus when cooling down the molten  $\text{LiMgLa}$  alloy. Due to its small size,  $\text{LaMg}_3$  cannot be indexed in X-ray diffraction (XRD) of the  $\text{LiMgLa}$  anode (**Figure 5-12 c**) due to its weak crystallinity along the (110) orientation. The Wulff shape (**Figure 5-14 b**) for  $\text{LaMg}_3$  has been constructed by calculating the surface energies of different orientations to provide a panorama of the  $\text{LaMg}_3$  nucleus. The atomic interfaces for  $\text{LaMg}_3(100)$  with  $\text{Li}(110)$  and  $\text{Li}(100)$  have been optimized by first-principles calculations based on density functional theory (**Figure 5-12 d**). The atomic structures suggest that the  $\text{LaMg}_3(100)$  surface assists in forming amorphous Li along the (110) orientation and well-crystallized Li along the (100) orientation, corresponding to the XRD patterns. The distribution of charge density differences indicates that the interfacial interaction is electrostatic in nature. The characterizations reveal that codoped Mg-La in Li forms  $\text{LaMg}_3$  intermetallic compounds, serving as excellent nuclei for the crystallization of Li solid solutions. The nucleus refines the grain size and changes the orientation and crystallization of the Li when annealing. The smaller grain size and amorphous Li with a higher defect concentration enhance the diffusion of  $\text{LiMgLa}$  anodes.

### 5.6 Void Evolution at the Interface with a High VSC Anode

**Figure 5-15** a-b show the SEM cross-sections of the LiMgLa|LLZTO interfaces after Li stripping at currents of 1.0 and 2.0 mA·cm<sup>-2</sup>, respectively. Voids are clearly observed in both currents, but the void depth of the LiMgLa|LLZTO interface after depletion at 1.0 mA·cm<sup>-2</sup> is significantly larger than that at 2.0 mA·cm<sup>-2</sup>, indicating that the smaller current density enables deeper Li stripping since VSC is a constant for the LiMgLa anode. Dendrite can be found inside the LLZTO pellets over the void after the plating process (**Figure 5-15** c).



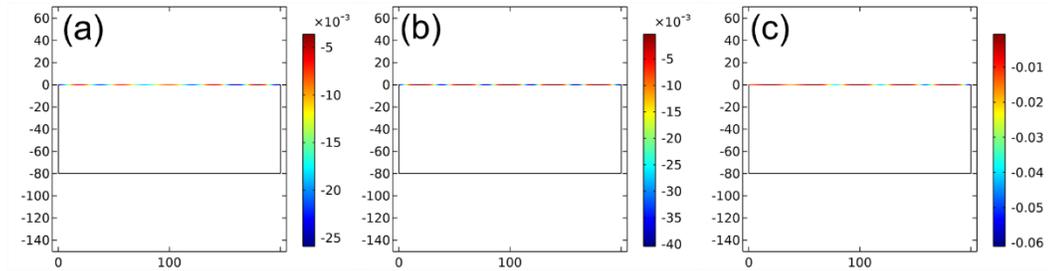
**Figure 5-15 Interface evolution of the LiMg and LiMgLa anodes during stripping at different current densities.** SEM cross-sections of the LiMgLa|LLZTO interface after full depletion at current densities of (a) 1.0 and (b) 2.0 mA·cm<sup>-2</sup> and (c) subsequently plated and shorted interface at 1.0 mA·cm<sup>-2</sup>. The voids are demarcated by the red dashed lines. (d) Snapshots of void phase at various evolution times and the corresponding (e) Butler-Volmer reaction overpotential, (f) effective current densities showing the current constriction, and (g) average diffusion coefficients for the LiMg anode at 1.0 mA·cm<sup>-2</sup>, LiMgLa anode at 1.0 mA·cm<sup>-2</sup>, and LiMgLa anode at 0.1 mA·cm<sup>-2</sup>. The order parameters ( $\xi$ ) are listed as  $\xi=1$  stands for lithium and  $\xi=0$  represents the void phase.

The dynamic void formation process at the Li|LLZTO interface during the Li stripping process was simulated using a mesoscale phase-field method (Figure 5-1

and **Table 5-1**). Snapshots of lithium ( $\xi=1$ , red) and void phases ( $\xi=0$ , blue) for LiMg and LiMgLa at various times and currents are captured to illustrate the evolution of the anodes (**Figure 5-15 d**).

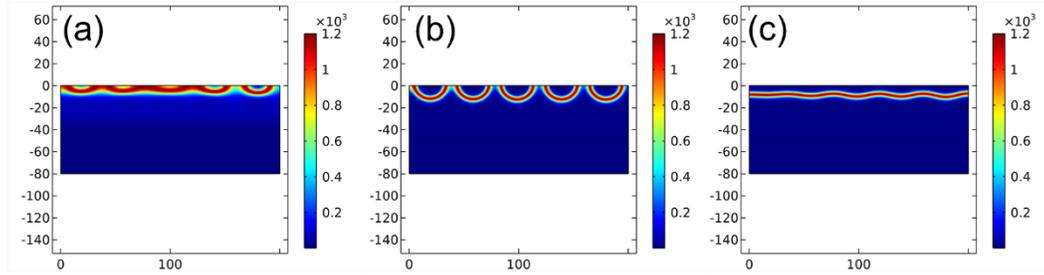
For Stage I, the lithium concentration near the Li|LLZTO interface gradually decreases, resulting in a density-gradient solid-solution reaction without void formation. The delivered capacities for LiMg at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  are  $0.49 \text{ mAh}\cdot\text{cm}^{-2}$ , LiMgLa at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  are  $1.50 \text{ mAh}\cdot\text{cm}^{-2}$ , and LiMgLa at  $0.1 \text{ mA}\cdot\text{cm}^{-2}$  are  $3.32 \text{ mAh}\cdot\text{cm}^{-2}$ . The corresponding depletion depths are approximately 5, 40, and 80  $\mu\text{m}$ , respectively. Upon further Li tripping, LiMgLa goes to Stage II with the phase transformation process by the formation of vacancies at the interfaces. The void at the LiMgLa|LLZTO interface is formed at 1.94 h with a current of  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  and at 35.09 h with a current of  $0.1 \text{ mA}\cdot\text{cm}^{-2}$ . The voids demonstrate a circular shape. The number of voids at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  is larger, but the depth of the voids is smaller than those at  $0.1 \text{ mA}\cdot\text{cm}^{-2}$ . Stage III presents detached interfaces with full lithium stripping. For LiMg anodes at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$ , Li was completely depleted at only  $0.69 \text{ mAh}\cdot\text{cm}^{-2}$  without the formation of a void. For the LiMgLa anodes, the anodes detach from the SSEs when the voids merge into one piece. The full depletion capacities of the LiMgLa anodes are  $2.12 \text{ mAh}\cdot\text{cm}^{-2}$  at a current of  $1.0 \text{ mA cm}^{-2}$  and  $4.27 \text{ mAh}\cdot\text{cm}^{-2}$  at a current of  $0.1 \text{ mA}\cdot\text{cm}^{-2}$ , corresponding to void depths over 10 and 20  $\mu\text{m}$ , respectively. The simulated results are consistent with the SEM cross-sections shown in **Figure 5-15 a-b**, suggesting that the simulations capture the key phenomenon of the anodic dissolution process. Interestingly, the anode evolution behavior is

counterintuitive, as the void is not forming and evolving along the whole stripping process but only at the late stage of Li stripping (**Supplementary Video**).



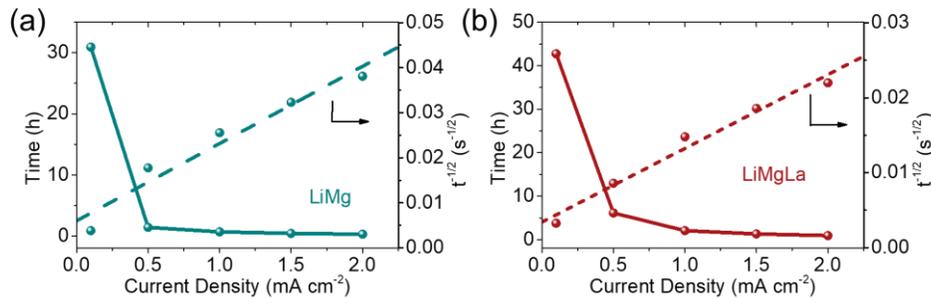
**Figure 5-16** Local current density distribution for the LiMgLa|LLZTO interfaces after stripping at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  for (a) 1.50 h, 1.94 h, and 2.12 h. The inhomogeneous distribution of the current densities during anodic dissolution indicates a current constriction resulting from the morphological evolution of anodes. As the stripping time increases, the current constriction is aggravated.

The simulated overpotential profiles for the Butler-Volmer reaction overpotential in **Figure 5-15 e** exhibit the same trends as the experimental voltage profiles (**Figure 5-7 b and e** and **Figure 5-11**). The overpotential is flat in Stage I, gradually increases between Stage I and Stage II, and rises rapidly between Stage II and Stage III. These results further confirmed that the abrupt increase in the voltages (**Figure 5-7 b**) during Li stripping comes from the mass-transfer overpotential. The profiles of effective current densities (**Figure 5-15 f**) and the spatial distribution of the current (**Figure 5-16**) at the interface indicate that the severe contact loss during dissolution, especially after the void formed, induces a high constriction of the current. The constricted current induced a high local overpotential across the SSE, acting as the driving force for SSE reduction and dendrite formation.



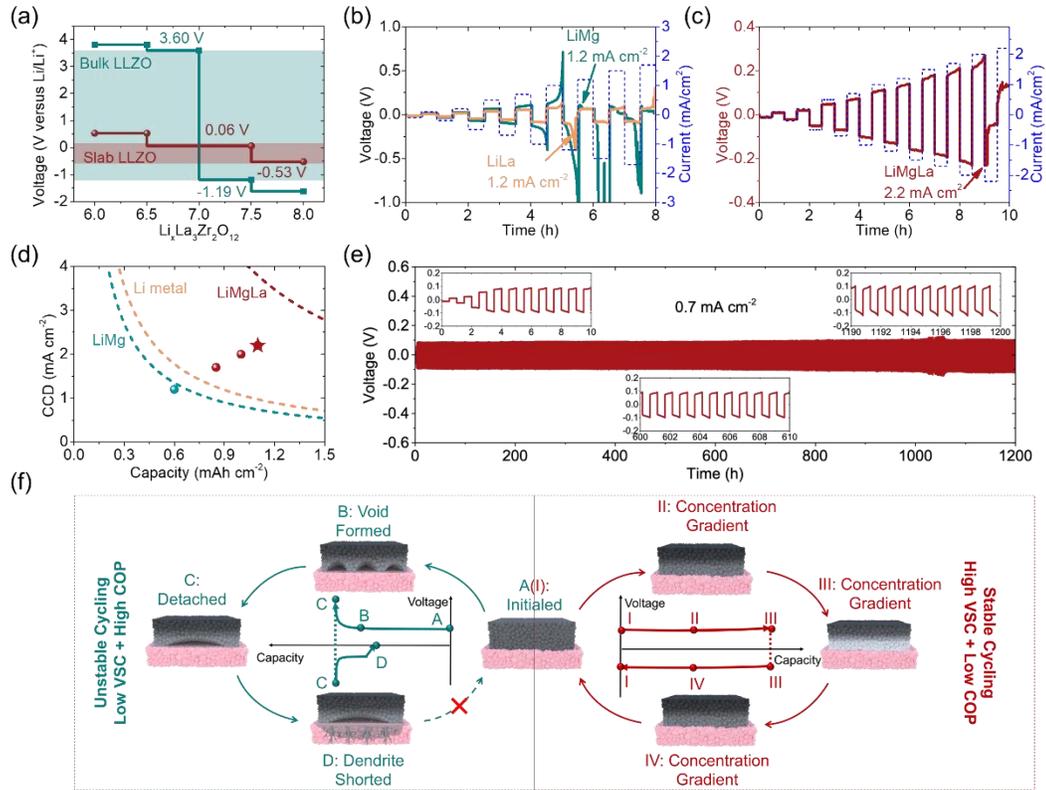
**Figure 5-17** Spatial distribution of the normalized diffusion coefficient for the LiMgLa/LLZTO interfaces after stripping at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  for (a) 1.5, 1.94, and 2.12 h. The distribution of the diffusion coefficient shows a decrease in the diffusion path for Li during anodic dissolution.

The evolution of the average (**Figure 5-15 g**) and spatial distribution (**Figure 5-17**) of the diffusion coefficients in the LiMgLa anode demonstrated that the average Li diffusivities of the anodes increased and reached their maximum at Stage I while slightly decreasing during the subsequent stripping process. The reason for the fast phase transformation to form voids is that the high diffusion coefficient at Stage I enables a fast accumulation of vacancies at the interface. Since the delivered capacity



**Figure 5-18** The phase-field modeled current density and depletion time dependence, and Sand's equation fitted (dotted lines) lithium diffusion coefficients for LiMg and LiMgLa anodes.

from Stage I to Stage III is small and void formation leads to unrecoverable morphological instability, lithium utilization within Stage I (~70% of full depletion capacity) is highly recommended for stable cycling, which was confirmed by recent work<sup>13</sup>.

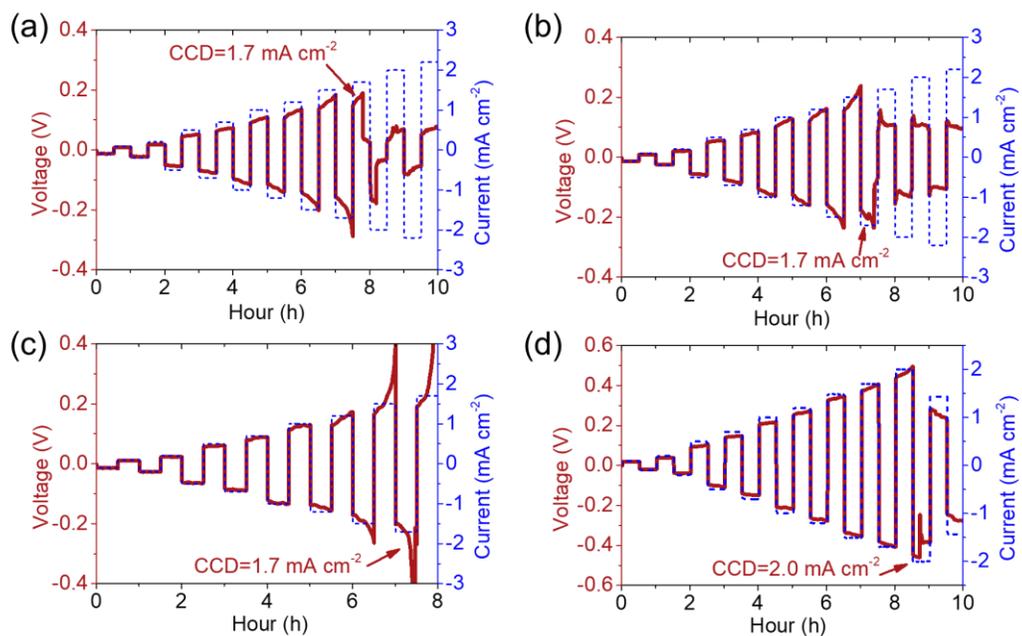


**Figure 5-19 Electrochemical characterization of LiMgLa anodes in a solid-state symmetric cell at room temperature.** (a) The calculated electrochemical stability window versus  $\text{Li/Li}^+$  for bulk (cyan region) and slab (red region)  $\text{Li}_x\text{La}_3\text{Zr}_2\text{O}_{12}$ . CCD measurements for symmetric cells with (b) LiMg, LiLa and (c) LiMgLa as anodes. (d) Comparison of CCD versus capacity for LiMg and LiMgLa anodes. The red dots indicate high reproducibility, as detailed in **Fig. S22**. (e) Cycling performance of LiMgLa|LLZTO|LiMgLa symmetric cells with a current density of 0.7  $\text{mA cm}^{-2}$  for a capacity of 0.35  $\text{mAh cm}^{-2}$ . (f) Interfacial evolution of unstable cycling with a low VSC anode and high COP SSE and stable cycling with a high VSC anode and low COP SSE.

Moreover, the simulated VSC (maximum capacity dependence on the rates) for LiMg and LiMgLa confirms the linear relationship between the current densities and  $\tau^{-1/2}$  (**Figure 5-18**). Increasing the diffusion coefficient is an effective strategy to enable fast-charging cells with high capacity by enlarging the duration to reach stage I. Another feasible way is to enhance the utilization of Li by suppressing the phase transformation utilizing elevated pressure.

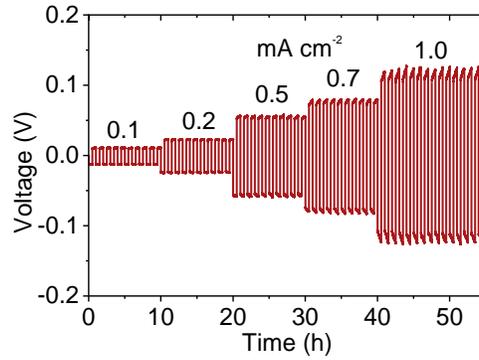
### 5.7 Electrochemical Performance with a High VSC Anode

To evaluate the dendrite suppression ability for the LiMg, LiLa, and LiMgLa anodes, the CCDs are obtained by the plating/stripping profiles using a stepwise current density for a fixed 0.5 hour. For both the LiMg and LiLa anodes (**Figure 5-19 b**), a steep increase in voltage occurs at a current of  $1.2 \text{ mA}\cdot\text{cm}^{-2}$ , while a short circuit then takes place with an abrupt voltage drop. The large polarizations at high current densities are believed to be related to the formation of voids. In sharp contrast, the LiMgLa anode enables a high CCD of  $2.2 \text{ mA}\cdot\text{cm}^{-2}$  with small voltage polarization even before the short circuit (**Figure 5-19 c**). The voltages of the plateaus roughly obey Ohm's law at low current densities, indicating no "soft" short during the process.



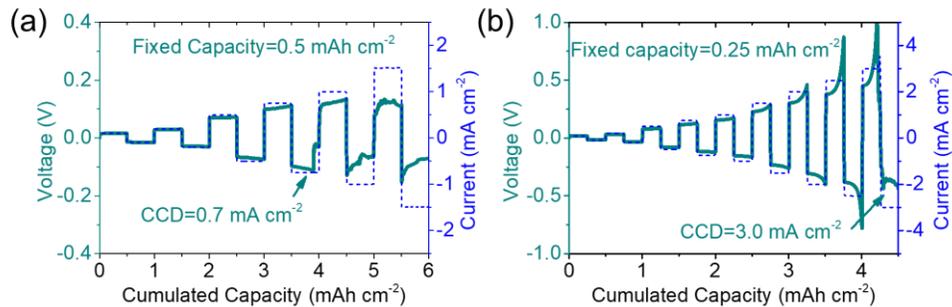
**Figure 5-20** CCD measurements for symmetric cells with LiMgLa as anodes showing the high reproducibility.

The LiMgLa anodes have a high CCD of  $2.2 \text{ mA cm}^{-2}$  due to their high VSC, which simultaneously increases the CCD and deliverable capacity (**Figure 5-19 d** and **Figure 5-20**). The LiMgLa anode enables stable cycling at  $0.7 \text{ mA}\cdot\text{cm}^{-2}$  for over 1,200 hours and a high accumulated capacity of  $>420 \text{ mAh}\cdot\text{cm}^{-2}$  (**Figure 5-19 e**).



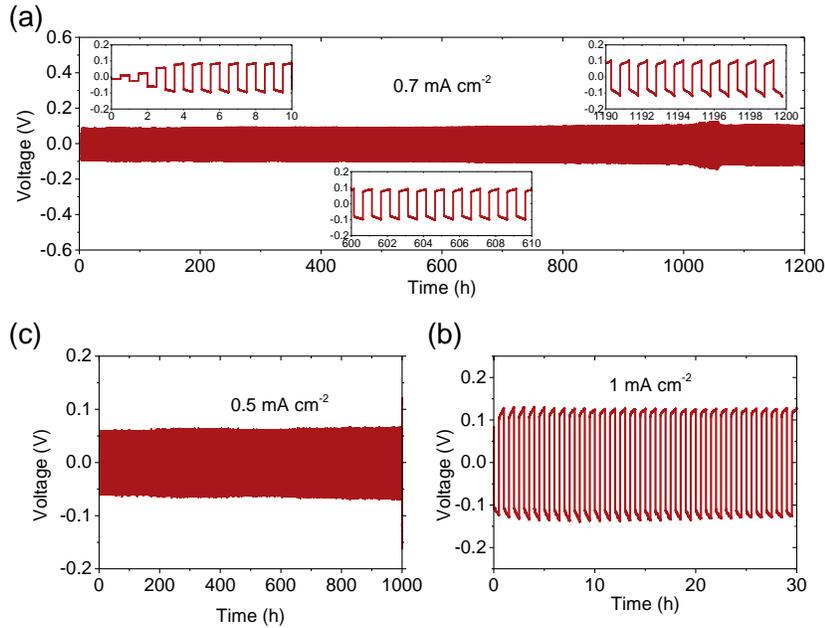
**Figure 5-21** Rate performance of symmetric cell with LiMgLa anode at a step-increase current densities of 0.1, 0.2, 0.5, 0.7, and 1.0 mA·cm<sup>-2</sup> for 10 cycles at each current density.

Moreover, the rate performance of the symmetric cell with the LiMgLa anode is tested at step-increase currents of 0.1, 0.2, 0.5, 0.7, and 1.0 mA·cm<sup>-2</sup> for 10 cycles at each current density, showing a promising high-rate capability (**Figure 5-21**). The symmetric cell with the LiMgLa anode shows stable and smooth cycling plateaus even at a large current density of 1.0 mA·cm<sup>-2</sup> at room temperature (**Figure 5-23**).



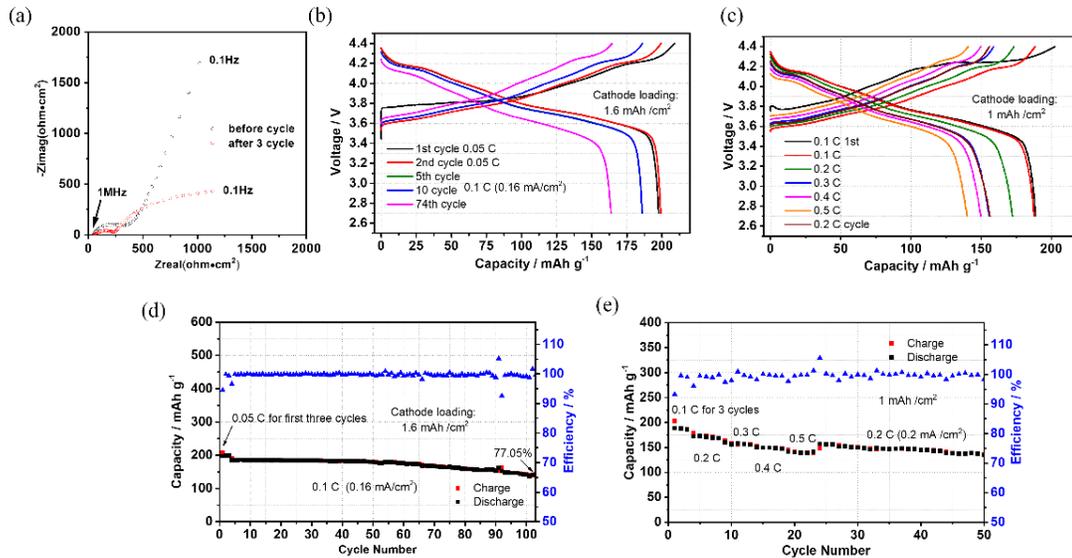
**Figure 5-22** Critical current density measurements for Li<sub>97.5</sub>Mg<sub>2.5</sub>|LLZTO|Li<sub>97.5</sub>Mg<sub>2.5</sub> symmetric cells at a fixed capacity of (a) 0.5 mAh·cm<sup>-2</sup> and (b) 0.25 mAh·cm<sup>-2</sup>. The measured CCD values are 0.7 mA·cm<sup>-2</sup> and 3.0 mA·cm<sup>-2</sup>, indicating that the CCD can be largely improved by reducing the cycling capacity.

The CCD for LiMg anodes can be significantly improved from 0.7 to 3.0 mA·cm<sup>-2</sup> when reducing the cycling capacity from 0.50 to 0.25 mAh·cm<sup>-2</sup> (**Figure 5-22**), further confirming the importance of VSC.



**Figure 5-23** Galvanostatic cycling of the LiMgLa|LLZTO|LiMgLa symmetric cell at 0.7, 0.5 and 1.0 mA·cm<sup>-2</sup> at room temperature. The symmetric cell with LiMgLa electrodes enables stable and smooth cycling at a large current density.

The LiMgLa|LLZTO|LiNi<sub>0.8</sub>Mn<sub>0.1</sub>Co<sub>0.1</sub>O<sub>2</sub> (NMC811) proof-of-concept cells demonstrate excellent cyclability and rate performance (**Figure 5-24**). The overall characterization of the EIS, CCD, rate performance, and cycling stability at a high current density suggests that the LiMgLa anodes have superior dendrite suppression ability with the LLZTO SSE, resulting from significant improvement of VSC.



**Figure 5-24** Electrochemical performance of the LiMgLa|LLZTO|NMC811 cell. (a) Nyquist spectra of the solid-state cell before and after 3 cycles with a constant current of 0.1 C. The electrochemical charge/discharge curves of the solid cell at (b) 0.1 C and (c) different rates from 0.1 to 0.5 C. (d) Cycling performance of the cell at a current density of 0.1 C. (e) Rate performance of the cell.

Comprehensive characterization, simulation and experiments demonstrated that Li dendrite growth occurs when the Li anode overpotential is higher than COP. The COP mainly depends on the lithiophobicity and mechanical and chemical stability of the SSE, while the Li anode overpotential mainly depends on the VSC, i.e., Li diffusivity and Li concentration. For a Li anode with a low VSC and a low COP, voids will be formed when the delivered capacity exceeds 70% of the maximum capacity (**Figure 5-19** f, left). The voids even detached Li from the SSE surface, leading to a rapid increase in the Li plating overpotential to be larger than COP, which accelerated dendrite formation inside the SSE. The unstable anode and SSE fail the cells rapidly. However, when using an anode with high VSC and an electrolyte with high COP, the Li anode undergoes recoverable concentration

depletion with low polarization without void formation, while the high COP of the SSE enables the Li metal cell to achieve a long cycle life even at a high rate with high capacity (**Figure 5-19** f, right). This study provides guidelines for SSE modification, interface engineering and Li anode doping to simultaneously achieve high capacity and long cycle life.

### 5.8 Conclusion

Void formation at the Li/SSE interface is controlled by the Li diffusivity and Li concentration at the Li/SSE interface. The products of full depletion capacity and stripping current can be used to evaluate the void suppression capability (VSC). The Li anode with a high VSC will not form voids even at a high capacity and current, which reduces the overpotential. To enhance the VSC of Li anodes, Mg and La were codoped into a Li metal anode to achieve a high Li diffusivity by refining the Li grain size. The induced Mg-La enhances the lithium diffusivity by 10 times compared to the LiMg alloy. The LiMgLa anode delivers a high critical capacity of  $4.1 \text{ mAh}\cdot\text{cm}^{-2}$  at  $1.0 \text{ mA}\cdot\text{cm}^{-2}$ , which is 10 times higher than that of the LiMg anode. The high critical rate capacity enables a high CCD of  $2.0 \text{ mA}\cdot\text{cm}^{-2}$  with a capacity of  $1.0 \text{ mA}\cdot\text{cm}^{-2}$  and a high cumulative capacity over  $420 \text{ mAh}\cdot\text{cm}^{-2}$ . The evolution of the anode during anodic dissolution is revealed by the phase-field model, in which the anode proceeds in three stages: solid-solution, phase transformation, and detachment. The higher diffusion coefficient of LiMgLa extends the solid solution and suppresses void formation. The LiMgLa anode provides a chemical strategy to simultaneously

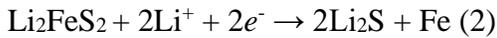
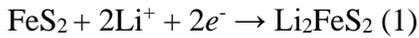
improve the fast-charge and high-capacity requirements to match the requirement for  
ASSLMBs.

## Chapter 6 Triple-Phase Design for Highly Reversible Sulfur Cathode in All-Solid-State Lithium-Sulfur Battery

### *6.1 Introduction*

Sulfur cathode is promising to be used in Li-metal batteries for practical application due to its high capacity and low cost. However, the sluggish reaction kinetics of S/Li<sub>2</sub>S and polysulfide shuttle in lithium-metal battery (LMB) using organic liquid electrolyte (LE) decrease the utilization of sulfur active materials. Using catalysts can promote the reversible reaction of polysulfide in LMB, thus extending the cycling life of sulfur cathode. To ensure a high polysulfide reversible reaction in LMB, the polysulfide adsorption ability and catalytic activity of the catalyst has to be balanced. The strong adsorption of the polysulfide will lead to the catalyst passivation, while, a poor adsorption can not effectively ameliorate the polysulfide shuttle<sup>96</sup>. However, the formation and dissolution of polysulfide in LE still can not be fully suppressed, which affects the long cycle life of sulfur cathode in LMB. Replacing organic liquid electrolyte to solid-state electrolyte (SSE) can prevent the formation of polysulfide and eliminate the polysulfide shuttle effect. However, the slow reaction kinetics of S/Li<sub>2</sub>S in all-solid-state lithium battery (SSLB) is more severe than that in LMB. In LMB, the S/Li<sub>2</sub>S is surrounded by LE, the Li<sup>+</sup> transfer between LE and S/Li<sub>2</sub>S is not the determining factor influencing the reaction kinetics of S/Li<sub>2</sub>S. While, in ASSLB, the limited interfacial contact at electronic additive/SSE/sulfur triple-phase boundaries restricts the utilization of sulfur active material. Improving the Li<sup>+</sup> transfer

through coating SSE on sulfur, or enhancing the  $e^-$  conduction using electronic conductive carbon as sulfur host can enhance S/Li<sub>2</sub>S redox reaction due to the improved triple-phase contacts in these modified sulfur composite cathode. However, the preparation procedures for these modified sulfur cathodes are time-consuming. Besides, the low active sulfur content in the S@C composite will decrease the cell-level energy density because the large amount of electronic conductive carbon host can not provide capacity to the battery. Therefore, sulfur host that can provide extra capacity was introduced into the sulfur composite<sup>22,23,97</sup>. Among these active sulfur hosts, FeS<sub>2</sub> with high electronic/ionic conductivity has been demonstrated to mediate the sulfur redox reaction in SSLB<sup>22</sup>. During lithiation/delithiation process at cut-off voltage of 1.0~3.0V, the following reactions occur in FeS<sub>2</sub>, and reaction (5) is the rate determining procedure for the electrochemical reversibility of FeS<sub>2</sub>.



Introducing transition metal into FeS<sub>2</sub> can improve the reaction kinetics of reaction (5).<sup>98</sup> However, the volume expansion of FeS<sub>2</sub> after fully lithiation remains unsolved, which will lead to the structure collapse of FeS<sub>2</sub>@S composite during long cycles,

thus resulting in rapid capacity decay of FeS<sub>2</sub>@S composite when the capacity is fully utilized<sup>2</sup>. Therefore, to stabilize the structure of FeS<sub>2</sub>@S composite in SSLB, the cell cut-off voltage was restricted at 1.5~2.8V<sup>23</sup>, where reaction (1) with small volume change and high reversibility proceeds in FeS<sub>2</sub>. However, the delivered capacity of FeS<sub>2</sub>@S composite was reduced when restricting the cut-off voltage to 1.5~2.8V. How to maintain a good cycling stability with a high capacity utilization of FeS<sub>2</sub>@S composite at high cathode loading remains challenging.

Increasing the Li<sup>+</sup>/e<sup>-</sup> transfer inside the bulk material or at the phase boundary of different components can enhance the reaction kinetics of the composite cathode in ASSLB. Therefore, to fully utilize the capacity of FeS<sub>2</sub>@S composite, a bridge with fast Li<sup>+</sup> diffusivity should be *in-situ* formed at FeS<sub>2</sub>-S-Li<sub>6</sub>PS<sub>5</sub>Cl triple phase boundary during the initial few delithiation/lithiation process to ensure high Li<sup>+</sup> exchange in FeS<sub>2</sub>@S-Li<sub>6</sub>PS<sub>5</sub>Cl-C composite cathode during the following cycles. We have demonstrated that introduction of LiI into Li<sub>2</sub>S can significantly improve the reversibility of S/Li<sub>2</sub>S redox reaction due to the reduced Li-S bond and improved ionic conductivity of Li<sub>2</sub>S@LiI composite<sup>99</sup>. Besides, Wagemaker's group<sup>100</sup> also demonstrated that the LiI coating on Li<sub>2</sub>S can improve the Li<sup>+</sup> diffusivity over Li<sub>6</sub>PS<sub>5</sub>Cl/Li<sub>2</sub>S interface, where LiI acts as a Li<sup>+</sup> transfer bridge between Li<sub>6</sub>PS<sub>5</sub>Cl and Li<sub>2</sub>S. Therefore, to improve the reaction kinetics of FeS<sub>2</sub>@S, transition metal iodide should be chosen as dopant, because transition metal iodide can *in-situ* transfer to LiI and transition metal when FeS<sub>2</sub>@S was fully lithiated, where transition metal can improve the reaction kinetics of FeS<sub>2</sub>, and LiI acts as a bridge at FeS<sub>2</sub>-S-Li<sub>6</sub>PS<sub>5</sub>Cl

phase boundary in FeS<sub>2</sub>@S-Li<sub>6</sub>PS<sub>5</sub>Cl composite cathode to improve the redox kinetics of S/Li<sub>2</sub>S, thus enhancing the electrochemical performance. To demonstrate this assumption, CuI was chosen as dopant in this work. After the first few cycles, FeS<sub>2</sub>@S@CuI composite *in-situ* transfers to FeS<sub>2</sub>@S@Cu@LiI, the *in-situ* built fast e<sup>-</sup>/Li<sup>+</sup> transfer in FeS<sub>2</sub>@S composite enables FeS<sub>2</sub>@S composite to cycle even without addition of Li<sub>6</sub>PS<sub>5</sub>Cl electrolyte and electronic conductive carbon into the cathode. The impedance spectra show that at the third fully lithiated state (discharge to 1.0V), the interfacial resistance in FeS<sub>2</sub>@S@CuI composite was decreased, because of the enhanced Li<sup>+</sup> exchange at FeS<sub>2</sub>-S-Li<sub>6</sub>PS<sub>5</sub>Cl triple-phase boundary. While for FeS<sub>2</sub>@S composite without CuI doping, the impedance increases continuously during discharge/charge processes due to the volume expansion of FeS<sub>2</sub>@S when fully lithiation, which leads to the contact loss at FeS<sub>2</sub>-S-Li<sub>6</sub>PS<sub>5</sub>Cl triple phase boundary and structure collapse of the composite cathode. Besides, the XRD pattern shows that CuI can promote the amorphization of S in FeS<sub>2</sub>@S composite, which can further decrease the reaction barriers of S/Li<sub>2</sub>S redox reaction. Benefited from these merits, the FeS<sub>2</sub>@S@CuI composite delivers a high reversible capacity of 4.0 mAh cm<sup>-2</sup> with a high initial Coulombic Efficiency of 94.6% at current density of 0.5 mA cm<sup>-2</sup> under room temperature. After five cycles, the capacity utilization of FeS<sub>2</sub>@S@CuI composite reaches to 96.5%. Even at low temperature, the FeS<sub>2</sub>@S@CuI composite cathodes deliver specific capacity of 499.9 mAh g<sup>-1</sup> (44.4% of capacity utilization) at -20°C, and 374.4 mAh g<sup>-1</sup> (33.3% of capacity utilization) at -30°C. Furthermore, the FeS<sub>2</sub>@S@CuI composite cathode with high areal capacity of 4.0 mAh cm<sup>-2</sup> also shows good cycling stability with

capacity retention of 88.8% after 145 cycles. Such a high capacity utilization and good cycling stability at high cathode loading has never been reported in ASSLB.

## 6.2 Experimental

### 6.2.1 Synthesis of FeS<sub>2</sub>@S@CuI and FeS<sub>2</sub>@S composite

FeS<sub>2</sub>@S@CuI was prepared by ball-milling procedures. Typically, FeS<sub>2</sub> and CuI with mole ratio of 9: 1 was ball-milled at 500 rpm for 12h. Then, the obtained FeS<sub>2</sub>@CuI and S with weight ratio of 1: 1 was further ball-milled at 500 rpm for 12.0 hours to obtain the final FeS<sub>2</sub>@S@CuI composite. FeS<sub>2</sub>@S was prepared by the same ball-milling procedures without adding CuI.

The theoretical capacity of S is 1673 mAh g<sup>-1</sup>, and FeS<sub>2</sub> is 894 mAh g<sup>-1</sup>. Therefore, the theoretical capacity of FeS<sub>2</sub>@S composite is (1673+894)/2=1283.5 mAh g<sup>-1</sup>. The weight ratio of FeS<sub>2</sub> in the FeS<sub>2</sub>@S@CuI composite was 42.5%, and the weight ratio of S in the FeS<sub>2</sub>@S@CuI composite was 50%. Therefore, the theoretical capacity of FeS<sub>2</sub>@S@CuI composite is 1673×0.5+894×0.425=1216.45 mAh g<sup>-1</sup> based on the weight of FeS<sub>2</sub>@S, and 1216.45×0.925=1125.2 mAh g<sup>-1</sup> based on the weight of FeS<sub>2</sub>@S@CuI.

### 6.2.2 Electrochemical Measurements

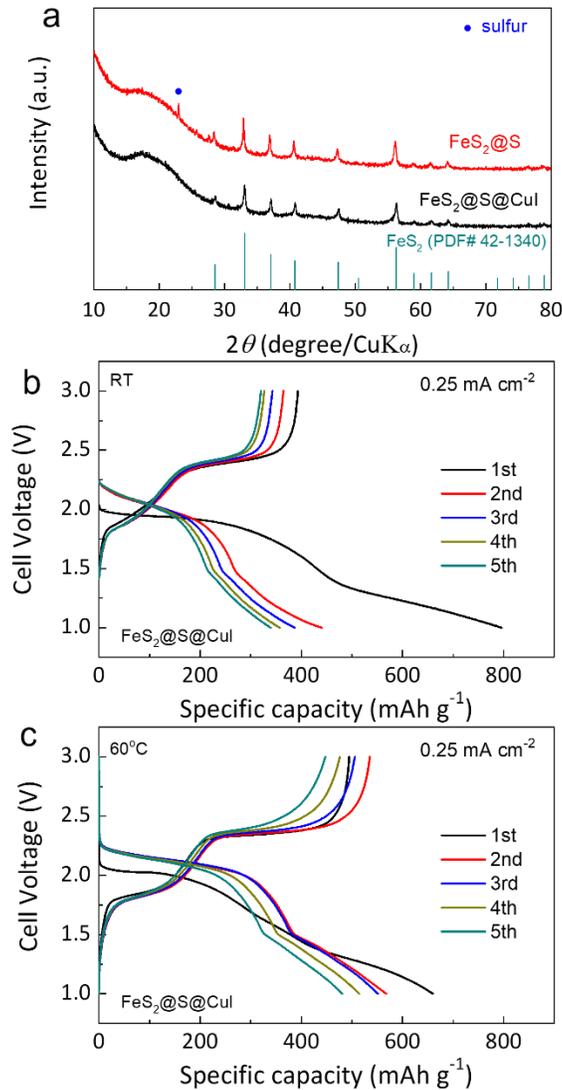
Before assembling all-solid-state battery, FeS<sub>2</sub>@S@CuI and C with weight ratio of 5: 1 was ball-milled, then the obtained FeS<sub>2</sub>@S@CuI-C was hand mixed with Li<sub>6</sub>PS<sub>5</sub>Cl

with weight ratio of 6: 4 to form FeS<sub>2</sub>@S@CuI-C-Li<sub>6</sub>PS<sub>5</sub>Cl composite cathode. All-solid-state battery was assembled as following. Firstly, 100 mg of Li<sub>6</sub>PS<sub>5</sub>Cl electrolyte was pressed at 2 ton to form a pellet with diameter of 10 mm. Then, the composite cathode material was spread on one side of Li<sub>6</sub>PS<sub>5</sub>Cl electrolyte and pressed at 4 ton. After that, LiIn anode was attached on the other side of Li<sub>6</sub>PS<sub>5</sub>Cl electrolyte.

The electrochemical performances of the fabricated all-solid-state lithium battery were evaluated on an Arbin BT2000 workstation (Arbin Instruments, TX, USA). To investigate impact of CuI doping on the redox kinetics of FeS<sub>2</sub>@S, cyclic voltammetry (CV) was measured at a scan rate of 0.2 mV s<sup>-1</sup>. Electrochemical impedance spectroscopy (EIS) analyses were conducted on Gamry instrument at frequencies from 1 MHz to 0.1 Hz with the amplitude of 15 mV under argon.

### 6.3 High e<sup>-</sup>/Li<sup>+</sup> Exchange across the FeS<sub>2</sub>@S@CuI

FeS<sub>2</sub>@S@CuI composite was prepared by ball-milling procedures, where the mole ratio of FeS<sub>2</sub> and CuI was 9: 1, and the weight ratio of FeS<sub>2</sub>@CuI: S was 50: 50. As shown in **Figure 6-1** a, after ball-milling, the diffraction peaks for sulfur disappeared in FeS<sub>2</sub>@S@CuI composite. While the sulfur diffraction peaks still maintain in FeS<sub>2</sub>@S composite without CuI, implying the introduction of CuI additive can promote the amorphization of S in FeS<sub>2</sub>@S composite, which will decrease the reaction barriers of S/Li<sub>2</sub>S redox reaction.



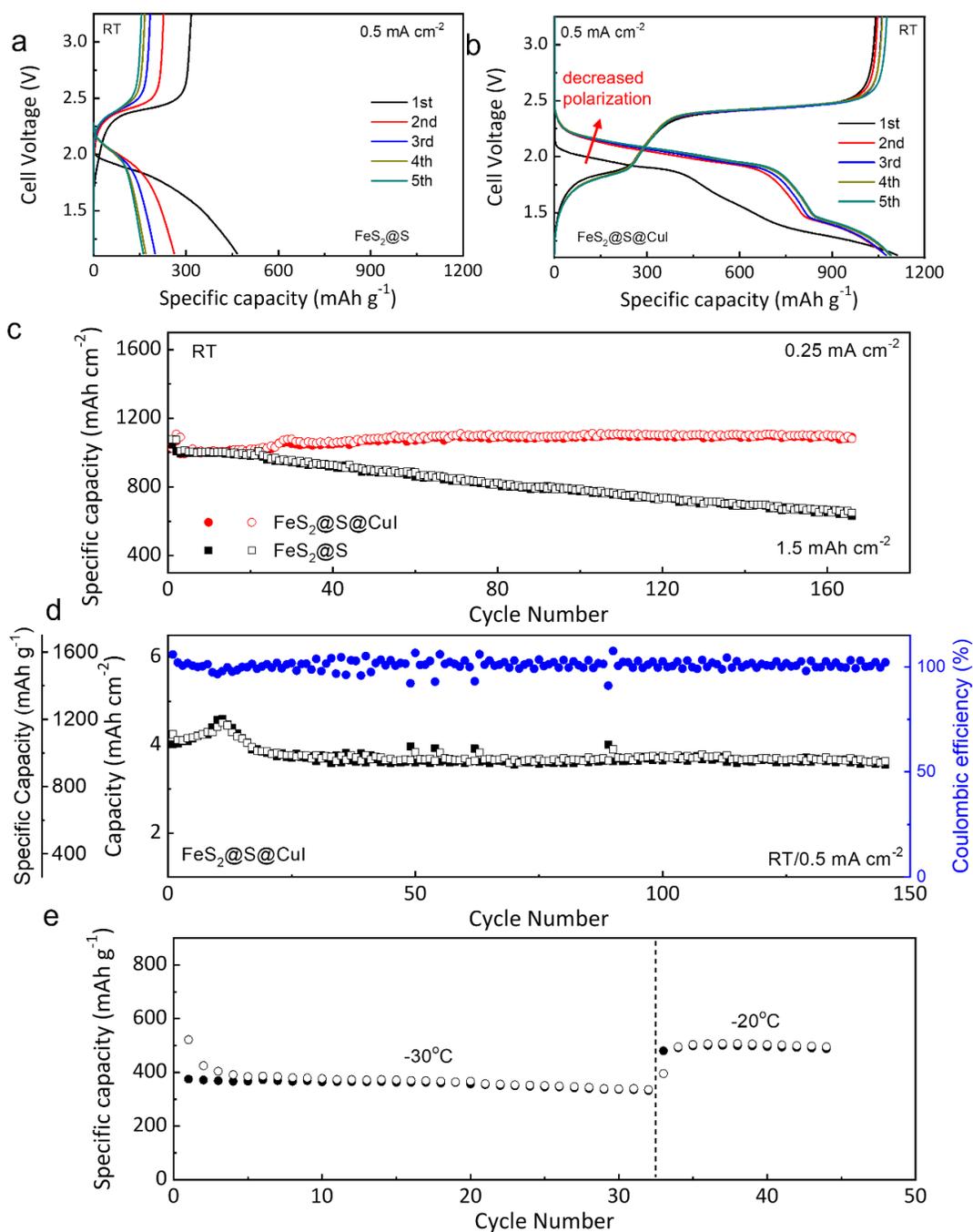
**Figure 6-1** (a) XRD patterns of  $\text{FeS}_2@S$  and  $\text{FeS}_2@S@CuI$  composite. Galvanostatic discharge/charge profile of  $\text{FeS}_2@S@CuI$  composite at (b) room temperature and (c) temperature of  $60^\circ\text{C}$  without addition of  $\text{Li}_6\text{PS}_5\text{Cl}$  electrolyte and conductive carbon in the cathode layer.

To demonstrate the *in-situ* formed fast  $e^-/\text{Li}^+$  transfer in  $\text{FeS}_2@S$  composite was achieved after  $\text{CuI}$  doping, all-solid-state battery using  $\text{FeS}_2@S@CuI$  cathode (without electrolyte and conductive carbon, cathode loading:  $1.3 \text{ mg cm}^{-2}$ ) were assembled. As shown in **Figure 6-1**,  $\text{FeS}_2@S@CuI$  cathode delivers initial reversible

capacity of 393.4 mAh g<sup>-1</sup> at room temperature (**Figure 6-1 b**, 35% of capacity utilization), and 535.4 mAh g<sup>-1</sup> at temperature of 60°C at the second cycle (**Figure 6-1 c**, 47.6% of capacity utilization) even without adding additional Li<sub>6</sub>PS<sub>5</sub>Cl electrolyte and electronic conductive carbon into the cathode, implying the high e<sup>-</sup>/Li<sup>+</sup> exchange in the *in-situ* formed FeS<sub>2</sub>@S@Cu@LiI composite after the first few lithiation/delithiation processes.

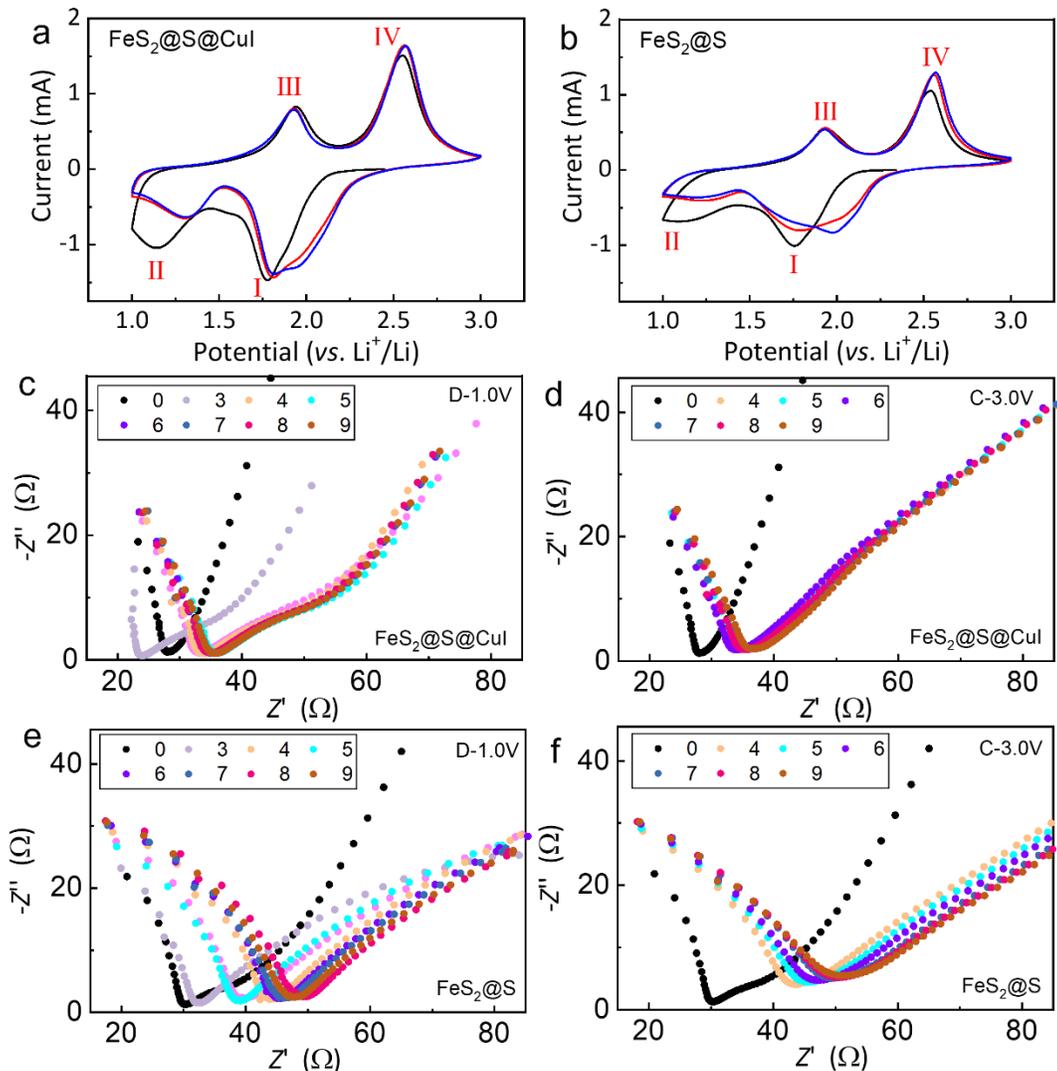
#### 6.4 Enhanced Kinetic in the FeS<sub>2</sub>@S@CuI Composite Cathode

To further improve the capacity utilization of FeS<sub>2</sub>@S@CuI, Li<sub>6</sub>PS<sub>5</sub>Cl solid electrolyte and electronic conductive carbon additive was further introduced forming FeS<sub>2</sub>@S@CuI-Li<sub>6</sub>PS<sub>5</sub>Cl-C composite cathode. Then, the electrochemical performance of FeS<sub>2</sub>@S@CuI-Li<sub>6</sub>PS<sub>5</sub>Cl-C composite cathode with areal capacity of 4 mAh cm<sup>-2</sup> was evaluated using LiIn alloy anode. As shown in **Figure 6-2 b**, for FeS<sub>2</sub>@S@CuI composite cathode, the first discharge plateau that corresponds to the lithiation of S to Li<sub>2</sub>S increased to higher potential after the initial cycle, and then the overpotential for S/Li<sub>2</sub>S redox reaction maintains almost constant in the following cycles. In sharp contrast, the FeS<sub>2</sub>@S composite cathode without CuI additive shows continuously increased S/Li<sub>2</sub>S redox overpotential (**Figure 6-2 a**), proving the introduction of CuI can significantly improve the reaction kinetics of S/Li<sub>2</sub>S after the initial lithiation of CuI to Cu@LiI composite.



**Figure 6-2** Galvanostatic discharge/charge profile of (a) FeS<sub>2</sub>@S and (b) FeS<sub>2</sub>@S@CuI composite cathode at room temperature. (c) Cyclic performance of FeS<sub>2</sub>@S composite cathode with and without CuI additive under areal capacity of 1.5 mAh cm<sup>-2</sup>. (d) Cyclic performance of FeS<sub>2</sub>@S@CuI composite cathode with areal capacity of 4.0 mAh cm<sup>-2</sup> at room temperature. (e) Cyclic performance of FeS<sub>2</sub>@S@CuI composite cathode at low temperature of -30°C and -20°C.

The improved S/Li<sub>2</sub>S redox kinetics leads to the FeS<sub>2</sub>@S@CuI composite cathode delivers a high reversible capacity of 4.0 mAh cm<sup>-2</sup> with a high initial Coulombic efficiency of 94.6% at current density of 0.5 mA cm<sup>-2</sup> under room temperature (**Figure 6-2 b**). Besides, after five cycles, the FeS<sub>2</sub>@S@CuI composite cathode shows a high reversible capacity of 1086.1 mAh g<sup>-1</sup>, corresponding to capacity utilization of 96.5% (**Figure 6-2b**). In sharp contrast, the reversible capacity of FeS<sub>2</sub>@S composite cathode decays to 162.2 mAh g<sup>-1</sup>, corresponding to capacity utilization of 12.6% at the fifth cycle. Such a modified FeS<sub>2</sub>@S@CuI composite cathode with areal capacity of 1.5 mAh cm<sup>-2</sup> can stable for >167 cycles at current density of 0.25 mA cm<sup>-2</sup> under room temperature (**Figure 6-2 c**). While, the FeS<sub>2</sub>@S composite cathode shows rapid capacity decay at the same cathode loading (Figure 2c). When further increasing the areal capacity to 4 mAh cm<sup>-2</sup>, the FeS<sub>2</sub>@S@CuI composite cathode still shows excellent cyclic performance with capacity retention of 88.8% after 145 cycles (**Figure 6-2 d**). Even at low temperature, the FeS<sub>2</sub>@S@CuI composite cathode can deliver specific capacity of 499.9 mAh g<sup>-1</sup> at -20°C, and 374.4 mAh g<sup>-1</sup> at -30°C (**Figure 6-2 e**). Such a high capacity utilization (44.4% of capacity utilization at -20°C, and 33.3% of capacity utilization at -30°C) at low temperature has never been reported in SSLBs.

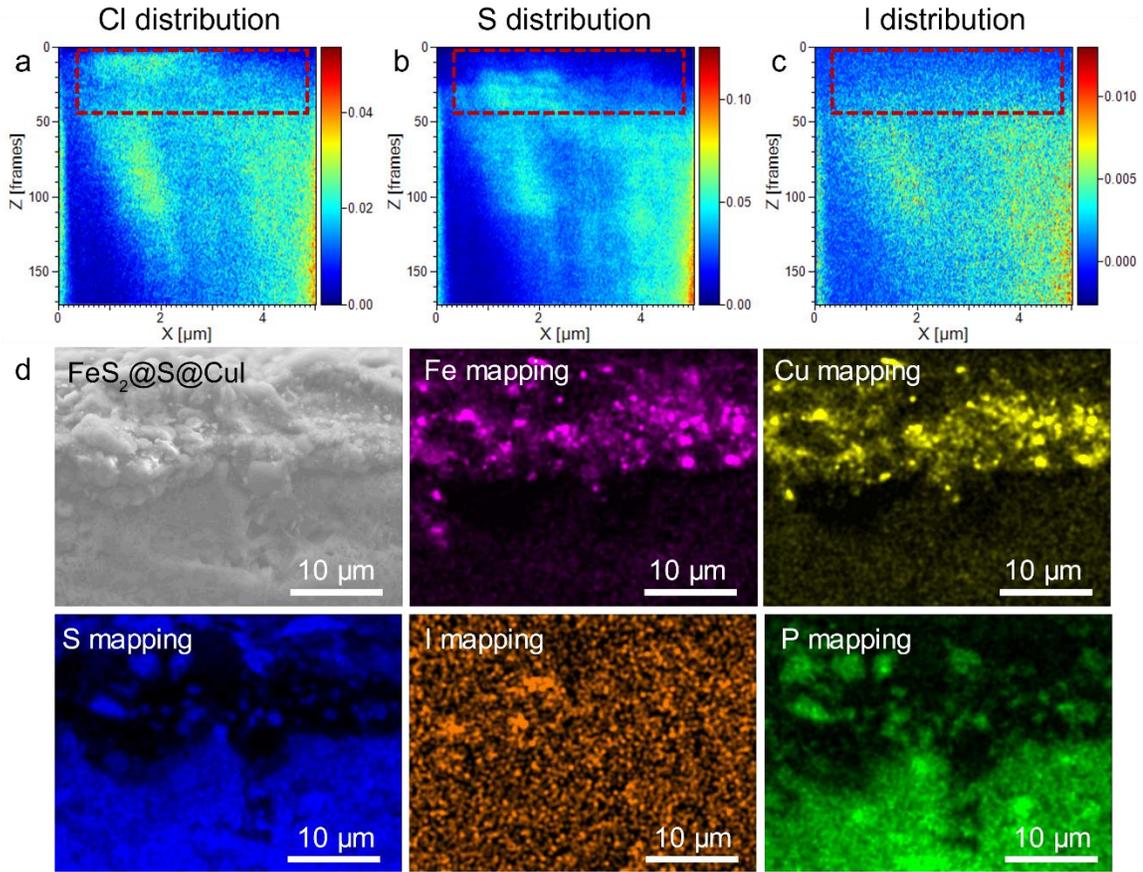


**Figure 6-3** CV curves of (a)  $\text{FeS}_2@\text{S}@\text{CuI}$  and (b)  $\text{FeS}_2@\text{S}$  composite cathode. EIS spectra of  $\text{FeS}_2@\text{S}@\text{CuI}$  composite cathode at (c) fully discharged state and (d) fully charged state. EIS spectra of  $\text{FeS}_2@\text{S}$  composite cathode at (e) fully discharged state and (f) fully charged state.

CV and operando EIS were collected to explore the catalytic effect of CuI on the redox kinetics of  $\text{FeS}_2@\text{S}$ . As shown in **Figure 6-3** a, during the first anodic scan of  $\text{FeS}_2@\text{S}@\text{CuI}$  composite, the reduction peak I belongs to the lithiation of S to  $\text{Li}_2\text{S}$ , and the reduction peak II belongs to the lithiation of  $\text{FeS}_2$  to  $\text{Li}_2\text{S}$  and Fe. Compared

with the reduction peaks in FeS<sub>2</sub>@S@CuI composite cathode, the reduction peaks I in FeS<sub>2</sub>@S moves to more negative value, and the reduction peak II were almost vanished (**Figure 6-3 b**), implying the formation of Li<sub>2</sub>S (reduction peaks I) affects the further lithiation of FeS<sub>2</sub> without CuI additive. In the first cathodic scan, the oxidation peak III belongs to the reaction (3)  $2\text{Li}_2\text{S} + \text{Fe} \rightarrow \text{Li}_2\text{FeS}_2 + 2\text{Li}^+ + 2e^-$  and oxidation peak IV attributes to reaction (4)  $\text{Li}_2\text{FeS}_2 \rightarrow \text{Li}_{2-x}\text{FeS}_2 + x\text{Li}^+ + xe^-$  and (5)  $\text{Li}_{2-x}\text{FeS}_2 \rightarrow \text{FeS}_y + (2-y)\text{S} + (2-x)\text{Li}^+ + (2-x)e^-$ , and the oxidation of Li<sub>2</sub>S back to S. Then, from the second cycle onward, the FeS<sub>2</sub>@S@CuI composite cathode shows excellent redox reversibility compared with FeS<sub>2</sub>@S composite cathode. The improved reaction kinetics in FeS<sub>2</sub>@S@CuI composite cathode after the first few cycles can also be proved by the reduced impedance of FeS<sub>2</sub>@S@CuI composite cathode at the third fully discharged state (D-1.0V, **Figure 6-3 c**). Then, from the fourth cycle onward, the interfacial resistance at fully discharged state (D-1.0V, **Figure 3c**), and the impedance at fully charged state (C-3.0V, **Figure 6-3 d**) remains almost constant, proving the highly reversible redox reaction proceeds in FeS<sub>2</sub>@S with CuI additive, which is beneficial for maintaining the structure integrity of FeS<sub>2</sub>@S@CuI composite cathode during cycles. In sharp contrast, for FeS<sub>2</sub>@S without CuI additive, the impedance continuously increases during discharge/charge process (**Figure 6-3 e-f**), proving the irreversible redox reaction and structure collapse of the FeS<sub>2</sub>@S composite cathode after lithiation/delithiation processes.

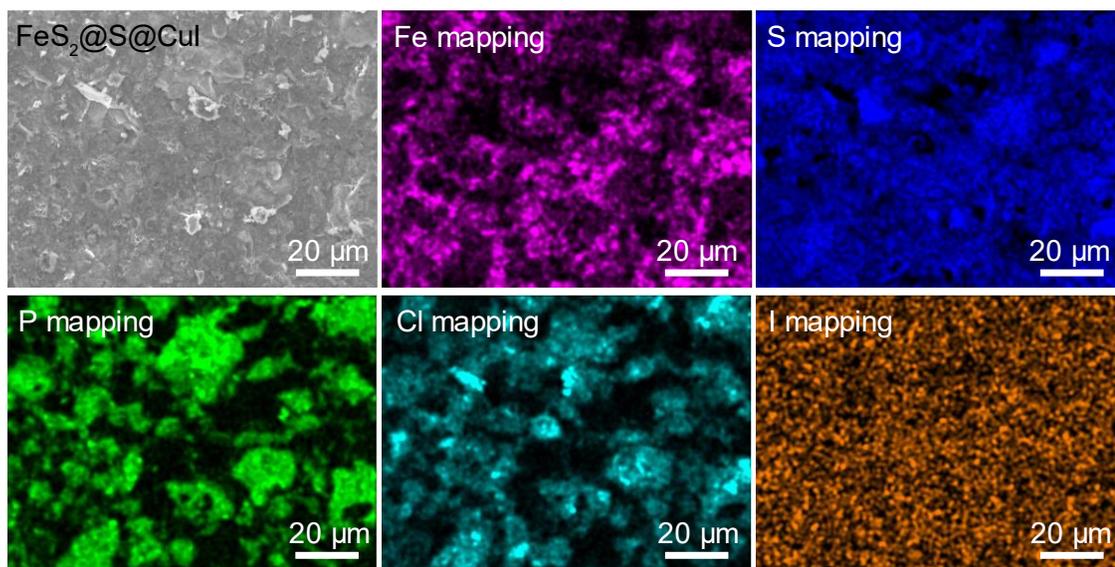
### 6.5 Interface Design of the $\text{FeS}_2@\text{S}@\text{CuI}$ Composite Cathode



**Figure 6-4** Element distribution for (a) Cl, (b) S and (c) I in  $\text{FeS}_2@\text{S}@\text{CuI}$  composite cathode after 20 cycles. (d) Cross-section SEM and EDS images of  $\text{FeS}_2@\text{S}@\text{CuI}$  composite cathode after 100 cycles.

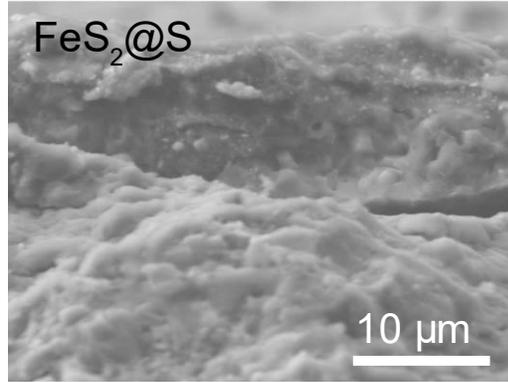
ToF-SIMS and EDS were collected to explore the mechanism of the catalytic effect of CuI. For the elemental distribution images in **Figure 6-4** a-c, the area that Cl-rich and S-poor is the  $\text{Li}_6\text{PS}_5\text{Cl}$  electrolyte rich area (marked by the red rectangle), while the area that Cl-poor and S-rich represents the  $\text{FeS}_2@\text{S}$  rich area. As shown in **Figure 6-4** a-c, I signal also has high intensity in  $\text{Li}_6\text{PS}_5\text{Cl}$  electrolyte rich area (marked by the red rectangle), proving the I migration from the  $\text{FeS}_2@\text{S}$  rich area to  $\text{Li}_6\text{PS}_5\text{Cl}$

electrolyte rich area after discharge/charge processes. The I migration can decrease the interfacial resistance of the composite cathode, because LiI can increase the  $\text{Li}^+$  transfer between  $\text{Li}_6\text{PS}_5\text{Cl}$  and  $\text{Li}_2\text{S}$ , which is in accordance with the EIS results in **Figure 6-3 c**. Benefited from the catalytic effect of CuI, the  $\text{FeS}_2@\text{S}@\text{CuI}$  composite cathode retains excellent structure integrity (**Figure 6-4 d**) without crack formation inside the composite cathode layer and at  $\text{Li}_6\text{PS}_5\text{Cl}/\text{FeS}_2@\text{S}@\text{CuI}$  interface.

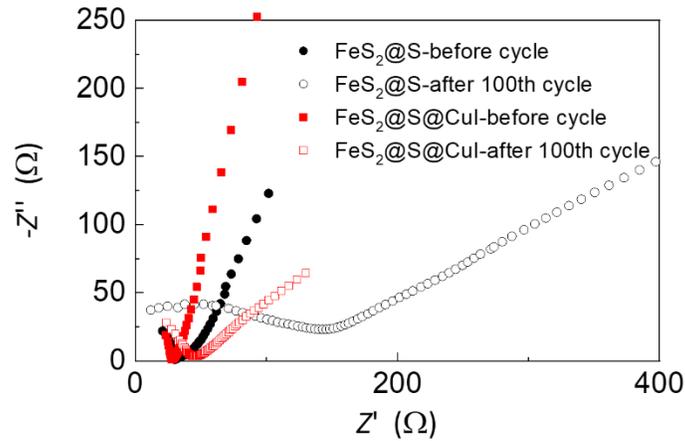


**Figure 6-5** SEM and EDS images for the surface of  $\text{FeS}_2@\text{S}@\text{CuI}$  composite cathode after 100 cycles.

Besides, all the components in the composite cathode were homogeneously distributed after 100 cycles (**Figure 6-5**). While cracks are obviously observed in  $\text{FeS}_2@\text{S}$  composite cathode without CuI additive (**Figure 6-6**) after 100 cycles, which lead to significantly impedance increase (**Figure 6-7**) compared with that of  $\text{FeS}_2@\text{S}@\text{CuI}$  composite cathode.



**Figure 6-6** SEM images for the surface of FeS<sub>2</sub>@S composite cathode after 100 cycles.



**Figure 6-7** Impedance spectra of FeS<sub>2</sub>@S@CuI and FeS<sub>2</sub>@S composite cathode before and after 100 cycles.

### 6.6 Conclusion

In summary, we use FeS<sub>2</sub>@S@CuI composite as a model material to demonstrate that the *in-situ* formed fast Li<sup>+</sup>/e<sup>-</sup> transfer in sulfur cathode is efficient to improve the S/Li<sub>2</sub>S redox kinetics. After the initial few cycles, FeS<sub>2</sub>@S@CuI *in-situ* transfers to FeS<sub>2</sub>@S@Cu@LiI composite. Electronic/ionic conductive FeS<sub>2</sub> acts as sulfur host, Cu acts as electronic conductive additive, LiI acts as Li<sup>+</sup> transfer bridge at FeS<sub>2</sub>-S-

Li<sub>6</sub>PS<sub>5</sub>Cl triple-phase boundaries due to the migration of I from the FeS<sub>2</sub>@S to Li<sub>6</sub>PS<sub>5</sub>Cl. Such a composite sulfur cathode with enhanced S/Li<sub>2</sub>S redox kinetics enables the battery with areal capacity of 4 mAh cm<sup>-2</sup> to achieve a high initial Coulombic efficiency of 94.6% at current density of 0.5 mA cm<sup>-2</sup> under room temperature. Besides, the constructed all-solid-state batteries show excellent cycling stability and high capacity utilization at both high areal capacity of 4 mAh cm<sup>-2</sup> and low temperature of -30°C. This work offers a new strategy for designing high-performance all-solid-state battery with sulfur cathode.

## Chapter 7 Summary and Future Work

### 7.1 Lithium Anode / SSE Interfaces

On the anode side interface, addressed both the challenges of Li dendrite and high interface resistance by doping strontium(Sr) into lithium anodes. Different from all previous metal/metal oxide coating on garnet or Li alloy anodes that form lithiophilic interlayer, Li-Sr/SrO-doped-Li<sub>2</sub>O are enriched on the interface forming a lithiophilic/lithiophobic bifunctional layer. The interlayer reduces the interfacial resistance and also suppresses lithium dendrite. The stability of the lithiophobic SrO doped Li<sub>2</sub>O against Li prevents reducing the garnet and suppresses Li dendrite, which distinguishes it from all reported alloy electron-conducting interlayers. The optimized Li-Sr | garnet | Li-Sr symmetric cell achieves a critical current density of 1.3 mA/cm<sup>2</sup> and can be cycled for 1,000 cycles under 0.5 mA/cm<sup>2</sup> at room temperature. The bifunctional lithiophilic/lithiophobic interlayer provides a new strategy for high-performance garnet solid-state lithium batteries

Enlightened by the effectiveness of the Sr work, I tried to further more stable material on the interface. I screened the Gibbs energy for the reaction between Li and the metal oxides ( $nLi + MO_m \leftrightarrow M + nLiO_{m/n}$ ) and identified the LiYO<sub>2</sub> as a highly thermodynamical stable candidate for the interface between the electrolyte and lithium. In addition, LiYO<sub>2</sub> has a record high interface energy against lithium of 81.65 meV/Å, which would provide high dynamic stability against dendrite

penetration. Guided by our design principle, we successfully established the Li | LLZTO interface with LiYO<sub>2</sub> as the interlayer, which endows the symmetric cells a high critical current density of 1.15 mA cm<sup>-2</sup>, a critical capacity of 4.2 mAh cm<sup>-2</sup> at 0.1 mA cm<sup>-2</sup> and a long cycle life of 600 cycles under 0.5 mA cm<sup>-2</sup>/0.25 mAh cm<sup>-2</sup>. This work sheds new insight on the rational design of the interface for SSLBs with high performance.

Inspired by the failure analysis ([Chapter 3.5](#)) in the Sr work, I realized the impact the anode bulk properties on interface stability. Void formation was carefully analyzed, which should be controlled by the product of the lithium full stripping capacity and the applied current, which is defined as the void suppression capability (VSC). The VSC can be enhanced by increasing the self-diffusivity and initial concentration of the lithium atoms. By refining the grain by introducing a Mg-1wt%La inoculant into molten lithium (LiMgLa), the lithium self-diffusivity and VSC are enhanced by 10.56 and 6.28 times, respectively, resulting in an increase in the critical current density/capacity from 1.2 mA·cm<sup>-2</sup>/0.6 mAh·cm<sup>-2</sup> for the Li anode to 2.2 mA·cm<sup>-2</sup>/1.1 mAh·cm<sup>-2</sup> for the LiMgLa anode. The LiMgLa anodes enable stable Li plating/stripping for over 1,200 h at 0.7 mA·cm<sup>-2</sup> at room temperature. The phase-field model dynamically shows that the interfacial overpotential will be higher than the critical overpotential of the electrolyte when the Li stripping is larger than 70% of the full depletion capacity, leading to dendrite growth and cell failure. The new understanding of the interface evolution and strategy of refining Li grain size paves the way for the design of both high power and high energy density SSLBs.

## 7.2 Cathode / SSE Interfaces

Low initial Coulombic efficiency (CE) and capacity utilization at high cathode loading are the main challenges that impede the cyclic performance and the energy density of sulfur cathode due to the poor S/Li<sub>2</sub>S redox kinetics. Herein, we address both challenges using FeS<sub>2</sub>@S@CuI composite, where Li<sup>+</sup>/e<sup>-</sup> conductive FeS<sub>2</sub> acts as an active sulfur host to ameliorate the volume change of sulfur, catalytic CuI additive will *in-situ* transfer to Cu-LiI, and the *in-situ* formed LiI acts as a Li<sup>+</sup> transfer bridge at FeS<sub>2</sub>-S-Li<sub>6</sub>PS<sub>5</sub>Cl phase boundaries to promote Li<sup>+</sup> transfer, thus increasing the S/Li<sub>2</sub>S redox kinetics. Benefited from these merits, the FeS<sub>2</sub>@S@CuI composite with areal capacity of 4.0 mAh cm<sup>-2</sup> shows a high initial CE of 94.6% at current density of 0.5 mA cm<sup>-2</sup> under room temperature. Besides, a long cyclic performance with capacity retention of 88.8% after 145 cycles was also at high areal capacity of 4.0 mAh cm<sup>-2</sup> under room temperature. Furthermore, a high capacity utilization of 96.5% at room temperature, 44.4% at -20°C and 33.3% at -30°C is also achieved for the FeS<sub>2</sub>@S@CuI composite cathode, which has never been reported in all-solid-state battery. This work provides a strategy for designing high-performance solid-state sulfur cathodes.

## 7.3 Future Work

For the past decades, the hotspot of all-solid-state batteries research has been switched from finding high ionic conductivity SSE to pursuing low interface resistance. In this dissertation, it has been demonstrated that new understanding such

as interface energy, VSC are critical and should be paid more attention to. Future works could focus on:

1. Controllable construction of the high interface energy interface. The *in-situ* formed method by molten lithium is not suitable for other SSE systems such as sulfide and polymer, and it does not have a good manufacturability for mass production.
2. Mechanical properties enhancement of the bulk anode and bulk SSE towards void suppression. Methods to achieve a more deformable anode without sacrificing the energy density, and to have more deformable SSEs without adding organic binders would be highly beneficial to construct a robust interface, and thus to realize the practical future SSLM without high external pressure add-on.
3. The failure mechanism of the Li<sup>+</sup>/e<sup>-</sup> conductive network inside a solid-state battery cathode should be further explored for us the design a interface that could realize high cathode active material ratio.

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## Publication and Presentation

### Publications:

- (1) **He, X.**; Ji, X.; Zhang, B.; Rodrigo, N. D.; Hou, S.; Gaskell, K.; Deng, T.; Wan, H.; Liu, S.; Xu, J.; Nan, B.; Lucht, B. L.; Wang, C. Tuning Interface Lithiophobicity for Lithium Metal Solid-State Batteries. *ACS Energy Letter* **2021**.  
<https://doi.org/10.1021/acseenergylett.1c02122>.
- (2) **He, X.**; Ji, X.; Wang, Z.; Wan, H.; Wang, C. High Interface Energy Enabled Highly Stable Garnet-based Lithium Metal Solid-State Batteries (Ready to Submit)
- (3) Ji, X.†; **He, X.†**; Chen, C.†; Hou, S.; Xu, J.; Zhang, B.; Ruan, Y.; Zhang, J.; Deng, T.; Chen, J.; Wang, C. Void Suppressive Lithium Anodes for All-Solid-State Batteries. *Nature Material* (Under Review) (Co-First Author)
- (4) Wan, H. †; **He, X.†**; Ren, Y.; Wang, C. Highly reversible sulfur cathode for all-solid-state lithium-sulfur battery (Ready to Submit) (Co-First Author)
- (5) Chiekezi, O.†; **He, X.†**; Wang, H.; Reed, D.; Wang, C.; Lu, X. Highly Conductive PEO-Based Composite Polymer Electrolyte for Na Battery Applications. *Journal of The Electrochemical Society* (Submitted) (Co-First Author)
- (6) Deng, T.†; Cao, L.†; **He, X.†**; Li, A.-M.; Li, D.; Xu, J.; Liu, S.; Bai, P.; Jin, T.; Ma, L.; Schroeder, M. A.; Fan, X.; Wang, C. In Situ Formation of Polymer-Inorganic Solid-Electrolyte Interphase for Stable Polymeric Solid-State Lithium-Metal Batteries. *Chem* **2021**. (Co-First Author)  
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#### **Presentations:**

- (1) **He, X.**; Wang, C. Interface Design for All-Solid-State Lithium Metal Batteries. *ACS Fall 2022 - American Chemical Society, Chicago, IL*. Student Presentation Award Competition. Oral, August 27 ([Third Prize Winner](#))
- (2) **He, X.**; Ji, X.; Wang, C. Interface Lithiophobicity Regulation for Lithium Metal Solid-State Batteries. *ACS Fall 2022 - American Chemical Society, Chicago, IL*. [ENFL] Division of Energy and Fuels. Oral - In-person, August 23. [3720265](#).
- (3) **He, X.**; Ji, X.; Wang, C. Interface Lithiophobicity Regulation for Lithium Metal Solid-State Batteries. *Electrochem Soc Meet Abstr* **2022**, MA2022-01 (1), 87–87. <https://doi.org/10.1149/ma2022-01187mtgabs>.
- (4) Lu, X.; **He, X.**; Wang, H.; Reed, D.; Sprenkle, V. Highly Conductive PEO-Based Polymer Electrolyte for Na Battery Applications. *Electrochem Soc Meet Abstr* **2019**. <https://doi.org/10.1149/ma2019-01/2/134>.